

**Request For a RCRA Class 2 Permit Modification
in Accordance with 20.4.1.900 NMAC
(incorporating 40 CFR Part 270)**

Drum Age Criteria

**Waste Isolation Pilot Plant
Carlsbad, New Mexico**

April 27, 2001

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Drum Age Criteria

Consistent with requirements of 20.4.1.900 New Mexico Administrative Code (NMAC) (hereafter referred to as Part 270 or Section 270.XX) the U.S. Department of Energy (DOE), Carlsbad Field Office (CBFO) is submitting to the New Mexico Environment Department (NMED) a request for a Class 2 modification to the Hazardous Waste Facility Permit (HWFP or Permit) (NM4890139088-TSDF) for the Waste Isolation Pilot Plant (WIPP). Specifically, this information is provided to comply with the requirements of Section 270.42(b).

The requested modification is listed in Table 1. Listed information includes a reference to the applicable section of the permit, a brief description of the item, and the class of the item, as identified in Appendix I to Section 270.42. The relevant permit modification category, as identified in Appendix I, is provided as well. A more complete description of the Class 2 modification is provided in Attachment A.

Table 1. Class 2 Hazardous Waste Facility Permit Modification

No.	Affected Permit Section	Item	Category	Attachment 1 Page #
1	a. Attachment B Attachment B, Table B-8 b. Attachment B1 Attachment B1-1a Attachment B1-1a(1) Attachment B1-1a(2) Attachment B1-1a(3) Attachment B1-1a(3)(i) Attachment B1-1a(3)(ii) Attachment B1-1a(3)(iii) Attachment B1-1c(5) Attachment B1-6 Attachment B1, Table B1-5 Attachment B1, Table B1-6 Attachment B1, Table B1-7 Attachment B1, Table B1-8 Attachment B1, Table B1-9 Attachment B1, Table B1-10 c. Attachment B3 Attachment B3-11a Attachment B3, Table B3-12 d. Attachment B6	Modification to allow generator/storage sites to establish a packaging specific drum age criteria (DAC)	20.4.900 NMAC (40 CFR 270.42 Appendix I) Class B.1.d	A-1

Attachment A

Descriptions of the Class 2 Hazardous Waste Facility Permit Modification

Item 1

Description:

A request for a permit modification to establish a revised methodology for determining a drum age criteria (DAC) based on packaging configuration groups.

Basis:

This permit modification provides generator/storage sites characterizing the headspace gas of TRU mixed waste a revised methodology for determining the drum age criteria based on specific packaging configurations. The results are applied simply through the addition of look-up tables to the Permit.

In responses to comments on both the draft Permit and the revised draft Permit, the NMED established three points regarding the DAC values:

1. Drum age must assure headspace gas has reached 90% of steady-state to preclude the necessity to collect samples from innermost layers of confinement.
2. Additional studies and experimental studies are required to justify alternative values.
3. Standardized values retain simplicity within the Permit.

Section B1-1a of the Permit establishes that a DAC must be met “to ensure that the drum contents have reached 90 percent of steady-state concentration within each layer of confinement.” The section also establishes a DAC for S5000 (Debris) waste as a minimum of 142 days after packaging and a DAC for S3000 (Homogeneous solids) and S4000 (Soil/gravel) waste as a minimum of 225 days after packaging. These DAC only considered the time necessary to meet the 90 percent of steady-state concentration criterion for the following packaging configurations, which were considered to be bounding at the time the permit was written:

- Containers are 55-gallon drums
- Containers are filtered at the time of packaging
- Containers of S5000 (debris) waste contain a maximum of 5 layers of confinement
- Containers of S3000 (Homogeneous solids) and S4000 (Soils/gravels) waste contain a maximum two layers of confinement
- Toluene is the constituent of interest (due to its prevalence in TRU mixed waste and its slow diffusion time)

This permit modification request establishes additional drum age criteria in the form of

packaging configuration specific DAC that ensure that the 90 percent of steady-state criterion is met for all currently identified packaging configurations. The packaging configuration DAC proposed in this modification were developed using the same model and calculation methodology as was used in developing the DAC in the permit. The packaging configuration assigned to each container is based on the number of layers of confinement used in packaging the waste. The layers of confinement are known based on the information currently collected. The identification of layers of confinement and number of rigid liners is required by the TRUPACT II Authorized Methods for Payload Control (TRAMPAC) for every shipment of TRU waste in TRUPACT II. The permit modification proposes to incorporate language from the TRAMPAC regarding the identification and verification of packaging information.

In addition, this modification proposes to provide clarification within the permit when using the term “unvented rigid container greater than 4 liters.” The way this term is used implies that the drum liner is considered an unvented container greater than 4 liters, which is inconsistent with Lockheed (1995) (entitled “Position for Determining Gas Phase Volatile Organic Compound Concentrations in Transuranic Waste Containers”, INEL-95/0109, August, 1995, Lockheed Idaho Technologies Company) which is referenced in the permit as the source of the DAC. To address this inconsistency, the Class 2 modification establishes three different sampling scenarios for containers subject to headspace gas sampling.

The Permit also contains language in Section B1-1a that states that a representative sample cannot be collected until the rigid poly liner has been vented to the drum. This is only applicable to samples that are taken between the drum lid and the unvented poly liner. Samples that are taken from within the rigid drum liner or through the pipe component vent hole are representative if the appropriate DAC has been met. Therefore, the language in this section has been modified to clarify this point and to ensure such sampling obtains a representative sample.

Discussion:

Section B1-1a of the Permit establishes that the DAC must be met “to ensure that the drum contents have reached 90 percent of steady-state concentration within each layer of confinement.” The section also establishes the DACs for S5000 (Debris) waste as a minimum of 142 days after packaging and for S3000 (Homogeneous solids) and S4000 (Soil/gravel) waste as a minimum of 225 days after packaging. These values are based on the results of the Lockheed (1995) report. This report describes the model and methodology used to establish the 142 and 225 day DAC. This document based the final DAC on the following packaging configurations, which were considered to be bounding at the time the permit was written:

- Containers are 55-gallon drums
- Containers are filtered at the time of packaging
- Containers of S5000 (debris) waste include 5 layers of confinement
- Containers of S3000 (Homogeneous solids) and S4000 (Soils/gravels) waste

include two layers of confinement

- Toluene is the constituent of interest (due to its prevalence in TRU mixed waste and its slow diffusion time)

The DAC is a unique value for each packaging configuration. The computer program that implements a VOC transport model is used to calculate the transient VOC gas-phase concentrations throughout a waste container. The VOC transport model consists of a series of material balance equations describing the transient VOC transport across layers of confinement in a container. The primary mechanisms for gas transport across a confinement layer are permeation across a polymeric layer, diffusion through air across an opening between layers, and diffusion through a filter vent in the case of a drum filter or filtered bag. One or all of these mechanisms of transport may be operating depending on the characteristics of the confinement layer. The governing equations for the model are presented in Lockheed (1995) and referenced in BWXT (2000) (entitled "Determination of Drum Age Criteria and Prediction Factors Based on Packaging Configurations", INEEL/EXT-2000-01207, Bechtel BWXT Idaho, October, 2000). A sensitivity analysis was conducted to evaluate the parameters that have the most impact on the calculated DAC value. This sensitivity analysis was conducted as part of the Liekhus et al. (1999) report that is referenced in the BWXT (2000) report.

Two types of testing were used in the development of the model used to calculate the DAC (Lockheed 1995). Some tests were conducted to establish the transport characteristics associated with the polymer bags. The polymer bags used in the testing were polyethylene bags because of their low permeability and use as the primary packaging material for TRU mixed waste. The specific parameters used in the modeling include VOC solubility in a polymer bag, VOC solubility in the rigid liner, VOC permeability through a polymer bag, and transfer coefficients. This testing was done using scaled-down 55-gallon drums.

Other tests were used to validate the final transport characteristics and models used by matching the results of the modeling to actual waste containers (Lockheed 1995). This testing was a validation that the diffusion model effectively simulated the physical process of VOC migration through an actual waste container in addition to the smaller simulated containers used in the initial testing. Additional testing is not necessary because the actual waste drum testing demonstrated that the parameters effectively describe the interactions of the VOC gas with the polyethylene used in the packaging and can be scaled to the size of the polyethylene bags and rigid liners used in actual system being modeled using the thickness and surface area.

The original Lockheed (1995) report only considered a single packaging configuration for the S5000 and S3000/S4000 waste forms and the equations used in the modeling reflect this by using a single value to account for the VOC transport. The BWXT (2000) considers multiple packaging configurations for the waste forms and although the equations used for the modeling are the same as those from the Lockheed (1995) report, the equations account for the number of layers of confinement rather than the single value used in the Lockheed (1995) report.

The BWXT (2000) report contains additional information and equations in Sections 5

and 6 that were used in calculating prediction factors and concentration multipliers. These same equations are also provided in the INEEL (1999) report that is referenced in the BWXT (2000) report and included as a reference attached to this permit modification. This permit modification **does not** request the addition of the prediction factor/concentration multiplier methodology to the permit; therefore, the equations that are provided in these sections do not impact the lookup tables in this modification and are not authorized for use during permit compliance under this modification.

Section 3 of the BWXT (2000) report specifically references a revision of the original Lockheed (1995) report (i.e., Connolly et al., 1998) for the model assumptions and other model input parameters that are used in calculating the DAC. This reference also applies to the equations used for the DAC calculation because the original model was used for the packaging configuration specific DACs with a minor change in approach to accommodate various packaging configurations. The revisions that were made to the original model were to include inputs for the number of layers of confinement (as opposed to the fixed number of 5 layers for S5000 waste and 2 layers for S3000 and S4000 waste), the size of the hole in the rigid liner (as opposed to the constant size of 0.375 in.), and the filter diffusivity (as opposed to the constant diffusivity of 3.7×10^{-6} mol/s/mol fraction). All of these changes are necessary to evaluate the various packaging configurations and do not change the actual equations that are used in the simulation (i.e., parameters that were treated as constants for the bounding case in the Lockheed [1995] report are variables in the BWXT [2000] report). At the same time, the model was also modified to remove some of the capabilities that cause increased run time, but were not used in calculating either the original DACs or the packaging specific DACs. The changes that fall into this category include eliminating gas generation and eliminating the newly packaged container with an unvented drum liner. Software verification and validation was conducted to ensure that these changes were correctly implemented and did not affect the final calculated results. The software verification and validation report is attached to this permit modification.

In order to provide a basis for generator/storage sites to select the appropriate DAC for their waste, three different sampling scenarios are identified in BWXT (2000). These scenarios are:

1. Unvented drums that have been packaged for a specified period of time sufficient to achieve equilibrium conditions (i.e., met the DAC for Scenario 1 drums in Table 2) shall be sampled as follows:
 - A. Unvented drums without rigid poly liners are sampled at the time of venting through the drum lid.
 - B1. Unvented drums with unvented rigid poly liners are sampled through the rigid liner
 - B2. Vented drums with unvented rigid poly liners are sampled through the rigid liner
 - C. Unvented drums with vented rigid poly liners are sampled through the drum lid

2. Drums that have been packaged for a specified period of time sufficient to achieve equilibrium conditions (i.e., met the DAC for Scenario 1 drums in Table 2) and then are vented, but not sampled at the time of venting.
3. Containers (i.e., drums, SWBs, and pipe components) that are initially packaged in a vented condition and sampled in the container headspace after a specified period of time sufficient to achieve equilibrium conditions.

Only unvented drums fall under Scenario 1. For these drums, the DAC was calculated based on 6 layers of confinement for S5000 waste and 2 layers of confinement for S3000/S4000 waste. Table 2 contains the matrix of DAC values that are applicable to drums that are covered under Scenario 1. Meeting the Scenario 1 DAC ensures that a representative sample may be collected under the drum lid (unlined drums or unvented drums with vented rigid poly liners) or collected through the rigid poly liner (unvented or vented drums with unvented rigid poly liners).

Scenario 2 is also for drums. In this Scenario, the drums are those that already meet the Scenario 1 DAC, but are not sampled at the time of venting. Because a Scenario 2 drum has already reached equilibrium conditions prior to venting, the initial condition used to determine the DAC applicable after venting is based on equilibrium conditions in the drum rather than the zero concentration conditions in a drum that is filtered at the time of packaging (see Scenario 3 discussion). However, if an unvented drum has not reached equilibrium prior to venting, (i.e., not met the Scenario 1 DAC) the drum must be classified under Scenario 3. Table 3 contains the Scenario 2 DAC matrix.

To evaluate the development of additional DAC values, generator/storage sites were asked to identify present and future packaging configurations. This review indicated that the packaging configurations can be summarized under a number of common configurations (BWXT 2000). These common configurations were divided into the two major categories: (1) packaging configurations of containers belonging to summary categories S3000 (Homogenous solids) and S4000 (Soil/gravel), and (2) packaging configurations of containers belonging to summary category S5000 (Debris waste).

Table 4 lists the currently identified packaging configurations applicable to Scenario 3 and identifies the most restrictive configuration for use as the default packaging configuration when necessary. In addition to the drum packaging configurations, packaging configurations for the pipe component and standard waste box (SWB) were evaluated. The pipe component is a metal pipe with a filtered lid that contains waste and conceptually is similar to a small drum in its configuration. The pipe component is overpacked in a drum for shipment and disposal. Similarly to other overpacked containers (e.g., drums inside of a standard waste box), the headspace gas sampling for pipe components is focused on the headspace of the pipe component, which then must be conservatively assigned to the overpacked container (in this case the drum).

The VOC transport model computer program was used to generate a matrix of packaging-specific DAC values for Scenario 3 (Tables 5 and 6).

To obtain the appropriate DAC value of a container, the sampling scenario is identified and then, for Scenario 3 containers, the actual container packaging configuration is

assigned to one of the packaging configuration groups. The packaging configuration group is assigned based on the number of layers of confinement that are in the container. The number of layers of confinement can be determined as part of the AK requirements (i.e., supplemental information includes packaging logs). Packaging logs at the generator/storage sites typically contain information on the types of packaging and layers of confinement used. In addition the number of layers of confinement are included as part of the testing batch report for radiography and visual examination as specified in Permit Attachment B3, Table B3-11: Testing Batch Data Report Contents.

In addition to these requirements, the proposed permit modification includes requirements for the packaging configuration to be documented as part of the headspace gas sampling data and subsequently be evaluated during reconciliation with the data quality objectives to ensure that an appropriate DAC was used. However, if a specific packaging configuration cannot be assigned based on the data collected during characterization and confirmation, a conservative default Table 4 packaging configuration of 3 for drums and 6 for SWBs must be assigned provided the drums and SWBs do not contain pipe component packaging. If pipe components are present as packaging in the drums or SWBs, the pipe components must be sampled following the requirements for packaging configuration 4.

The DAC for the container is then located on the applicable matrix by looking up the entry that corresponds to the appropriate summary category group, bounding packaging configuration, filter diffusivity, and rigid drum liner hole size of the container being evaluated. If a the filter diffusivity and/or the rigid drum liner hole size fall between two values on the tables, the value that results in the longer (i.e., more conservative) DAC must be used.

The permit currently implies that if a container has met the DAC in an unvented condition and the headspace gas sample is not taken at the time of venting, the venting date starts the clock for meeting the DAC. This implication comes from the reference to unvented rigid containers greater than 4 liters which can be interpreted to mean that the reference to unvented sealed rigid containers greater than 4 liters includes the drum liner. This is not the case. Lockheed (1995) and BWXT (2000) both indicate that if the drum has met the Scenario 1 DAC in an unvented condition, a specific waiting period equal to the appropriate Scenario 2 DAC is needed for re-equilibration of the headspace gas after venting the drum liner if a sample is not taken at the time of venting. This contradicts the implication in the permit that because the rigid liner is greater than 4 liters and is sealed, the Scenario 3 DAC must be met. Therefore, the language in this permit modification relative to sampling Scenario 2 revises the permit to clarify this point and emphasizes that if sampling through a rigid container (including the rigid liner) occurs, a representative sample must be taken by ensuring that the sampling device forms an airtight seal with the rigid liner.

If additional packaging configurations are identified at a later date, CBFO will submit modifications to specify appropriate DAC based on the methodology in the BWXT (2000) report. Sites are being encouraged to use packaging configurations that have a DAC established whenever possible.

References

BWXT, 2000, Determination of Drum Age Criteria and Prediction Factors Based on Packaging Configurations, INEEL/EXT-2000-01207, October 2000, Liekhus, K.J., S.M. Djordjevic, M. Devarakonda, and M.J. Connolly, Bechtel BWXT Idaho, Idaho National Engineering and Environmental Laboratory, Idaho Falls, Idaho.

Lockheed Idaho Technologies Company, 1995, Position for Determining Gas Phase Volatile Organic Compound Concentrations in Transuranic Waste Containers, INEL-95/0109/Revision 1, M.J. Connolly, et. al., Lockheed Idaho Technologies Company.

Table 2. Scenario 1 DAC Matrix

Summary Category Group	DAC (days)
S3000/S4000	127
S5000	53

Table 3. Scenario 2 DAC Matrix

	Summary Category Group S3000/S4000				Summary Category Group S5000			
Filter H ₂ Diffusivity ^a	Liner Lid Opening Diameter (in)				Liner Lid Opening Diameter (in) ^b			
(mol/s/mol fraction)	0.30	0.375	0.75	1.0	0.30	0.375	0.75	1.0
1.9 x 10 ⁻⁶	36	30	23	22	29	22	13	12
3.7 x 10 ⁻⁶	30	25	19	18	25	20	12	11
3.7 x 10 ⁻⁵	13	11	11	11	7	6	6	4

^a The documented filter H₂ diffusivity must be greater than or equal to the listed value to use the DAC for the listed filter H₂ diffusivity (e.g., a container with a filter H₂ diffusivity of 4.2 x 10⁻⁶ must use a DAC for a filter with a 3.7 x 10⁻⁶ filter H₂ diffusivity).

^b The documented liner lid opening diameter must be greater than or equal to the listed value to use the DAC for the listed liner lid opening diameter (e.g., a container with a liner lid opening of 0.5 in must use a DAC for a liner lid opening of 0.375 in.)

Table 4
Scenario 3 Packaging Configurations

Packaging Configuration Group	Covered S3000/S4000 Packaging Configurations	Covered S5000 Packaging Configurations
Packaging Configuration 1, drums ^a	<ul style="list-style-type: none"> • No layers of confinement, filtered inner lid • No inner bags, no liner bags (bounding case) 	<ul style="list-style-type: none"> • No layers of confinement, filtered inner lid • No inner bags, no liner bags (bounding case)
Packaging Configuration 2, drums ^a	<ul style="list-style-type: none"> • 1 inner bag • 1 filtered inner bag • 1 liner bag (bounding case) • 1 filtered liner bag 	<ul style="list-style-type: none"> • 1 inner bag • 1 filtered inner bag • 1 liner bag • 1 filtered liner bag • 1 inner bag, 1 liner bag • 1 filtered inner bag, 1 filtered liner bag • 2 inner bags • 2 filtered inner bags • 2 inner bags, 1 liner bag • 2 filtered inner bags, 1 filtered liner bag • 3 inner bags • 3 filtered inner bags • 3 filtered inner bags, 1 filtered liner bag • 3 inner bags, 1 liner bag (bounding case)
Packaging Configuration 3, drums ^a	<ul style="list-style-type: none"> • 1 inner bag, 1 liner bag • 1 filtered inner bag, 1 filtered liner bag • 2 inner bags • 2 filtered inner bags • 2 liner bags (bounding case) • 2 filtered liner bags 	<ul style="list-style-type: none"> • 2 liner bags • 2 filtered liner bags • 1 inner bag, 2 liner bags • 1 filtered inner bag, 2 filtered liner bags • 2 inner bags, 2 liner bags • 2 filtered inner bags, 2 filtered liner bags • 3 filtered inner bags, 2 filtered liner bags • 4 inner bags • 3 inner bags, 2 liner bags • 4 inner bags, 2 liner bags (bounding case)

Packaging Configuration 4, pipe components	<ul style="list-style-type: none"> • No layers of confinement inside a pipe component • 1 filtered inner bag, 1 filtered metal can inside a pipe component • 2 inner bags inside a pipe component • 2 filtered inner bags inside a pipe component • 2 filtered inner bags, 1 filtered metal can inside a pipe component • 2 inner bags, 1 filtered metal can inside a pipe component (bounding case) 	<ul style="list-style-type: none"> • No layers of confinement inside a pipe component • 1 filtered inner bag, 1 filtered metal can inside a pipe component • 2 inner bags inside a pipe component • 2 filtered inner bags inside a pipe component • 2 filtered inner bags, 1 filtered metal can inside a pipe component • 2 inner bags, 1 filtered metal can inside a pipe component (bounding case)
Packaging Configuration 5, Standard Waste Box ^a	<ul style="list-style-type: none"> • No layers of confinement • 1 SWB liner bag (bounding case) 	<ul style="list-style-type: none"> • No layers of confinement • 1 SWB liner bag (bounding case)
Packaging Configuration 6, Standard Waste Box ^a	<ul style="list-style-type: none"> • any combination of inner and/or liner bags that is less than or equal to 6 • 5 inner bags, 1 SWB liner bag (bounding case) 	<ul style="list-style-type: none"> • any combination of inner and/or liner bags that is less than or equal to 6 • 5 inner bags, 1 SWB liner bag (bounding case)

^a If a specific packaging configuration cannot be assigned based on the data collected during characterization and confirmation, a conservative default packaging configuration of 3 for drums and 6 for SWBs must be assigned provided the drums and SWBs do not contain pipe component packaging. If pipe components are present as packaging in the drums or SWBs, the pipe components must be sampled following the requirements for packaging configuration 4.

Table 5
Scenario 3 Drum Age Criteria (in days) Matrix for S3000 and S4000 Waste
by Packaging Configuration Group

Packaging Configuration 1						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	131	95	37	24	4	4
3.7 x 10 ⁻⁶	111	85	36	24	4	4
3.7 x 10 ⁻⁵	28	28	23	19	4	4

Packaging Configuration 2						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	213	175	108	92	56	18
3.7 x 10 ⁻⁶	188	161	105	90	56	17
3.7 x 10 ⁻⁵	80	80	75	71	49	10

Packaging Configuration 3						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	283	243	171	154	107	34
3.7 x 10 ⁻⁶	253	225	166	151	106	31
3.7 x 10 ⁻⁵	121	121	115	110	84	13

Packaging Configuration 4	
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Headspace Sample Taken Inside Pipe Component
> 1.9 x 10 ⁻⁶	152

Packaging Configuration 5	
Filter H ₂ Diffusivity ^{a, c} (mol/s/mol fraction)	Headspace Sample Taken Inside SWB
> 7.4 x 10 ⁻⁶	15

Packaging Configuration 6	
Filter H ₂ Diffusivity ^{a, c} (mol/s/mol fraction)	Headspace Sample Taken Inside SWB
> 7.4 x 10 ⁻⁶	56

- ^a The documented filter H₂ diffusivity must be greater than or equal to the listed value to use the DAC for the listed filter H₂ diffusivity (e.g., a container with a filter H₂ diffusivity of 4.2 x 10⁻⁶ must use a DAC for a filter with a 3.7 x 10⁻⁶ filter H₂ diffusivity).
- ^b The documented liner lid opening diameter must be greater than or equal to the listed value to use the DAC for the listed liner lid opening diameter (e.g., a container with a liner lid opening of 0.5 in must use a DAC for a liner lid opening of 0.375 in.)
- ^c The filter H₂ diffusivity for SWBs is the sum of the diffusivities for all of the filters on the SWB because an SWB has more than 1 filter.

Table 6
Scenario 3 Drum Age Criteria (in days) Matrix for S5000 Waste
by Packaging Configuration Group

Packaging Configuration 1						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	131	95	37	24	4	4
3.7 x 10 ⁻⁶	111	85	36	24	4	4
3.7 x 10 ⁻⁵	28	28	23	19	4	4

Packaging Configuration 2						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	175	138	75	60	30	11
3.7 x 10 ⁻⁶	152	126	73	59	30	11
3.7 x 10 ⁻⁵	58	57	52	47	28	8

Packaging Configuration 3						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	197	161	96	80	46	16
3.7 x 10 ⁻⁶	175	148 ^c	93	79	46	16
3.7 x 10 ⁻⁵	72	72	67	62	42	10

Packaging Configuration 4	
Filter H ₂ Diffusivity (mol/s/mol fraction)	Headspace Sample Taken Inside Pipe Component
> 1.9 x 10 ⁻⁶	152

Packaging Configuration 5	
Filter H ₂ Diffusivity ^{a, d} (mol/s/mol fraction)	Headspace Sample Taken Inside SWB
> 7.4 x 10 ⁻⁶	15

Packaging Configuration 6	
Filter H ₂ Diffusivity ^{a, d} (mol/s/mol fraction)	Headspace Sample Taken Inside SWB
> 7.4 x 10 ⁻⁶	56

^a The documented filter H₂ diffusivity must be greater than or equal to the listed value to use the DAC for the listed filter H₂ diffusivity (e.g., a container with a filter H₂ diffusivity of 4.2 x 10⁻⁶ must use a DAC for a filter with a 3.7 x 10⁻⁶ filter H₂ diffusivity).

^b The documented liner lid opening diameter must be greater than or equal to the listed value to use the DAC for the listed liner lid opening diameter (e.g., a container with a liner lid opening of 0.5 in must use a DAC for a liner lid opening of 0.375 in.)

^c A DAC of 142 days can be used for this case provided the packaging configuration does not exceed a total of 5 layers of confinement.

^d The filter H₂ diffusivity for SWBs is the sum of the diffusivities for all of the filters on the SWBS because an SWBS has more than 1 filter.

Revised Permit Text:

a. 1. B-3c Radiography and Visual Examination

Radiography is a nondestructive qualitative and quantitative technique that involves X-ray scanning of waste containers to identify and verify waste container contents. Visual examination (VE) constitutes opening a container and physically examining its contents. Radiography and/or visual examination will be used to examine every waste container to verify its physical form and may be used in conjunction with acceptable knowledge to determine and/or verify an appropriate packaging configuration for specifying the container-specific drum age criterion (DAC). These techniques can detect liquid wastes and containerized gases, which are prohibited for WIPP disposal. The prohibition of liquids and containerized gases prevents the shipment of corrosive, ignitable, or reactive wastes. Radiography and/or VE will also be able to confirm that the physical form of the waste matches its waste stream description (i.e. Homogeneous Solids, Soil/Gravel, or Debris Waste [including uncategorized metals]). If the physical form does not match the waste stream description, the waste will be designated as another waste stream and assigned the preliminary hazardous waste codes associated with that new waste stream assignment. That is, if radiography and/or VE indicates that the waste does not match the waste stream description arrived at by acceptable knowledge characterization, a non-conformance report will be completed and the inconsistency will be resolved as specified in Permit Attachment B4. The proper waste stream assignment will be determined (including preparation of a new Waste Stream Profile Form), the correct hazardous waste codes will be assigned, and the resolution will be documented. Refer to Permit Attachment B4 for a discussion of acceptable knowledge and its confirmation process.

a. 2. Attachment B, Table B-8

TABLE B-8
WIPP WASTE INFORMATION SYSTEM DATA FIELDS^a

Characterization Module Data Fields ^b	
Container ID ^c	Total VOC Sample Date
Generator EPA ID	Total VOC Analysis Date
Generator Address	Total VOC Analyte Name ^d
Generator Name	Total VOC Analyte Concentration ^d
Generator Contact	Total Metal Sample Date
Hazardous Code	Total Metal Analysis Date
Headspace Gas Sample Date	Total Metal Analyte Name ^d
Headspace Gas Analysis Date	Total Metal Analyte Concentration ^d
Layers of Packaging (i.e., confinement)	Semi-VOC Sample Date
Drum Liner Hole Size	Semi-VOC Analysis Date
Headspace Gas Analyte ^d	Semi-VOC Analyte Name ^d
Headspace Gas Concentration ^d	Semi-VOC Concentration ^d
Headspace Gas Char. Method ^d	Transporter EPA ID
Total VOC Char. Method ^d	Transporter Name
Total Metals Char. Method ^d	Visual Exam Container ^e
Total Semi-VOC Char. Method ^d	Waste Material Parameter ^d
Item Description Code	Waste Material Weight ^d
Haz. Manifest Number	Waste Matrix Code
NDE Complete ^e	Waste Matrix Code Group
PCB Concentration	Waste Stream Profile Number
Certification Module Data Fields	
Container ID ^c	Handling Code
Container type	
Container Weight	
Contact Dose Rate	
Container Certification date	
Container Closure Date	
Transportation Data Module	
TRUPACT Number	Ship Date
Assembly Number ^f	Receive Date
Container IDs ^{c,d}	
ICV Closure Date	
Disposal Module Data	
Container ID ^c	
Disposal Date	
Disposal Location	

^a This is not a complete list of the WWIS data fields.

^b Some of the fields required for characterization are also required for certification and/or transportation.

^c Container ID is the main relational field in the WWIS Database.

^d This is a multiple occurring field for each analyte, nuclide, etc.

^e These are logical fields requiring only a yes/no.

^f Required for 7-Packs of 55 gal drums to tie all of the drums in that assembly together. This facilitates the identification of waste containers in a shipment without need to breakup the assembly.

b. 1. Attachment B1

List of Tables

Table	Title
B1-1	Gas Sample Containers and Holding Times
B1-2	Summary of Drum Field QC Headspace Sample Frequencies
B1-3	Summary of Sampling Quality Control Sample Acceptance Criteria
B1-4	Sampling Handling Requirements for Homogeneous Solids and Soil/Gravel
B1-5	Headspace Gas Drum Age Criteria Sampling Scenarios
B1-6	Scenario 1 Drum Age Criteria (In Days) Matrix
B1-7	Scenario 2 Drum Age Criteria (In Days) Matrix
B1-8	Scenario 3 Packaging Configurations
B1-9	Scenario 3 Drum Age Criteria (In Days) Matrix for S5000 Waste By Packaging Configuration Group
B1-10	Scenario 3 Drum Age Criteria (In Days) Matrix for S3000 and S4000 Waste By Packaging Configuration Group

b. 2. Attachment B1-1a

The Permittees shall require all headspace gas sampling be performed in an appropriate radiation containment area on waste containers that are in compliance with the container equilibrium requirements (i.e. 72 hours at 18 degrees C or higher).

Summary Category S5000

All waste containers or randomly selected containers from waste streams that meet the conditions for reduced headspace gas sampling listed in Section B-3a(1) designated as summary category S5000 (Debris waste) shall be categorized under one of the sampling scenarios shown in Table B1-5. If the container is categorized under Scenario 1, the applicable drum age criteria (DAC) from Table B1-6 must be met prior to headspace gas sampling. If the container is categorized under Scenario 2, the applicable Scenario 1 DAC from Table B1-6 must be met prior to venting the container and then the applicable Scenario 2 DAC from Table B1-7 must be met after venting the container. The DAC for Scenario 2 containers that contain filters or liner vent holes other than those listed in Table B1-7 shall be determined using footnotes "a" and "b" in Table B1-7. Containers that have not met the Scenario 1 DAC at the time of venting must be categorized under Scenario 3. Containers categorized under Scenario 3 must be placed into one of the packaging configuration groups listed in Table B1-8. If a specific packaging configuration cannot be assigned based on the data collected during characterization and confirmation, a conservative default packaging configuration of 3 for drums and 6 for SWBs must be assigned provided the drums and SWBs do not contain pipe component packaging. If a container is designated as packaging configuration group 4 (i.e., a pipe component), the headspace gas sample must be taken from the pipe component headspace. The DAC for Scenario 3 containers that contain filters or liner vent holes other than those listed in Table B1-9 shall be determined using footnotes "a" and "b" in Table B1-9. Each of the Scenario 3 containers shall be sampled for headspace gas after waiting the DAC in Table B1-9 based on its packaging configuration (note: packaging configurations 4, 5, and 6 are not summary category group dependent) a minimum of 142 days after packaging.

Summary Category S3000/S4000

All waste containers or randomly selected containers from waste streams that meet the conditions for reduced headspace gas sampling listed in Section

B-3a(1) designated as summary categories S3000 (Homogenous solids) and S4000 (Soil/gravel) shall be categorized under one of the sampling scenarios shown in Table B1-5. If the container is categorized under Scenario 1, the applicable drum age criteria (DAC) from Table B1-6 must be met prior to headspace gas sampling. If the container is categorized under Scenario 2, the applicable Scenario 1 DAC from Table B1-6 must be met prior to venting the container and then the applicable Scenario 2 DAC from Table B1-7 must be met after venting the container. The DAC for Scenario 2 containers that contain filters or liner vent holes other than those listed in Table B1-7 shall be determined using footnotes "a" and "b" in Table B1-7. Containers that have not met the Scenario 1 DAC at the time of venting must be categorized under Scenario 3. Containers categorized under Scenario 3 must be placed into one of the packaging configuration groups listed in Table B1-8. If a specific packaging configuration cannot be assigned based on the data collected during characterization and confirmation, a conservative default packaging configuration of 3 for drums and 6 for SWBs must be assigned provided the drums and SWBs do not contain pipe component packaging. If a container is designated as packaging configuration group 4 (i.e., a pipe component), the headspace gas sample must be taken from the pipe component headspace. The DAC for Scenario 3 containers that contain filters or liner vent holes other than those listed in Table B1-10 shall be determined using footnotes "a" and "b" in Table B1-10. Each of the Scenario 3 containers shall be sampled after waiting the DAC in Table B1-10 based on its packaging configuration (note: packaging configurations 4, 5, and 6 are not summary category group dependent) ~~a minimum of 225 days after packaging.~~

The determination of packaging configuration consists of identifying the number of confinement layers and the identification of rigid liners when present. Generator/storage sites are to use acceptable knowledge (procedural controls, etc.) as specified in Permit Attachment B4 and may use radiography and/or visual examination as specified in Permit Attachment B1 to make the determination of the appropriate sampling scenario and packaging configuration. ~~These drum age criteria are is to ensure that the drum container contents have reached 90 percent of steady state concentration within each layer of confinement (Lockheed, 1995, BWXT 2000).~~ The following information must be reported in the headspace gas sampling documents for all containers from which a headspace gas sample is collected:

- sampling scenario from Table B1-5 and associated information from Tables B1-6 and/or Table B1-7;
- the packaging configuration from Table B1-8 and associated information from Tables B1-9 or B1-10,
- the equilibrium time, and
- ~~the drum age of all containers from which a headspace gas sample is collected will be documented in headspace gas sampling documents.~~

All waste containers with unvented rigid containers greater than 4 liters (exclusive of rigid poly container liners), except for Waste Material Type II.2 packaged in a metal container, shall be subject to innermost layer of containment sampling or shall be vented prior to initiating drum age and equilibrium criteria. When sampling the rigid drum liner under Scenario 1, the sampling device must form an airtight seal with the rigid poly drum liner to ensure that a representative sample is collected (using a sampling needle connected to the sampling head to pierce the rigid drum liner satisfies this requirement). The configuration of the containment area and remote-handling equipment at each sampling facility are expected to differ. Headspace-gas samples will be analyzed for the analytes listed in Table B3-2 of Permit Attachment B3. If additional packaging configurations are identified, an appropriate Permit Modification will be submitted to incorporate the DAC using the methodology in BWXT (2000).

b. 3. Attachment B1-1a(1)

This headspace-gas sampling protocol employs a multiport manifold capable of collecting multiple simultaneous headspace samples for analysis and QC purposes. The manifold can be used to collect samples in SUMMA® or equivalent canisters or as part of an on-line integrated sampling/analysis system. The sampling equipment will be leak checked and cleaned prior to first use and as needed thereafter. The manifold and sample canisters will be evacuated to 0.0039 inches (in.) (0.10 millimeters [mm]) mercury (Hg) prior to sample collection. Cleaned and evacuated sample canisters will be attached to the evacuated manifold before the manifold inlet valve is opened. The manifold inlet valve will be attached to a changeable filter connected to either a side port needle sampling head **capable of forming an airtight seal** (for penetrating a carbon-composite filter **or rigid poly liner when necessary**), ~~or~~ a sampling head with an airtight ~~seal fitting~~ for sampling through an existing filter vent hole, ~~or~~ a drum punch sampling head **capable of forming an airtight seal** (capable of punching through the metal lid of a drum).

b. 4. Attachment B1-1a(2)

This headspace-gas sampling protocol employs a canister-sampling system to collect headspace-gas samples for analysis and QC purposes without the use of the manifold described above. Rather than attaching sampling heads to a manifold, in this method the sampling heads are attached directly to an evacuated sample canister as shown in Figure B1-3.

Canisters shall be evacuated to 0.0039 in. (0.10 mm) Hg prior to use and attached to a changeable filter connected to the appropriate sampling head. The sampling head(s) must be capable of punching through the metal lid of the drums **and/or the rigid poly liner when necessary**, ~~a sampling head with providing an air tight airtight seal for~~ **when** sampling through the existing filter vent hole or penetrating a carbon-composite filter to obtain the drum headspace samples. Field duplicates must be collected at the same time, in the same manner, and using the same type of sampling apparatus as used for headspace-gas sample collection. Field blanks shall be samples of room air collected in the immediate vicinity of the waste-drum sampling area prior to removal of the drum lid. Equipment blanks and field-reference standards must be collected using a purge assembly equivalent to the standard side of the manifold described above. These samples shall be collected from the needle tip through the same components (e.g., needle and filter) that the headspace-gas samples pass through.

The sample canisters, associated sampling heads, and the headspace-sample volume requirements ensure that a representative sample is collected. When an estimate of the available headspace-gas volume of the waste container can be made, less than 10 percent of that volume should be withdrawn. A determination of the sampling head internal volume shall be made and documented. The total volume of headspace gases collected during each headspace gas sampling operation can be determined by adding the volume of the sample canister(s) attached to the sampling head to the internal volume of the sampling head. Every effort shall be made to minimize the internal volume of sampling heads.

Each sample canister used with the direct canister method shall have a pressure/vacuum gauge capable of indicating leaks and sample collection volumes. Canister gauges are intended to be gross leak-detection devices not vacuum-certification devices. If a canister pressure/vacuum gauge indicates an unexpected pressure change, determination of whether the change is a result of ambient temperature and pressure differences or a canister leak shall be made. This gauge shall be helium-leak tested to 1.5×10^{-7} standard cc/s, have all stainless steel construction, and be capable of tolerating temperatures to 125EC.

The SUMMA® or equivalent sample canisters as specified in EPA's Compendium Method TO-14 (EPA 1988) shall be used when sampling each drum. These heads shall form a leak-tight connection with the canister and allow sampling through the drum ~~lid~~ carbon-composite filter, ~~or~~

through the drum lid itself ~~and/or rigid poly liner when necessary~~ (by punching, or using an airtight ~~seal~~ fitting to collect a sample through the existing filter vent hole, ~~or using a hollow side port needle~~). Figure B1-3 illustrates the direct canister-sampling equipment.

b. 5. Attachment B1-1a(3)

A sample of the headspace gas directly under the ~~drum container lid~~, ~~pipe overpack filter vent hole, or rigid liner~~ shall be collected. ~~from within the drum~~ Two Five methods, sampling through the carbon filter, ~~and~~ sampling through the drum lid, ~~sampling through the pipe overpack filter vent hole, sampling through the rigid liner, and sampling with an airtight fitting in the existing container vent hole~~ have been developed for collecting a representative sample. The chosen sampling method shall preserve the integrity of the drum to contain radionuclides (e.g., replace the damaged filter, seal the punched drum lid).

b. 6. Attachment B1-1a(3)(i)

- C The lid of the drum's 90-mil ~~rigid~~ poly liner shall contain a hole for venting to the drum ~~headspace~~. A representative sample cannot be collected ~~from the drum headspace~~ until the 90-mil ~~rigid~~ poly-liner has been vented. ~~to the drum~~ If the DAC for Scenario 1 is met, a sample may be collected from inside the 90-mil rigid poly liner. If the sample is collected by removing the drum lid, the sampling device shall form an airtight seal with the rigid poly liner to prevent the intrusion of outside air into the sample (using a sampling needle connected to the sampling head to pierce the rigid drum liner satisfies this requirement). If headspace-gas samples are collected ~~from the drum headspace~~ prior to venting the 90-mil ~~rigid~~ poly liner, the sample is not acceptable and a nonconformance report shall be prepared, submitted, and resolved. Nonconformance procedures are outlined in Permit Attachment B3.

b. 7. Attachment B1-1a(3)(ii)

- C The lid of the drum's 90-mil ~~rigid~~ poly liner shall contain a hole for venting to the drum ~~headspace~~. A representative sample cannot be collected ~~from the drum headspace~~ until the 90-mil ~~rigid~~ poly-liner has been vented. ~~to the drum~~ If the DAC for Scenario 1 is met, a sample may be collected from inside the 90-mil rigid poly liner drum liner. If headspace-gas samples are collected ~~from the drum headspace~~ prior to venting the 90-mil ~~rigid~~ poly liner, the sample is not acceptable and a nonconformance report shall be prepared, submitted, and resolved. Nonconformance procedures are outlined in Permit Attachment B3.

b. 8. Attachment B1-1a(3)(iii)

- C The lid of the drum's 90-mil ~~rigid~~ poly liner shall contain a hole for venting to the container ~~headspace~~. A representative sample cannot be collected ~~from the container headspace~~ until the 90-mil ~~rigid~~ poly-liner has been vented. ~~to the container~~ If the DAC for Scenario 1 is met, a sample may be collected from inside the 90-mil rigid poly liner. If headspace-gas samples are collected ~~from the container headspace~~ prior to venting the 90-mil ~~rigid~~ poly liner, the sample is not acceptable and a nonconformance report shall be prepared, submitted, and resolved. Nonconformance procedures are outlined in Permit Attachment B3. Note, as an option, the ~~same gas-tight seal~~ airtight fitting sampling apparatus may include a needle to penetrate the 90-mil rigid poly ~~rigid~~ liner.

b. 9. Attachment B1-1c(5)

To prevent cross contamination, the needle, ~~or~~ airtight ~~seal~~ fitting, adapters, and filter of the sampling heads shall be cleaned in accordance with the cleaning procedures described in EPA's Compendium Method TO-14 (EPA 1988). After sample collection, a sampling head shall be disposed of or cleaned in accordance with EPA's Compendium Method TO-14 (EPA 1988),

prior to reuse. As a further QC measure, the needle, or airtight seal fitting and filter, after cleaning, should be purged with zero air, nitrogen, or helium and capped for storage to prevent sample contamination by VOCs potentially present in ambient air.

b. 10 Attachment B1-6

BWXT, 2000, Determination of Drum Age Criteria and Prediction Factors Based on Packaging Configurations, INEEL/EXT-2000-01207, October 2000, Liekhus, K.J., S.M. Djordjevic, M. Devarakonda, and M.J. Connolly, Idaho National Engineering and Environmental Laboratory, Idaho Falls, Idaho.

b. 11. Attachment B1, Table B1-5

TABLE B1-5

HEADSPACE GAS DRUM AGE CRITERIA SAMPLING SCENARIOS

Scenario	Description
1	A. Unvented drums without rigid poly liners are sampled at the time venting through the drum lid B1. Unvented drums with unvented rigid poly liners are sampled through the rigid liner B2. Vented drums with unvented rigid poly liners are sampled through the rigid liner C. Unvented drums with vented rigid poly liners are sampled through the drum lid
2	Drums that have been packaged for a specified period of time sufficient to achieve equilibrium conditions (i.e., met the DAC for Scenario 1 drums) and then are vented, but not sampled at the time of venting.
3	Containers (i.e., drums, SWBs, and pipe components) that are initially packaged in a vented condition and sampled in the container headspace.

b. 12. Attachment B1, Table B1-6

TABLE B1-6

SCENARIO 1 DRUM AGE CRITERIA (in days) MATRIX

Summary Category Group	DAC (days)
S3000/S4000	127
S5000	53

b. 13. Attachment B1, Table B1-7

TABLE B1-7

SCENARIO 2 DRUM AGE CRITERIA (in days) MATRIX

	Summary Category Group S3000/S4000				Summary Category Group S5000			
Filter H ₂ Diffusivity ^a	Liner Lid Opening Diameter (in) ^b				Liner Lid Opening Diameter (in) ^b			
(mol/s/mod fraction)	0.30	0.375	0.75	1.0	0.30	0.375	0.75	1.0
1.9 x 10 ⁻⁶	36	30	23	22	29	22	13	12
3.7 x 10 ⁻⁶	30	25	19	18	25	20	12	11
3.7 x 10 ⁻⁵	13	11	11	11	7	6	6	4

^a The documented filter H₂ diffusivity must be greater than or equal to the listed value to use the DAC for the listed filter H₂ diffusivity (e.g., a container with a filter H₂ diffusivity of 4.2 x 10⁻⁶ must use a DAC for a filter with a 3.7 x 10⁻⁶ filter H₂ diffusivity).

^b The documented liner lid opening diameter must be greater than or equal to the listed value to use the DAC for the listed liner lid opening diameter (e.g., a container with a liner lid opening of 0.5 in must use a DAC for a liner lid opening of 0.375 in.)

b. 14. Attachment B1, Table B1-8

TABLE B1-8
SCENARIO 3 PACKAGING CONFIGURATIONS

Packaging Configuration Group	Covered S3000/S4000 Packaging Configurations	Covered S5000 Packaging Configurations
Packaging Configuration 1, drums ^a	<ul style="list-style-type: none"> No layers of confinement, filtered inner lid No inner bags, no liner bags (bounding case) 	<ul style="list-style-type: none"> No layers of confinement, filtered inner lid No inner bags, no liner bags (bounding case)

Packaging Configuration 2, drums ^a	<ul style="list-style-type: none"> • 1 inner bag • 1 filtered inner bag • 1 liner bag (bounding case) • 1 filtered liner bag 	<ul style="list-style-type: none"> • 1 inner bag • 1 filtered inner bag • 1 liner bag • 1 filtered liner bag • 1 inner bag, 1 liner bag • 1 filtered inner bag, 1 filtered liner bag • 2 inner bags • 2 filtered inner bags • 2 inner bags, 1 liner bag • 2 filtered inner bags, 1 filtered liner bag • 3 inner bags • 3 filtered inner bags • 3 filtered inner bags, 1 filtered liner bag • 3 inner bags, 1 liner bag (bounding case)
Packaging Configuration 3, drums ^a	<ul style="list-style-type: none"> • 1 inner bag, 1 liner bag • 1 filtered inner bag, 1 filtered liner bag • 2 inner bags • 2 filtered inner bags • 2 liner bags (bounding case) • 2 filtered liner bags 	<ul style="list-style-type: none"> • 2 liner bags • 2 filtered liner bags • 1 inner bag, 2 liner bags • 1 filtered inner bag, 2 filtered liner bags • 2 inner bags, 2 liner bags • 2 filtered inner bags, 2 filtered liner bags • 3 filtered inner bags, 2 filtered liner bags • 4 inner bags • 3 inner bags, 2 liner bags • 4 inner bags, 2 liner bags (bounding case)

Packaging Configuration 4, pipe components	<ul style="list-style-type: none"> • No layers of confinement inside a pipe component • 1 filtered inner bag, 1 filtered metal can inside a pipe component • 2 inner bags inside a pipe component • 2 filtered inner bags inside a pipe component • 2 filtered inner bags, 1 filtered metal can inside a pipe component • 2 inner bags, 1 filtered metal can inside a pipe component (bounding case) 	<ul style="list-style-type: none"> • No layers of confinement inside a pipe component • 1 filtered inner bag, 1 filtered metal can inside a pipe component • 2 inner bags inside a pipe component • 2 filtered inner bags inside a pipe component • 2 filtered inner bags, 1 filtered metal can inside a pipe component • 2 inner bags, 1 filtered metal can inside a pipe component (bounding case)
^a Packaging Configuration 5, Standard Waste Box	<ul style="list-style-type: none"> • No layers of confinement • 1 SWB liner bag (bounding case) 	<ul style="list-style-type: none"> • No layers of confinement • 1 SWB liner bag (bounding case)
^a Packaging Configuration 6, Standard Waste Box	<ul style="list-style-type: none"> • any combination of inner and/or liner bags that is less than or equal to 6 • 5 inner bags, 1 SWB liner bag (bounding case) 	<ul style="list-style-type: none"> • any combination of inner and/or liner bags that is less than or equal to 6 • 5 inner bags, 1 SWB liner bag (bounding case)

^a If a specific packaging configuration cannot be assigned based on the data collected during characterization and confirmation, a conservative default packaging configuration of 3 for drums and 6 for SWBs must be assigned provided the drums and SWBs do not contain pipe component packaging. If pipe components are present as packaging in the drums or SWBs, the pipe components must be sampled following the requirements for packaging configuration 4.

b. 15. Attachment B1, Table B1-9

TABLE B1-9
SCENARIO 3 DRUM AGE CRITERIA (in days) MATRIX FOR S5000 WASTE
BY PACKAGING CONFIGURATION GROUP

Packaging Configuration 1						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	131	95	37	24	4	4
3.7 x 10 ⁻⁶	111	85	36	24	4	4
3.7 x 10 ⁻⁵	28	28	23	19	4	4

Packaging Configuration 2						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	175	138	75	60	30	11
3.7 x 10 ⁻⁶	152	126	73	59	30	11
3.7 x 10 ⁻⁵	58	57	52	47	28	8

Packaging Configuration 3						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Liner Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	197	161	96	80	46	16
3.7 x 10 ⁻⁶	175	148 ^c	93	79	46	16
3.7 x 10 ⁻⁵	72	72	67	62	42	10

Packaging Configuration 4	
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Headspace Sample Taken Inside Pipe Component
$> 1.9 \times 10^{-6}$	152

Packaging Configuration 5	
Filter H ₂ Diffusivity ^{a, d} (mol/s/mol fraction)	Headspace Sample Taken Inside SWB
$> 7.4 \times 10^{-6}$	15

Packaging Configuration 6	
Filter H ₂ Diffusivity ^{a, d} (mol/s/mol fraction)	Headspace Sample Taken Inside SWB
$> 7.4 \times 10^{-6}$	56

- ^a The documented filter H₂ diffusivity must be greater than or equal to the listed value to use the DAC for the listed filter H₂ diffusivity (e.g., a container with a filter H₂ diffusivity of 4.2×10^{-6} must use a DAC for a filter with a 3.7×10^{-6} filter H₂ diffusivity).
- ^b The documented liner lid opening diameter must be greater than or equal to the listed value to use the DAC for the listed liner lid opening diameter (e.g., a container with a liner lid opening of 0.5 in must use a DAC for a liner lid opening of 0.375 in.)
- ^c A DAC of 142 days can be used for this case provided the packaging configuration does not exceed a total of 5 layers of confinement.
- ^d The filter H₂ diffusivity for SWBs is the sum of the diffusivities for all of the filters on the SWBS because an SWBS has more than 1 filter.

b. 16. Attachment B1, Table B1-10

TABLE B1-10
SCENARIO 3 DRUM AGE CRITERIA (in days) MATRIX FOR S3000 AND S4000 WASTE
BY PACKAGING CONFIGURATION GROUP

Packaging Configuration 1						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	131	95	37	24	4	4
3.7 x 10 ⁻⁶	111	85	36	24	4	4
3.7 x 10 ⁻⁵	28	28	23	19	4	4

Packaging Configuration 2						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	213	175	108	92	56	18
3.7 x 10 ⁻⁶	188	161	105	90	56	17
3.7 x 10 ⁻⁵	80	80	75	71	49	10

Packaging Configuration 3						
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Liner Lid Opening Diameter ^b				No Lid	No Liner
	0.3-inch Diameter Hole	0.375- inch Diameter Hole	0.75-inch Diameter Hole	1-inch Diameter Hole		
1.9 x 10 ⁻⁶	283	243	171	154	107	34
3.7 x 10 ⁻⁶	253	225	166	151	106	31
3.7 x 10 ⁻⁵	121	121	115	110	84	13

Packaging Configuration 4	
Filter H ₂ Diffusivity ^a (mol/s/mol fraction)	Headspace Sample Taken Inside Pipe Component
> 1.9 x 10 ⁻⁶	152

Packaging Configuration 5	
Filter H ₂ Diffusivity ^{a, c} (mol/s/mol fraction)	Headspace Sample Taken Inside SWBS
> 7.4 x 10 ⁻⁶	15

Packaging Configuration 6	
Filter H ₂ Diffusivity ^{a, c} (mol/s/mol fraction)	Headspace Sample Taken Inside SWBS
> 7.4 x 10 ⁻⁶	56

- ^a The documented filter H₂ diffusivity must be greater than or equal to the listed value to use the DAC for the listed filter H₂ diffusivity (e.g., a container with a filter H₂ diffusivity of 4.2 x 10⁻⁶ must use a DAC for a filter with a 3.7 x 10⁻⁶ filter H₂ diffusivity).
- ^b The documented liner lid opening diameter must be greater than or equal to the listed value to use the DAC for the listed liner lid opening diameter (e.g., a container with a liner lid opening of 0.5 in must use a DAC for a liner lid opening of 0.375 in.)
- ^c The filter H₂ diffusivity for SWBs is the sum of the diffusivities for all of the filters on the SWBS because an SWBS has more than 1 filter.

c. 1. Attachment B3, Section B3-11a

For each waste stream characterized, the Permittees shall require each Site Project Manager to determine if sufficient data have been collected to determine the following WAP-required waste parameters:

- ! Waste matrix code
- ! Waste material parameter weights
- ! If each waste container of waste contains TRU radioactive waste
- ! Mean concentrations, UCL_{90} for the mean concentrations, standard deviations, and the number of samples collected for each VOC in the headspace gas of waste containers in the waste stream (if applicable)
- ! The potential flammability of TRU waste headspace gases
- ! Mean concentrations, UCL_{90} for the mean concentrations, standard deviations, and number of samples collected for VOCs, SVOCs, and metals in the waste stream
- ! Whether the waste stream exhibits a toxicity characteristic (**TC**) under 40 CFR Part 261, Subpart C
- ! Whether the waste stream can be classified as hazardous or nonhazardous at the 90-percent confidence level
- ! Whether a sufficient number of waste containers have been visually examined (as a QC check on radiography) to determine with a reasonable level of certainty that the UCL_{90} for the misclassification rate is less than 14 percent (if applicable)
- ! Whether an appropriate packaging configuration and Drum Age Criteria (DAC) were applied and documented in the headspace gas sampling documentation.
- ! Whether all TICs were appropriately identified and reported in accordance with the requirements of Section B3-1 prior to submittal of a waste stream profile form for a waste stream or waste stream lot.
- ! Whether the overall completeness, comparability, and representativeness QAOs were met for each of the analytical and testing procedures as specified in Sections B3-2 through B3-9 prior to submittal of a waste stream profile form for a waste stream or waste stream lot.
- ! Whether the PRQLs for all analyses were met prior to submittal of a waste stream profile form for a waste stream or waste stream lot.

c. 2. Attachment B3, Table B3-12

TABLE B3-12
SAMPLING BATCH DATA REPORT CONTENTS

Required Information	Headspace Gas	Solid Sampling	Comment
Cross-reference of sampling equipment numbers with associated cleaning batch numbers	O	X	As applicable to the equipment used for the sampling. For disposable equipment, a reference to the lot and procurement records to support cleanliness is sufficient
Packaging Configuration	X		If Scenario 3 is used, the packaging configuration used in determining the DAC must be documented in the headspace gas sampling documentation.
Drum age	O		
Equilibration time	O		

d. 1. Attachment B6–Table B6-5

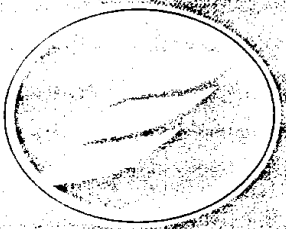
27	<p>Are procedures in place to ensure that all waste containers or randomly selected containers from waste streams that meet the conditions for reduced headspace gas sampling listed in Section B-3a(1)(i) and B-3a(1)(ii) will be allowed to equilibrate to sampling room temperature for 72 hours prior to sampling (18°C or higher) and that the drum ages specified in accordance with Section B1-1a of 142 days for debris waste and 225 days for homogeneous (S3000) and soil/gravel (S4000) wastes are met? Are procedures in place to ensure that packaging configuration, equilibrium time and drum ages are documented? (Section B1-1a)</p>
32	<p>Are procedures, processes, and equipment in place to ensure that the following manifold sampling procedures are implemented:</p> <ul style="list-style-type: none"> A. The sampling equipment is leak checked and cleaned upon first use and as needed B. The manifold and sample canisters are evacuated to 0.1 mm Hg prior to sample collection C. Cleaned and evacuated sample canisters are attached to the evacuated manifold before the manifold inlet valve is opened D. The manifold inlet valve is attached to a changeable filter connected to different sampling heads that are capable of punching through the metal lid of the drums with an airtight seal, or penetrating a carbon composite filter with an airtight seal, penetrating the rigid poly liner with an airtight seal (using a sampling needle connected to the sampling head to pierce the rigid drum liner satisfies this requirement), or providing an airtight fitting when sampling through the existing filter vent hole. E. Field blanks are collected using samples of room air collected in the sampling area in the immediate vicinity of the waste container <i>(Note: field blanks for SUMMA® canisters are collected directly into the canister)</i> F. Manifold equipped with purge assembly that allows QC samples to be collected through all sampling components that affect compliance with QAOs G. The manifold internal volume is calculated and documented in a field logbook H. The volume of headspace gas collected as calculated by the canister volume and internal manifold volume is less than 10 percent of the available headspace volume when a volume estimate is available <p>(Section B1-1a(1))</p>
37	<p>Are procedures, processes, and equipment in place to ensure that the following operating conditions are in place for direct canister sampling:</p> <ul style="list-style-type: none"> I. Canisters are evacuated to 0.1 mm Hg prior to use and attached to a changeable filter connected to the sampling head

- J. Sampling heads are capable of punching through the metal lid of the drums **with an airtight seal, or** penetrating a carbon composite filter **with an airtight seal, penetrating the rigid poly liner with an airtight seal** (using a sampling needle connected to the sampling head to pierce the rigid drum liner satisfies this requirement), **or providing an airtight fitting when sampling through the existing filter vent hole.**
- K. Field duplicates are collected in the same manner and at the same time as the original sample
- L. Field blanks shall be samples of room air collected in the immediate vicinity of the waste drum sampling area prior to removal of the drum lid
- M. Equipment blanks and field reference standards shall be collected using a purge assembly equivalent to the standard side of the manifold
- N. Less than 10 percent of the headspace is withdrawn when a headspace estimate is available
(Note: The volume withdrawn is the canister volume and the internal volume of the sampling head)
- O. Each sample canister is equipped with a pressure/vacuum gauge capable of indicating leaks and sample collection volumes. The gauge shall be helium-leak tested to 1.5×10^{-7} standard cc/s, have all stainless steel construction, and be capable of tolerating temperatures to 125°C
- P. SUMMA® canisters or equivalent are used to collect samples

(Section B1-1a(2))

Attachment B

**Determination of Drum Age Criteria and Prediction Factors Based on Packaging
Configurations INEEL/EXT-2000-01207**



Determination of Drum Age Criteria and Prediction Factors Based on Packaging Configurations

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Determination of Drum Age Criteria and Prediction Factors Based on Packaging Configurations

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SUMMARY

The drum age criterion (DAC) is the time required to pass after drum closure, or after drum closure and drum venting, before a headspace gas sample can be collected. In an earlier report, drum age criteria were defined for two waste drum configurations under three different drum venting and sampling scenarios. The highest DAC values reported for each waste drum configuration are currently being used to define the minimum period of time required after drum venting before headspace gas sampling can occur. The application of only two specific DAC values to all waste drums require that sufficiently conservative assumptions were made regarding the waste drum configurations to ensure that the DACs represent the worst cases. Since the selection of the two DACs, other more restrictive waste packaging configurations have also been identified. As a result, there is currently no appropriate minimum waiting period identified for these waste drums. Furthermore, the availability of additional DACs for packaging configurations and sampling scenarios that better represent actual waste drums would result in shorter holding times between drum closure and drum gas sampling. In this report, additional DAC values are calculated for different venting and sampling scenarios as well as for a wider variety of waste drum packaging configurations. Model parameters and assumptions used in determining the DACs are documented.

Drum venting and sampling scenarios are defined by the time elapsed after drum closure and drum venting. Drum age criteria are defined for three unique drum venting and sampling scenarios:

Scenario 1: The drum liner headspace can be sampled at the time of venting if the waste drum was unvented for a period of time exceeding DAC_1 .

The drum age criterion DAC_1 is defined as the time for a representative VOC to reach a concentration of at least 90% of its equilibrium concentration before drum venting. The drum age criterion DAC_1 for bounding waste packaging configuration used for Waste Types I and IV or S3000 (Homogeneous Solids) and S4000 (Soil/Gravel) was determined to be 127 days and for that used for Waste Types II and III or S5000 (Debris) waste was 53 days.

Scenario 2: If a waste drum is not vented until the DAC_1 has been exceeded, the drum headspace can be sampled in a vented drum after DAC_2 has been exceeded.

The drum age criterion DAC_2 is defined as the time for a representative VOC to reach a concentration of at least 90% of its steady-state concentration after venting a waste drum that was unvented for at least DAC_1 . DAC_2 values are calculated for the two waste configurations under Scenario 1 with four different opening sizes in the punctured drum liner lid and three different drum filter vents. DAC_2 values range from 4 to 36 days. In this scenario, a single DAC is not to be defined by adding DAC_1 and DAC_2 values. DAC_1 and DAC_2 are separate drum age criteria, which must both be met.

Scenario 3: If DAC_1 is not met when the drum is vented, the drum headspace can be sampled after the DAC_3 has been exceeded. For newly generated drums that were vented at the time of generation, the drum headspace can also be sampled after the DAC_3 has been exceeded.

The drum age criterion DAC_3 is defined as the time for a representative VOC to reach a concentration within at least 10% of its steady-state concentration. DAC_3 values are calculated for the two category waste types and for each of the three different packaging configurations representing

different layers of polymer bags with five different opening sizes in the drum liner lid as well as the case of no rigid liner inside the drum and three different drum filter vents. Nearly 100 DAC_3 values are calculated and range between 4 and 283 days. A considerable number of the DAC_3 values are less than the current DAC values of 142 and 225 days. DAC_3 values were also calculated for packaging configurations that included standard waste boxes (SWBs) and pipe components (sampling inside the pipe component headspace). The DAC_3 values calculated for the SWBs and the pipe component were intended to conservatively bound the wide range of likely packaging configurations. The methodology used to determine prediction factors that relate the measured VOC concentration in the container headspace to the VOC concentration in the innermost confinement layer is also presented.

The concept of a DAC can be impractical for waste containers with a highly restrictive packaging configuration, which may require an extremely long time to achieve steady state. This can be expected of waste drums containing metal cans and pipe overpacks. "Pipe Overpack" is a vented 55-gallon drum containing a pipe component. For pipe overpacks and drums containing metal cans, a more time-efficient methodology is outlined to evaluate the VOC concentration in the drum headspace after a given period of time and relating it to the steady-state VOC headspace concentration. A VOC concentration multiplier is defined as the ratio of 90% of the steady-state VOC concentration in the sampling headspace divided by the VOC headspace concentration at a given time. The use of these multipliers and steady-state prediction factors can be used to relate the measured VOC concentration in the drum headspace to the steady-state VOC concentration within the innermost layer of confinement. The VOC concentration multipliers were calculated using the same equations that are used to calculate DAC s. Multipliers for three bounding packaging configurations involving pipe overpack and metal cans with two possible filter vents as well as two different filter vents for the waste drum were calculated as a function of drum age. Lower multipliers for older drums take credit for the higher drum headspace concentration that can be expected with increasing drum age.

The calculation of DAC s for three common drum venting and sampling scenarios provides more realistic waiting periods for sampling than current DAC s. For example, DAC_2 values indicate that unvented drums that have been in storage in excess of DAC_1 values (53 or 127 days) can be realistically sampled in anywhere from 4 to 36 days depending on the liner lid opening and drum filter vent installed at the time of venting. This could provide relief (compared to current DAC s of 142 or 225 days) of over 200 days in some cases in reducing the waiting time required before sampling the drum headspace. The DAC values calculated for the SWBs and the pipe component were intended to conservatively bound the wide range of likely packaging configurations. In the case of the pipe component, the DAC is the waiting time required before sampling directly from the pipe component headspace. This DAC does not apply to pipe overpacks for which VOC concentration multipliers can be used.

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Determination of Drum Age Criteria and Prediction Factors Based on Packaging Configurations

1. BACKGROUND

Transuranic (TRU) waste drums must meet a minimum age criterion before a gas sample collected from the waste drum is considered representative of the total drum headspace. The drum age criterion (DAC) is the time required to pass after drum closure, or after drum closure and drum venting, before a headspace gas sample can be collected. The manner in which the DACs are defined is dependent on when drum venting and headspace gas sampling occur (Connolly et al., 1998). Drum age criteria were defined for two waste drum configurations under three different drum venting and sampling scenarios. The waste drum configurations were selected to represent the worst cases of common packaging configurations. In each combination of waste drum configuration and sampling scenario, the DAC was defined as the time necessary for the concentration of a representative volatile organic compound (VOC) in the sampling headspace to be within at least 10% of its final steady-state or equilibrium concentration (Connolly et al., 1998). From these three sampling scenarios, the highest DAC values reported for each waste drum configuration were used to define the minimum period of time required before headspace gas sampling can occur.

The DAC values are a strong function of the waste packaging configuration. Packaging parameters include the number of layers of polymer bags surrounding the waste, the thickness and surface area of the polymer bags, the presence or absence of a rigid polymer drum liner and its characteristics, and the gas diffusion characteristic of the drum filter vent. The application of only two specific DAC values to all waste drums require that sufficiently conservative assumptions were made regarding the waste drum configurations to ensure that the DACs represent the worst cases. Since the generation of the two DACs, other more restrictive waste packaging configurations have been identified. As a result, there is currently no appropriate minimum waiting period identified for these waste drums. Furthermore, the availability of additional DACs for packaging configurations and sampling scenarios that better represent actual waste drums would result in shorter holding times between drum closure and drum gas sampling.

2. PURPOSE AND SCOPE

Additional DAC values are calculated for different venting and sampling scenarios as well as for a wider variety of waste drum packaging configurations. Model parameters and assumptions used in determining the DACs are documented. The concept of a VOC concentration multiplier is described and a time-efficient methodology is outlined, which relates the measured VOC drum headspace concentration of waste containers with a highly restrictive packaging configuration to its steady-state VOC headspace concentration. Equations defining prediction factors relating the measured VOC concentration to the VOC concentration within the innermost layer of confinement are detailed.

3. PREVIOUS DAC CALCULATIONS

The current limits for DACs (Connolly et al., 1998) are categorized based on the waste form and packaging as follows:

Waste Types I and IV, Solidified Inorganics and Solidified Organics. These wastes were assumed to be packaged in two drum liner bags, in a rigid drum liner with a 0.375-inch diameter hole, in a 55-gallon drum fitted with a filter with a hydrogen diffusivity of $4.2\text{E-}06$ moles/second/mole fraction.

Waste Types II and III, Solid Inorganics and Solid Organics. These wastes were assumed to be packaged in three inner bags and two drum liner bags, in a rigid drum liner with a 0.375-inch diameter hole, in a 55-gallon drum fitted with a filter with a hydrogen diffusivity of $4.2\text{E-}06$ moles/second/mole fraction.

The drum age criteria were determined for these waste packaging configurations and the following venting and sampling scenarios (Connolly et al., 1998):

1. Containers that are unvented and are sampled under the rigid liners at the time of venting.

The drum age criterion is the time required for a representative VOC to achieve a concentration of at least 90% of its equilibrium concentration in the drum liner headspace before venting. A representative VOC is a compound that is significant and yields the highest DAC (Connolly et al., 1998). For drums containing Waste Types I/IV drums, a DAC of 127 days was calculated. For drums containing Waste Types II/III, a DAC of 48 days was calculated.

2. Containers that have been packaged for a specified period of time sufficient to achieve equilibrium conditions and then are vented.

In this case, the total waiting time before headspace sampling is the time after drum closure to achieve equilibrium conditions and the time between venting and sampling for the drum headspace concentration of a representative VOC to be within at least 10% of its steady-state concentration. In the case where complete equilibrium had been achieved before drum venting, the DACs after venting were calculated to be 22 and 18 days for Waste Types I/IV and Waste Types II/III, respectively.

3. Containers that are initially packaged in a vented condition.

The drum age criterion is defined as the time for a representative VOC to reach a concentration that is at least 90% of its steady-state concentration in the drum headspace. For drums containing Waste Types I/IV drums, a DAC of 225 days was calculated. For drums containing Waste Types II/III, a DAC of 142 days was calculated. These DACs were the highest values calculated for the three venting and sampling scenarios.

The DAC for each case was determined using a computer program that solved a series of differential equations describing the VOC transport phenomena within the waste drum. Model input parameters include the physical properties of the VOC, the initial concentration profile in the drum, physical dimensions of each layer of confinement (thickness, surface area, void volume), and the hydrogen diffusion characteristic of the drum filter vent. Other model input parameters and model assumptions are described in Connolly et al. (1998).

4. DEFINING BOUNDING DRUM AGE CRITERIA

The past work (Connolly et al., 1998) determining DACs for specific waste packaging configurations as well as a sensitivity analysis to identify the most important parameters that influence the calculated DAC (Liekhus et al. 1999) serves as the foundation for calculating DACs for different venting and sampling scenarios as well as for a wider variety of waste drum packaging configurations. The sensitivity analysis indicated that filter vent characteristic, opening size in liner lid, as well as the presence or absence of the liner itself had a significant influence on the DAC values. Variables such as total bag thickness and the presence or absence of bag filters had little influence.

Drum age criteria are defined for three unique drum venting and sampling scenarios. These drum venting and sampling scenarios are defined by the time elapsed after drum closure and drum venting:

t_1 – time (days) elapsed after drum closure until drum venting

t_2 – time (days) elapsed after drum venting

Scenario 1: The drum liner headspace can be sampled at the time of venting if t_1 is greater than DAC_1 .

The drum age criterion DAC_1 is defined as the time for a representative VOC to reach a concentration of at least 90% of its equilibrium concentration before drum venting. Two waste drum configurations are considered:

1. Drum liner with two polymer drum liners bags

This packaging configuration is assumed for S3000 (Homogeneous solids) and S4000 (Soil/gravel) wastes. This corresponds to Waste Types I and IV (Connolly et al., 1998).

2. Drum liner with four polymer inner bags and two polymer drum liners bags

This packaging configuration is assumed for S5000 (Debris) waste. This configuration is similar to that assumed for Waste Types II and III (Connolly et al., 1998) except that the assumption of six polymer bags is considered to represent the bounding case.

The DAC_1 values for these two configurations are listed in Table 1. The model input parameters used to calculate these results are listed in Appendix A.

Table 1. DAC_1 values for S3000/S4000 (Waste Types I and IV) and S5000 (Waste Types II and III) waste.

Waste Type	DAC_1 (days)
S3000/S4000 (Waste Types I and IV)	127
S5000 (Waste Types II and III)	53

Scenario 2: The drum headspace can be sampled in a vented drum if t_1 is greater than DAC_1 , and t_2 is greater than DAC_2 .

The drum age criterion DAC_2 is defined as the time for a representative VOC to reach a headspace concentration within at least 10% of its steady-state concentration after venting a waste drum that was unvented for at least DAC_1 . DAC_2 values are calculated for the two waste configurations under Scenario 1 with four different opening sizes in the punctured drum liner lid and three different drum filter vents. The DAC_2 values are listed in Table 2. The model input parameters used to calculate these results are listed in Appendix A.

A single DAC is not defined by adding DAC_1 and DAC_2 . DAC_1 and DAC_2 are separate drum age criteria which must both be met under this scenario. If not, scenario 3 should be used.

Table 2. DAC₂ values for S3000/S4000 (Waste Types I and IV) and S5000 (Waste Types II and III) waste.

	S3000/S4000 (Waste Types I and IV)				S5000 (Waste Types II and III)			
Drum Filter Vent	Liner Lid Opening Diameter (in)				Liner Lid Opening Diameter (in)			
D* _{H2} (mol/s/mol fr)	0.30	0.375	0.75	1.0	0.30	0.375	0.75	1.0
1.9 x 10 ⁻⁶	36	30	23	22	29	22	13	12
3.7 x 10 ⁻⁶	30	25	19	18	25	20	12	11
3.7 x 10 ⁻⁵	13	11	11	11	7	6	6	4

Scenario 3: If t₁ is less than DAC₁ when the drum is vented, the drum headspace can be sampled when t₂ is greater than DAC₃. Also for newly generated drums that were vented at the time of generation, the drum headspace can be sampled after the DAC₃ has been exceeded.

The drum age criterion DAC₃ is defined as the time for a representative VOC to reach a headspace concentration of at least 90% of its steady-state concentration. DAC₃ values are calculated for the two categories of waste types each with three different packaging configurations representing different layers of polymer bags with five different opening sizes in the drum liner lid as well as the case of no rigid liner inside the drum and three different drum filter vents. The model input parameters used to calculate these results are listed in Appendix A. The DAC₃ values are listed in Tables 3 and 4.

Table 3. DAC₃ values for S3000/S4000 (Waste Types I and IV) waste packaging configurations.

Packaging Configuration	Filter Vent H ₂ Diffusion Characteristic (mol/s/mol fr.)	Liner Lid Opening					
		0.30-in diameter	0.375-in diameter	0.75-in diameter	1-in diameter	No Lid	
No bags	1.9 x 10 ⁻⁶	131	95	37	24	4	4 ^a
No bags	3.7 x 10 ⁻⁶	111	85	36	24	4	4 ^a
No bags	3.7 x 10 ⁻⁵	28	28	23	19	4	4 ^a
One liner bag	1.9 x 10 ⁻⁶	213	175	108	92	56	18
One liner bag	3.7 x 10 ⁻⁶	188	161	105	90	56	17
One liner bag	3.7 x 10 ⁻⁵	80	80	75	71	49	10
Two liner bags	1.9 x 10 ⁻⁶	283	243	171	154	107	34
Two liner bags	3.7 x 10 ⁻⁶	253	225	166	151	106	31
Two liner bags	3.7 x 10 ⁻⁵	121	121	115	110	84	13

^a - DACs not calculated and assumed to be same as case of liner with no lid.

Table 4. DAC₃ values for S5000 (Waste Types II and III) waste packaging configurations.

Packaging Configuration	Filter Vent H ₂ Diffusion Characteristic (mol/s/mol fr.)	Liner Lid Opening					No Liner
		0.30-in diameter	0.375-in diameter	0.75-in diameter	1-in diameter	No Lid	
No bags	1.9×10^{-6}	131	95	37	24	4	4 ^a
No bags	3.7×10^{-6}	111	85	36	24	4	4 ^a
No bags	3.7×10^{-5}	28	28	23	19	4	4 ^a
3 IBs, 1 LB	1.9×10^{-6}	175	138	75	60	30	11
3 IBs, 1 LB	3.7×10^{-6}	152	126 ^b	73	59	30	11
3 IBs, 1 LB	3.7×10^{-5}	58	57	52	47	28	8
4 IBs, 2 LBs	1.9×10^{-6}	197	161	96	80	46	16
4 IBs, 2 LBs	3.7×10^{-6}	175	148 ^b	93	79	46	16
4 IBs, 2 LBs	3.7×10^{-5}	72	72	67	62	42	10

IB=inner bag, LB=liner bag.

^a DACs not calculated and assumed to be same as case of liner with no lid.

^b DAC=142 days (Connolly et al., 1998) based on packaging configuration on 3 IBs, 2LBs, filter vent= 4.2×10^{-6} mol/s/mol fr.

DAC₃ values were also calculated for packaging configurations other than waste drums. These configurations included standard waste boxes (SWBs) and pipe components. Two SWB configurations and one pipe component configuration intended to serve as a bounding case were considered. The SWB packing configuration 1 assumes waste wrapped inside 5 inner bags is placed in a single liner bag in a SWB. The SWB packing configuration 2 assumes waste is directly placed inside a single liner bag in a SWB. The SWB has two or more filter vents with a total hydrogen diffusion characteristic of 7.4×10^{-6} mol/s/mol fr. The packaging configuration of 2 polymer bags surrounding waste in a vented metal can inside a vented pipe component is intended to represent the bounding case for waste packaged inside a pipe component. The sampling in this case is required inside the headspace of the pipe component itself. In the case of the pipe component the model input parameters used to calculate these DAC₃ values are listed in Appendix A. The DACs for these packaging configurations are listed in Table 5.

Table 5. DAC₃ values for special packaging configuration.

Waste Packaging Configuration	DAC (days) ^a
SWB (5 layers inner bags, one SWB liner bag)	56
SWB (one SWB liner bag)	15
Pipe component (2 inner bags, vented metal can)	152

^a Applies to sampling directly from SWB or pipe component.

5. VOC CONCENTRATION MULTIPLIERS

The concept of a DAC (time to achieve 90% of steady-state concentration) for sampling vented waste drum headspace can be impractical for waste containers with a highly restrictive packaging configuration which may require an extremely long time to achieve steady state. This can be expected of waste drum containing metal cans and pipe overpacks. "Pipe Overpack" is a vented 55-gallon drum containing a pipe component. For these cases, a more time-efficient methodology is outlined to evaluate the VOC concentration in the drum headspace after a given period of time and relating it to the steady-state VOC headspace concentration.

A VOC concentration multiplier is defined as the ratio of 90% of the steady-state VOC concentration in the sampling headspace divided by the VOC headspace concentration at a given time. This ratio can be calculated using the same differential equations as are in the computer program (VDRUM.FOR) that determines the DACs. The software program was revised to allow for a greater number of layers of confinement, multiple mechanisms for VOC transport to occur simultaneously across each layer of confinement, and greater flexibility in program output. The revised computer code, VDRUM2.FOR, was created, verified, and validated (Liekhus and Chambers, 2000). The VOC concentration multipliers were calculated as a function of the waste drum age for three bounding packaging configurations involving vented pipe components and metal cans with two possible filter vents as well as two different filter vents for the waste drum using the code VDRUM2.FOR. Lower multipliers for older drums take credit for the higher drum headspace concentration that can be expected with increasing drum age. The VOC concentration multipliers associated with vented drum headspace sampling of drums containing vented pipe components or vented metal cans are tabulated in Tables 6 through 9. The model input parameters used to calculate the VOC concentration multipliers are listed in Appendix B.

Table 6. VOC Concentration Multipliers ($D^*_{H_2, drum} = D^*_{H_2, can} = 1.9 \times 10^{-6} \text{ mol/s/mol fr.}$) as a function of time (days) after venting.

		Waste Drum Packaging Configuration											
		2IB-PC-DL-DF*				3IB-FC-2LB-DL-DF*				2IB-FC-PC-DL-DF*			
	Days	75	150	300	600	75	150	300	600	75	150	300	600
Volatile Organic Compound													
carbon tetrachloride		5.5	2.9	1.7	1.1	7.8	3.9	2.2	1.4	14.9	5.4	2.4	1.4
cyclohexane		6.6	2.6	1.4	1.0	11.6	4.2	1.9	1.2	10.5	3.8	1.8	1.1
methanol		2.8	1.8	1.2	1.0	4.0	2.4	1.5	1.1	5.3	2.6	1.5	1.1
dichloromethane		3.2	1.8	1.2	1.0	4.5	2.5	1.5	1.1	7.5	3.1	1.6	1.1
toluene		22.7	11.5	6.0	3.2	32.6	15.5	7.7	4.0	64.9	22.9	9.5	4.5
trichloroethane		4.3	2.3	1.4	1.0	6.2	3.2	1.8	1.2	11.2	4.2	2.0	1.2
trichloroethylene		11.2	5.7	3.1	1.8	15.4	7.6	4.0	2.2	31.2	11.1	4.8	2.4
Freon-13		4.5	2.1	1.3	1.0	6.7	3.1	1.7	1.1	9.9	3.6	1.7	1.1
p-xylene		45.1	22.8	11.7	6.1	74.4	33.2	15.7	7.8	136.9	47.6	19.2	8.8
acetone		3.1	1.8	1.2	1.0	4.5	2.4	1.5	1.1	7.4	2.9	1.5	1.0
butanol		4.8	2.6	1.6	1.1	6.7	3.5	2.0	1.3	12.7	4.8	2.2	1.3
chloroform		3.5	2.0	1.3	1.0	5.0	2.7	1.6	1.1	8.9	3.5	1.7	1.1
1,1-dichloroethene		3.3	1.8	1.2	1.0	4.8	2.5	1.5	1.1	7.8	3.0	1.5	1.0
methyl ethyl ketone		4.1	2.2	1.4	1.0	5.8	3.0	1.8	1.2	10.3	3.9	1.9	1.2
methyl isobutyl ketone		7.1	3.6	2.0	1.3	10.1	5.0	2.7	1.6	19.6	6.9	3.0	1.6
1,1,2,2-tetrachloroethane		17.0	8.8	4.6	2.6	23.8	11.6	5.9	3.1	49.4	17.5	7.3	3.6
tetrachloroethene		9.1	4.7	2.6	1.6	12.5	6.3	3.3	1.9	26.4	9.4	4.0	2.1
benzene		4.2	2.3	1.4	1.0	5.9	3.1	1.8	1.2	10.7	4.1	2.0	1.2
bromoform		20.1	10.3	5.4	3.0	28.5	13.7	6.9	3.6	57.2	20.4	8.6	4.1
chlorobenzene		10.2	5.3	2.9	1.7	14.1	7.0	3.7	2.1	29.7	10.6	4.5	2.3
1,1-dichloroethane		3.3	1.9	1.2	1.0	4.8	2.6	1.5	1.1	8.3	3.3	1.6	1.1
1,2-dichloroethane		4.5	2.5	1.5	1.1	6.2	3.3	1.9	1.2	11.7	4.5	2.1	1.3
cis-1,2-dichloroethene		3.4	1.9	1.2	1.0	4.8	2.6	1.5	1.1	8.4	3.3	1.7	1.1
ethylbenzene		10.8	5.4	2.9	1.7	15.1	7.4	3.9	2.2	31.5	11.0	4.6	2.3
ethyl ether		4.1	2.0	1.2	1.0	6.1	2.9	1.6	1.1	8.4	3.2	1.6	1.1
1,3,5-trimethylbenzene		18.1	9.0	4.7	2.6	26.1	12.4	6.2	3.3	55.9	19.0	7.6	3.6
1,2,4-trimethylbenzene		20.6	10.3	5.3	2.9	30.0	14.1	7.0	3.7	64.3	21.8	8.7	4.1
o-xylene		12.4	6.3	3.4	1.9	17.4	8.5	4.4	2.4	36.9	12.9	5.3	2.6
m-xylene		10.8	5.5	2.9	1.7	15.2	7.4	3.9	2.2	31.8	11.1	4.6	2.3

*IB-inner bag; PC-vented pipe component; FC-filtered can; LB-drum liner bag; DL-drum liner; DF-drum filter vent

Table 7. VOC Concentration Multipliers ($D^*_{H_2, \text{drum}} = 1.9\text{e-}6 \text{ mol/s/mol fr.}$; $D^*_{H_2, \text{can}} = 3.7\text{e-}6 \text{ mol/s/mol fr.}$) as a function of time (days) after venting.

	Days	Waste Drum Packaging Configuration											
		2IB-PC-DL-DF*				3IB-FC-2LB-DL-DF*				2IB-FC-PC-DL-DF*			
		75	150	300	600	75	150	300	600	75	150	300	600
Volatile Organic Compound													
carbon tetrachloride		4.1	2.2	1.4	1.0	6.2	3.2	1.8	1.2	8.5	3.6	1.9	1.2
cyclohexane		5.0	2.2	1.3	1.0	11.1	4.1	1.9	1.2	7.1	2.9	1.6	1.1
methanol		2.3	1.5	1.1	1.0	3.5	2.2	1.4	1.0	3.6	2.1	1.3	1.0
dichloromethane		2.4	1.5	1.1	1.0	3.6	2.0	1.3	1.0	4.6	2.2	1.3	1.0
toluene		15.8	8.1	4.3	2.4	23.5	11.2	5.7	3.0	35.3	14.4	6.7	3.4
trichloroethane		3.2	1.8	1.2	1.0	5.1	2.7	1.6	1.1	6.6	2.9	1.6	1.1
trichloroethylene		7.9	4.1	2.3	1.4	11.2	5.6	3.0	1.7	17.2	7.1	3.5	1.9
Freon-13		3.5	1.8	1.1	1.0	6.1	2.9	1.6	1.1	6.3	2.7	1.5	1.0
p-xylene		31.1	15.8	8.2	4.3	52.7	23.5	11.2	5.7	72.8	29.2	13.3	6.5
acetone		2.4	1.4	1.0	1.0	3.8	2.1	1.3	1.0	4.6	2.1	1.3	1.0
butanol		3.5	2.0	1.3	1.0	5.2	2.8	1.6	1.1	7.3	3.2	1.7	1.1
chloroform		2.6	1.6	1.1	1.0	3.9	2.2	1.4	1.0	5.3	2.4	1.4	1.0
1,1-dichloroethene		2.5	1.5	1.0	1.0	4.1	2.2	1.4	1.0	4.8	2.2	1.3	1.0
methyl ethyl ketone		3.1	1.7	1.2	1.0	4.8	2.5	1.5	1.1	6.1	2.7	1.5	1.1
methyl isobutyl ketone		5.3	2.7	1.6	1.1	8.3	4.1	2.3	1.4	11.2	4.6	2.3	1.4
1,1,2,2-tetrachloroethane		11.8	6.1	3.3	1.9	16.5	8.1	4.2	2.3	26.6	11.0	5.2	2.7
tetrachloroethene		6.4	3.4	2.0	1.3	9.1	4.6	2.5	1.5	14.4	6.0	2.9	1.7
benzene		3.1	1.8	1.2	1.0	4.6	2.5	1.5	1.1	6.3	2.8	1.6	1.1
bromoform		13.8	7.2	3.8	2.2	19.6	9.5	4.9	2.6	30.9	12.8	6.0	3.1
chlorobenzene		7.2	3.8	2.2	1.4	10.3	5.2	2.8	1.7	16.2	6.7	3.3	1.8
1,1-dichloroethane		2.5	1.5	1.1	1.0	3.9	2.1	1.3	1.0	5.0	2.3	1.3	1.0
1,2-dichloroethane		3.3	1.9	1.2	1.0	4.7	2.5	1.5	1.1	6.7	3.0	1.7	1.1
cis-1,2-dichloroethene		2.5	1.5	1.1	1.0	3.8	2.1	1.3	1.0	5.0	2.3	1.4	1.0
ethylbenzene		7.7	4.0	2.2	1.4	11.5	5.7	3.0	1.8	17.3	7.0	3.3	1.9
ethyl ether		3.3	1.7	1.1	1.0	5.6	2.7	1.5	1.1	5.5	2.4	1.4	1.0
1,3,5-trimethylbenzene		12.8	6.5	3.4	2.0	19.7	9.4	4.8	2.6	30.1	11.8	5.4	2.8
1,2,4-trimethylbenzene		14.5	7.3	3.9	2.2	22.3	10.6	5.3	2.9	34.3	13.4	6.1	3.1
o-xylene		8.8	4.6	2.5	1.5	13.0	6.4	3.4	1.9	20.0	8.1	3.8	2.1
m-xylene		7.7	4.0	2.2	1.4	11.6	5.7	3.0	1.8	17.4	7.0	3.4	1.9

*IB-Inner bag; PC-vented pipe component; FC-filtered can; LB-drum liner bag; DL-drum liner; DF-drum filter vent

Table 8. VOC Concentration Multipliers ($D^*_{H_2, drum} = 3.7 \times 10^{-6}$ mol/s/mol fr.; $D^*_{H_2, can} = 1.9 \times 10^{-6}$ mol/s/mol fr.) as a function of time (days) after venting.

Volatile Organic Compound	Days	Waste Drum Packaging Configuration											
		2IB-PC-DL-DF*				3IB-FC-2LB-DL-DF*				2IB-FC-PC-DL-DF*			
		75	150	300	600	75	150	300	600	75	150	300	600
carbon tetrachloride		3.9	2.1	1.3	1.0	5.3	2.8	1.6	1.1	9.3	3.5	1.7	1.1
cyclohexane		4.3	1.9	1.1	1.0	6.9	2.6	1.4	1.0	6.4	2.5	1.3	1.0
methanol		2.1	1.4	1.1	1.0	2.8	1.8	1.2	1.0	3.5	1.9	1.2	1.0
dichloromethane		2.3	1.4	1.0	1.0	3.2	1.8	1.2	1.0	4.8	2.1	1.2	1.0
toluene		15.5	7.9	4.2	2.3	22.3	10.7	5.4	2.9	40.0	14.2	6.0	3.0
trichloroethane		3.0	1.7	1.1	1.0	4.2	2.3	1.4	1.0	7.1	2.8	1.4	1.0
trichloroethylene		7.7	4.0	2.3	1.4	10.6	5.3	2.8	1.7	19.4	7.0	3.1	1.7
Freon-13		3.2	1.6	1.1	1.0	4.3	2.1	1.3	1.0	6.2	2.4	1.3	1.0
p-xylene		30.7	15.6	8.0	4.3	50.7	22.7	10.9	5.5	84.1	29.4	11.9	5.6
acetone		2.3	1.4	1.0	1.0	3.1	1.8	1.2	1.0	4.8	2.0	1.2	1.0
butanol		3.4	1.9	1.2	1.0	4.7	2.5	1.5	1.1	8.0	3.1	1.6	1.1
chloroform		2.5	1.5	1.1	1.0	3.5	2.0	1.3	1.0	5.7	2.4	1.3	1.0
1,1-dichloroethane		2.3	1.4	1.0	1.0	3.3	1.8	1.2	1.0	5.0	2.1	1.2	1.0
methyl ethyl ketone		2.9	1.6	1.1	1.0	4.0	2.2	1.4	1.0	6.5	2.6	1.4	1.0
methyl isobutyl ketone		4.9	2.6	1.5	1.1	6.8	3.4	1.9	1.2	12.2	4.4	2.0	1.2
1,1,2,2-tetrachloroethane		11.7	6.1	3.3	1.9	16.5	8.1	4.2	2.3	30.6	11.0	4.7	2.4
tetrachloroethene		6.3	3.4	1.9	1.3	8.6	4.4	2.4	1.5	16.4	6.0	2.7	1.5
benzene		3.0	1.7	1.2	1.0	4.1	2.2	1.4	1.0	6.8	2.7	1.4	1.0
bromoform		13.8	7.2	3.8	2.2	19.7	9.6	4.9	2.7	35.4	12.7	5.4	2.7
chlorobenzene		7.1	3.7	2.1	1.3	9.7	4.9	2.7	1.6	18.4	6.7	3.0	1.6
1,1-dichloroethane		2.4	1.4	1.0	1.0	3.3	1.9	1.2	1.0	5.4	2.2	1.2	1.0
1,2-dichloroethane		3.2	1.8	1.2	1.0	4.4	2.4	1.5	1.1	7.4	3.0	1.5	1.0
cis-1,2-dichloroethene		2.4	1.5	1.1	1.0	3.4	1.9	1.2	1.0	5.4	2.3	1.3	1.0
ethylbenzene		7.4	3.8	2.1	1.4	10.3	5.1	2.7	1.6	19.5	6.9	3.0	1.6
ethyl ether		2.9	1.5	1.0	1.0	3.9	2.0	1.2	1.0	5.3	2.2	1.2	1.0
1,3,5-trimethylbenzene		12.4	6.2	3.3	1.9	17.7	8.4	4.3	2.4	34.4	11.8	4.8	2.4
1,2,4-trimethylbenzene		14.1	7.1	3.7	2.1	20.3	9.7	4.9	2.7	39.6	13.6	5.5	2.7
o-xylene		8.5	4.4	2.4	1.5	11.9	5.9	3.1	1.8	22.8	8.1	3.5	1.8
m-xylene		7.4	3.8	2.2	1.4	10.3	5.1	2.8	1.6	19.7	7.0	3.0	1.6

*IB-Inner bag; PC-vented pipe component; FC-filtered can; LB-drum liner bag; DL-drum liner; DF-drum filter vent

Table 9. VOC Concentration Multipliers ($D^*_{H_2, drum} = D^*_{H_2, can} = 3.7e-6 \text{ mol/s/mol fr.}$) as a function of time (days) after venting.

Table 9. VOC Concentration Multiplicities (D ₁ , D ₂ , can = 3.7; FC = 0.0005; m = 0.1) as a function of time (any of three venting														
		Waste Drum Packaging Configuration												
		2IB-PC-DL-DF*				3IB-FC-2LB-DL-DF*				2IB-FC-PC-DL-DF*				
		Days	75	150	300	600	75	150	300	600	75	150	300	600
Volatile Organic Compound														
carbon tetrachloride			3.1	1.8	1.2	1.0	4.5	2.4	1.5	1.1	5.8	2.6	1.4	1.0
cyclohexane			3.4	1.6	1.1	1.0	6.7	2.6	1.4	1.0	4.4	2.0	1.2	1.0
methanol			1.8	1.3	1.0	1.0	2.6	1.7	1.2	1.0	2.6	1.6	1.1	1.0
dichloromethane			1.9	1.3	1.0	1.0	2.7	1.6	1.1	1.0	3.2	1.7	1.1	1.0
toluene			12.0	6.2	3.3	1.9	17.6	8.5	4.4	2.4	23.9	9.8	4.7	2.5
trichloroethane			2.5	1.5	1.0	1.0	3.7	2.0	1.3	1.0	4.6	2.1	1.2	1.0
trichloroethylene			6.0	3.2	1.9	1.2	8.5	4.3	2.4	1.4	11.7	5.0	2.5	1.5
Freon-13			2.6	1.4	1.0	1.0	4.1	2.0	1.2	1.0	4.2	1.9	1.2	1.0
p-xylene			23.6	12.0	6.3	3.4	39.6	17.8	8.6	4.4	49.1	19.8	9.1	4.5
acetone			1.9	1.2	1.0	1.0	2.8	1.6	1.1	1.0	3.2	1.6	1.1	1.0
butanol			2.8	1.6	1.1	1.0	3.9	2.2	1.4	1.0	5.1	2.3	1.4	1.0
chloroform			2.1	1.3	1.0	1.0	3.0	1.7	1.2	1.0	3.7	1.8	1.1	1.0
1,1-dichloroethene			2.0	1.2	1.0	1.0	2.9	1.7	1.1	1.0	3.3	1.6	1.1	1.0
methyl ethyl ketone			2.4	1.4	1.0	1.0	3.5	1.9	1.3	1.0	4.2	2.0	1.2	1.0
methyl isobutyl ketone			4.0	2.1	1.3	1.0	5.9	3.0	1.7	1.2	7.6	3.2	1.7	1.1
1,1,2,2-tetrachloroethane			9.0	4.8	2.6	1.6	12.7	6.3	3.3	1.9	18.1	7.6	3.7	2.0
tetrachloroethene			4.9	2.7	1.6	1.1	6.9	3.6	2.0	1.3	9.9	4.2	2.1	1.3
benzene			2.4	1.5	1.1	1.0	3.5	1.9	1.3	1.0	4.4	2.1	1.2	1.0
bromoform			10.6	5.6	3.0	1.8	15.0	7.3	3.8	2.1	21.1	8.8	4.2	2.3
chlorobenzene			5.5	3.0	1.8	1.2	7.8	4.0	2.2	1.4	11.0	4.7	2.4	1.4
1,1-dichloroethane			2.0	1.3	1.0	1.0	2.9	1.7	1.1	1.0	3.5	1.7	1.1	1.0
1,2-dichloroethane			2.6	1.5	1.1	1.0	3.6	2.0	1.3	1.0	4.7	2.2	1.3	1.0
cis-1,2-dichloroethene			2.0	1.3	1.0	1.0	2.9	1.7	1.1	1.0	3.5	1.7	1.1	1.0
ethylbenzene			5.9	3.1	1.8	1.2	8.5	4.3	2.3	1.4	11.7	4.8	2.4	1.4
ethyl ether			2.4	1.3	1.0	1.0	3.7	1.9	1.2	1.0	3.7	1.7	1.1	1.0
1,3,5-trimethylbenzene			9.7	4.9	2.7	1.6	14.5	7.0	3.6	2.0	20.2	8.0	3.8	2.0
1,2,4-trimethylbenzene			11.0	5.6	3.0	1.8	16.5	7.9	4.0	2.2	23.1	9.2	4.3	2.3
o-xylene			6.7	3.5	2.0	1.3	9.7	4.8	2.6	1.6	13.6	5.6	2.7	1.6
m-xylene			5.9	3.1	1.8	1.2	8.5	4.3	2.4	1.4	11.8	4.9	2.4	1.4
[IB-inner bag; PC-vented pipe component; FC-filtered can; LB-drum liner bag; DL-drum liner; DF-drum filter vent														

*IB-Inner bag; PC-vented pipe component; FC-filtered can; LB-drum liner bag; DL-drum liner; DF-drum filter vent

6. PREDICTION FACTOR METHODOLOGY

The prediction factor (PF) is a variable with a unique value for each VOC and packaging configuration that, when multiplied by the measured VOC concentration in the container headspace, predicts the VOC concentration in the innermost confinement layer. Prediction factors are not required with Scenario 1; however, they are used in conjunction with Scenario 2 and 3 when inner layer of confinement VOC concentration ratios are required. This section describes the methodology used for the determination of PFs. This methodology is based on the analysis presented in Connolly et al. (1998).

At steady conditions, there is no accumulation of VOC within any layer of confinement, the concentrations of VOCs are constant within each layer of confinement and the VOC transport rate across each layer of confinement is equal to a constant rate. The primary mechanisms for gas transport across a confinement layer are permeation across a polymeric layer, diffusion through air across an opening in the layer, and diffusion through a filter vent in the case of a filtered bag. One or all these mechanisms of transport may be operating depending on the characteristics of the confinement layer.

6.1 Model Assumptions

The following assumptions are made in developing the PF methodology:

1. All gases exhibit ideal behavior.
2. Temperature and pressure are constant.
3. An equilibrium exists between the VOC-contaminated waste and the vapor phase in the innermost layer of confinement. Thus, the VOC concentration within the innermost confinement layer is constant.
4. A sufficient period of time has elapsed (i.e., the DAC has been satisfied) such that the VOC transport rates across all layers of confinement are equal and at steady-state. Thus, the VOC concentration within a void volume is constant and there is no accumulation of gas within any confinement layer.
5. The VOC concentration within a void volume is uniform at all times. Thus, there are no concentration variations within a single void volume.
6. Multiple layers of inner bags, liner bags, and SWB liners are treated as a single inner bag, liner bag, or SWB liner with a total thickness equal to the product of the number of such layers and the thickness of the individual layer.
7. The concentration of VOC outside the container is zero. Thus, there is rapid transport by diffusion and convection of VOC outside the container to maintain a zero concentration outside the drum.
8. All VOC properties and confinement layer properties are constant and uniform.

For the various layers of confinement that may be present in a container, the rate of VOC transport across each confinement layer, r , is defined as follows for each unique confinement layer:

6.1.1 Inner Bag (Twist and Tape)

Equation 1

$$r = \frac{\phi c \rho A_{ib} P}{n_{ib} x_{ib}} \Delta y_{ib} = \frac{K_{ib}}{n_{ib}} \Delta y_{ib}$$

where,

- ϕ = 76 T / (273.15 P) (dimensionless)
- c = gas concentration at standard temperature (273.15 °K) and pressure (1 atm) from ideal gas law, P/RT (4.46×10^{-5} mol cm⁻³)
- T = gas temperature (K)
- ρ = VOC permeability [cm³ (STP) cm⁻¹ sec⁻¹ (cm Hg)⁻¹ = 10¹⁰ Ba]
- A_{ib} = surface area of inner bag (cm²)
- P = gas pressure (cm Hg)
- n_{ib} = number of inner bags in packaging configuration
- x_{ib} = thickness of inner bag (cm)
- Δy_{ib} = VOC mole fraction difference across inner bag (dimensionless)
- K_{ib} = inner bag VOC transport characteristic (mol sec⁻¹)
- R = gas constant (6236.6 cm Hg cm³ mol⁻¹ °K⁻¹)

6.1.2 Liner Bag (Twist and Tape)

Equation 2

$$r = \frac{\phi c \rho A_{lb} P}{n_{lb} x_{lb}} \Delta y_{lb} = \frac{K_{lb}}{n_{lb}} \Delta y_{lb}$$

where,

- A_{lb} = surface area of liner bag (cm²)
- n_{lb} = number of liner bags in packaging configuration
- x_{lb} = thickness of liner bag (cm)

Δy_{ib} = VOC mole fraction difference across liner bag (dimensionless)

K_{ib} = liner bag VOC transport characteristic (mol sec^{-1})

6.1.3 Inner Bag (Filtered)

Equation 3

$$r = \left(\frac{\phi c \rho A_{ib} P}{n_{ib} x_{ib}} + \frac{D_{VOC-bf}^*}{n_{ib}} \right) \Delta y_{ib} = \frac{K_{ib}}{n_{ib}} \Delta y_{ib}$$

where,

D_{VOC-bf}^* = VOC-bag filter diffusion characteristic (mol s^{-1}), defined in Equation 4:

Equation 4

$$D_{VOC-bf}^* = \frac{D_{VOC-air}}{D_{H_2-air}} D_{H_2-bf}^*$$

where,

$D_{VOC-air}$ = VOC diffusivity in air ($\text{cm}^2 \text{sec}^{-1}$)

D_{H_2-air} = Hydrogen diffusivity in air ($\text{cm}^2 \text{sec}^{-1}$)

$D_{H_2-bf}^*$ = Hydrogen-bag filter diffusion characteristic (mol s^{-1}).

6.1.4 Liner Bag (Filtered)

Equation 5

$$r = \left(\frac{\phi c \rho A_{ib} P}{n_{ib} x_{ib}} + \frac{D_{VOC-bf}^*}{n_{ib}} \right) \Delta y_{ib} = \frac{K_{ib}}{n_{ib}} \Delta y_{ib}$$

6.1.5 Rigid Drum Liner

Equation 6

$$r = \frac{P D_{VOC-air} A_{rl}}{R T x_{rl}} \Delta y_{rl} = K_{rl} \Delta y_{rl}$$

where,

- A_{rl} = cross-sectional area of the hole in the rigid drum liner lid (cm²)
- x_{rl} = diffusional path length across hole in the rigid drum liner lid (cm)
- Δy_{rl} = VOC mole fraction difference across the rigid liner (dimensionless)
- K_{rl} = rigid liner transport characteristic (mol sec⁻¹)

The VOC-diffusivity in air, $D_{VOC-air}$, can be estimated at low pressures using an equation developed from a combination of kinetic theory and corresponding-states arguments as:

Equation 7

$$D_{VOC-air} = 2.745 \times 10^{-4} \frac{T^{1.823}}{P} [p_{c-VOC} p_{c-air}]^{1/3} [T_{c-VOC} T_{c-air}]^{-1/2} \left[\frac{1}{M_{VOC}} + \frac{1}{M_{air}} \right]^{1/2}$$

where,

- M_{VOC} = molecular weight of VOC (g/mol)
- M_{air} = molecular weight of air = 29 g/mol
- p_{c-VOC} = critical pressure of VOC (atm)
- p_{c-air} = critical pressure of air = 36.4 atm
- T_{c-VOC} = critical temperature of VOC (K)
- T_{c-air} = critical temperature of air = 132 K.

6.1.6 SWB/Ten-Drum Overpack(TDOP)/Bin Liner (Fold and Tape)

Equation 8

$$r = \frac{c \rho A_{cl} P}{n_{cl} x_{cl}} \Delta y_{cl} = \frac{K_{cl}}{n_{cl}} \Delta y_{cl}$$

where,

- A_{cl} = surface area of the container (i.e., SWB, TDOP, or Bin) liner bag (cm^2)
 n_{lb} = number of container liner bags in packaging configuration
 x_{cl} = thickness of the container liner bag (cm)
 Δy_{cl} = VOC mole fraction difference across the container liner bag (dimensionless)
 K_{cl} = container liner bag VOC transport characteristic (mol sec^{-1}).

6.1.7 SWB/TDOP/Bin Liner (Filtered)

Equation 9

$$r = \left(\frac{c \rho A_{cl} P}{n_{cl} x_{cl}} + \frac{D_{VOC-bf}^*}{n_{cl}} \right) \Delta y_{cl} = \frac{K_{cl}}{n_{cl}} \Delta y_{cl}$$

where all variables have been previously defined.

6.1.8 Container Filter

Equation 10

$$r = n_{cf} D_{VOC-cf}^* \Delta y_{cf} = n_{cf} D_{VOC-cf}^* y_{hs}$$

where,

- Δy_{cf} = VOC mole fraction difference across the container filter (dimensionless)
 y_{hs} = VOC mole fraction measured in container headspace (dimensionless)
 n_{cf} = number of container filters in packaging configuration
 D_{VOC-cf}^* = VOC-container filter diffusion characteristic (mol s^{-1}), calculated in Equation 11:

Equation 11

$$D_{VOC-cf}^* = \frac{D_{VOC-air}}{D_{H_2-air}} D_{H_2-cf}^*$$

where $D_{H_2-cf}^*$ is the container filter hydrogen diffusion characteristic (mol s^{-1}). Sequential substitution and rearrangement of terms yields a relationship for the innermost confinement layer VOC concentration as a function of the measured container headspace VOC concentration:

Equation 12

$$y_{icl} = y_{hs} \left[1 + n_{cf} D_{voc-cf} \left(\sum_{i=1}^{nl} \frac{n_i}{K_i} \right) \right]$$

where,

- y_{icl} = innermost confinement layer VOC mole fraction
- n_i = number of type “i” confinement layers in packaging configuration
- K_i = transport characteristic of type “i” confinement layer (mol s^{-1})
- nl = number of different confinement layer types.

Multiplying both sides of Equation 12 by a conversion factor (10^6 ppm/mole fraction) yields the following final equation for the prediction factor.

Equation 13

$$Y_{icl} = Y_{hs} \left[1 + n_{cf} D_{voc-cf} \left(\sum_{i=1}^{nl} \frac{n_i}{K_i} \right) \right]$$

where,

- Y_{icl} = innermost confinement layer VOC concentration (ppm)
- Y_{hs} = measured VOC concentration in container headspace (ppm)

Thus, the prediction factor, PF, is defined as:

Equation 14

$$PF = \left[1 + n_{cf} D_{voc-cf} \left(\sum_{i=1}^{nl} \frac{n_i}{K_i} \right) \right]$$

7. DISCUSSION

The calculation of DACs for three common drum venting and sampling scenarios provides more realistic waiting periods for sampling than current conservative DACs applied uniformly to all packaging configurations. For example, DAC₂ values indicate that unvented drums that have been in storage in excess of DAC₁ values can be realistically sampled anywhere from 4 to 36 days depending on the liner lid opening and drum filter vent installed at the time of venting. This could provide relief of over 200 days in some cases in reducing the waiting time required before sampling the drum headspace.

A comparison of DAC₂ values calculated for drums with 0.375-in diameter opening in liner lid and a drum vent with a hydrogen diffusion characteristic of 3.7×10^{-6} mol/s/mol fr (20 and 25 days) to similar values reported by Connolly et al. (1998) (18 and 22 days) show close agreement. The higher values calculated in this report result from more restrictive packaging (S5000 waste or Waste Types II and III), an assumption of a filter vent with 10% lower diffusion characteristic, and a model assumption of a 10% lower drum liner headspace concentration at the time of venting. The DAC for newly packaged and vented waste drums with a packaging configuration for Waste Types II and III was previously calculated to be 142 days (Connolly et al., 1998). This value is not in Table 4 because its packaging configuration was assumed to have three inner bags, two liner bags, and filter vent with an average hydrogen diffusion characteristic of 4.2×10^{-6} mol/s/mol fr. Some DAC₃ values are greater than earlier DAC values of 142 and 225 days (Connolly et al., 1998). The higher DAC₃ values result from assuming the limiting values for the filter vent diffusion characteristic and the liner lid opening as well as considering a greater possible number of polymer bags in the drum.

Separate DAC₃ values were calculated for S3000/S4000 (Waste Types I and IV) and S5000 (Waste Types II and III) waste packaging configurations. Since waste packaging configurations were assumed for each waste type, these DACs should be considered packaging-specific DACs and not waste-specific. In some cases, S3000/S4000 (Waste Types I and IV) waste is packaged inside inner bags before being placed inside a liner bag. An argument can be made that the S5000 (Waste Types II and III) DAC₃ value for the appropriate packaging configuration could be used to define when a headspace gas sample can be taken. In this case, a comparison of DAC₃ values by waste type for a given packaging configuration shows that S3000/S4000 (Waste Types I and IV) DAC₃ values are higher and, thus, more conservative.

The DAC values calculated for the SWBs and the pipe component are intended to conservatively bound the wide range of likely packaging configurations. As more information becomes available on the configurations used, it is foreseeable that additional packaging-specific DACs could be generated in the same manner as was for waste drums in this report. The VOC concentration multiplier was defined to relate the measured VOC concentration in the headspace of a waste drum containing a vented pipe component (i.e. pipe overpack) or metal can to the VOC headspace concentration when it had achieved 90% of its steady-state value. This approach was developed to avoid excessively lengthy waiting times due to slow diffusion of the VOCs.

8. REFERENCES

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- Liekhus K.J. and A.G. Chambers, 2000, "Software Validation and Verification of Revised Computer Code (VDRUM) Used to Calculate Drum Age Criteria", *INEEL/EXT-2000-01208*, Bechtel BWXT Idaho, LLC, Idaho Falls, Idaho.

Appendix A

Model Input Parameters to Calculate DAC

The physical properties of indicator VOCs used in calculating DACs are listed in Table A-1. Toluene, 1,1-dichloroethene (DCE), or methyl isobutyl ketone (MIBK) have been identified as the VOCs that yield the highest packaging-specific DACs (Connolly et al., 1998). Toluene defined the DAC in drums containing drum liners during transient conditions where the VOC solubility in the drum liner is important. In cases where the VOC concentration in the liner had approached its equilibrium concentration or in drums that did not contain a drum liner, the time required for the other two VOCs to reach near equilibrium concentration define the DAC. The diffusivity of DCE and MIBK in air is estimated using the VOC critical properties.

Table A-1. VOC physical properties used to calculate DAC₂ values.

VOC	MW	P _{voc}	D _{voc}	T _c	P _c	H	k
Toluene	92.1	669e-10	0.0849	591.8	40.5	0.002857	7.e-6
DCE	96.9	110e-10	0	513.0	47.5	0.09091	8.e-6
MIBK	100.2	130e-10	0	571.0	32.3	0.01724	8.e-6

MW – molecular weight

P_{voc} – VOC permeability across polymer bags, cm³(STP) cm cm⁻² s⁻¹ (cm Hg)⁻¹

D_{voc} – VOC diffusivity in air, cm² s⁻¹

T_c – critical temperature, K

P_c – critical pressure, atm

H – VOC Henrys constant for drum liner, cm³ polymer atm cm⁻³ (STP)

k – VOC mass transfer coefficient at drum liner, s⁻¹

DAC₁ Model Input Parameters

The physical dimensions of each layer of confinement in waste drums containing S3000/S4000 and S5000 drums specified in the model input file are listed in Table A-2. Since accumulating VOC will interact with the drum liner, toluene is the chosen VOC to achieve the highest DAC. The initial VOC concentration profile has a constant VOC concentration within the innermost layer of confinement and zero in all other layers indicative of a newly packaged drum. The drum is unvented so the diffusion characteristic of the filter vent is set to zero. All drums are assumed to be at 25°C and ambient pressure of 76 cm Hg (1 atm).

Table A-2. Physical parameters used to calculate DAC₁ values

Layer of Confinement	A _p (cm ²)	V (cm ³)	x _p (cm)
Inner bags (S5000 only)	14,000	---	0.050
Liner Bags (S3000/S4000)	3,000	20,000	0.056
Liner Bags (S5000)	14,000		
Drum Liner	15,500	40,000	0.229
Drum Headspace	---	28,000	---

A_p – permeable/soluble surface area

V – void volume inside later of confinement

x_p – thickness of permeable/soluble polymer

DAC₂ Model Input Parameters

The methodology for calculating the drum age criterion in a drum being vented after remaining unvented for at least DAC_1 days is the same as for newly vented drums with liners at complete equilibrium. The only difference is in calculating DAC_2 values, the VOC in the drum liner headspace is assumed to be at 90% of the VOC concentration within the innermost layer of confinement instead of 100%. The VOC solubility in the liner is not considered since it is assumed that the liner is nearly saturated. This is reflected in the model input file by setting the mass-transfer coefficients (k) for each VOC to zero. All other VOC physical properties used to calculate DAC_2 values are listed in Table A-1. The physical parameters used to calculate DAC_2 values are listed in Table A-2. All drums are assumed to be at 25°C and ambient pressure of 76 cm Hg (1 atm). The other variables considered in calculating the DAC_2 values were the diameter of the circular opening in the drum liner lid and the hydrogen diffusion characteristic of the drum filter vent. The cross-sectional areas and diffusion lengths associated with each liner lid opening is shown in Table A-3. **The drum filter vent H_2 diffusion characteristic (mol/s/mol fr.) was evaluated at three values: 1.9×10^{-6} ; 3.7×10^{-6} ; 3.7×10^{-5} .**

Table A-3. Physical parameters associated with liner lid opening

Liner Lid Opening Diameter (in)	A_d (cm ²)	x_d (cm)
0.30	0.456	1.2
0.375	0.71	1.2
0.75	2.85	1.4
1.0	5.08	1.4

A_d – diffusion cross-sectional area

x_d - diffusional length

The initial concentration is defined by a constant VOC concentration within the innermost layer of confinement, with the same VOC concentration in all other layers of confinement except the drum liner headspace which is assumed to have achieved 90% of the constant source concentration. The drum headspace is assumed to be free of any VOCs until the liner is punctured. This is a conservative assumption.

DAC_3 Model Input Parameters

Three packaging configurations in waste drums were considered for each waste type (S3000/S4000 and S5000). The packaging configurations are distinguished by the number of bags and were selected to cover the range of packaging configurations. The physical parameters associated with each packaging configuration is summarized in Table A-4. The liner lid opening of five different sizes as well as the case of no liner present in the waste drum were considered. The physical properties associated with the liner in each case is listed in Table A-5. **The drum filter vent H_2 diffusion characteristic (mol/s/mol fr.) was evaluated at three values: 1.9×10^{-6} ; 3.7×10^{-6} ; 3.7×10^{-5} .** The VOCs and their physical properties used in calculating DAC_3 values are listed in Table A-1.

Table A-4. Physical parameters associated with waste type and packaging configuration.

Waste Type	Packaging Configuration	Inner bag		Liner Bag	
		A_p (cm ²)	x_p (cm)	A_p (cm ²)	x_p (cm)
S3000/S4000	1: No liner bags	---	---	3,000	0.0005*
S3000/S4000	2: One liner bag	---	---	3,000	0.028
S3000/S4000	3: Two liner bags	---	---	3,000	0.056
S5000	1: No inner or liner bags	---	---	14,000	0.0003*
S5000	2: Three inner, one liner bags	14,000	0.038	14,000	0.028
S5000	3: Four inner, two liner bags	14,000	0.050	14,000	0.056

*Model requires one bag so bag thickness is assumed to be negligible.

Table A-5. Physical parameters associated with liner and liner lid for DAC₃.

Liner lid opening diameter (in)/liner status	$A_{d,opening}$ (cm ²)	$x_{d,opening}$ (cm)	$A_{p,liner}$ (cm ²)	$x_{p,liner}$ (cm)
0.3	0.456	1.2	15,500	0.229
0.375	0.71	1.2	15,500	0.229
0.75	2.85	1.4	15,500	0.229
1.0	5.08	1.4	15,500	0.229
No lid	150^	1.4	12,800	0.229
No liner	150^	1.4	12,800	0.00005*

^Larger values cause instability in program and do not yield a lower DAC.

*Represent liner as having negligible thickness

In addition, two packaging configurations for standard waste boxes (SWBs) and a bounding case of bagged waste inside a vented metal can inside a vented pipe component were evaluated. The SWB packaging configuration 1 assumes waste wrapped inside 5 inner bags is placed in a single liner bag in a SWB. The SWB packaging configuration 2 assumes waste is directly placed inside a single liner bag in a SWB. For the two cases of SWBs, the DAC was defined by the physical properties of DCE (see Table A-1). The SWB has one or more filter vents with a total hydrogen diffusion characteristic of 7.4×10^{-6} mol/s/mol fr. The initial concentration profiles in all configurations is a constant VOC concentration inside the innermost layer of confinement and zero in all other layers indicative of a newly packaged container. The physical dimensions of each layer of confinement for the SWBs and pipe component used as model input are listed in Table A-6. The code VDRUM.FOR was used to calculate the DACs for the SWBs. The code VDRUM2.FOR was used to calculate the DAC for the limiting packaging configuration for a pipe component.

Table A-6. Model input parameters for calculating SWB and pipe component DACs.

Packaging Configuration	Layer of confinement	A_p (cm ²)	x_p (cm)	V (cm ³)	A_d (cm ²)	x_d (cm)	D^* , mol/s/mol
SWB	Inner bag (case 2 only)	14,000	0.063	---	---	---	---
	Liner Bag	14,000	0.036	190,000	---	---	---
	Liner (none)*	14,000	0.0001*	100,000	150*	1.4	---
	SWB Headspace	---	---	100,000	---	---	7.4e-6
Pipe component	Inner bags	500	---	---	0.025	---	---
	Metal can	---	---	1,000	---	---	1.9e-6
	Pipe component	---	---	46,000	---	---	1.9e-6

* - Liner wall thickness is assumed negligible to mimic configuration with no liner.

Appendix B

Model Input Parameters to Calculate VOC Concentration Multipliers

The physical properties of VOCs used in calculating VOC concentration multipliers are listed in Table B-1. The VOC diffusivity, in some cases, is estimated using the VOC critical properties.

Table B-1. VOC physical properties used to calculate VOC concentration multipliers.

VOC	MW	P _{voc}	D _{voc}	T _c	P _c	H	k
Carbon tetrachloride	153.82	193e-10	0.0828	556.4	45.0	0.0217	6.e-5
Cyclohexane	84.1	12.4e-10	0	553.2	40.2	0.8333	3.e-5
Methanol	32.0	135e-10	0.152	513.2	78.5	0.0272	2.4e-7
Dichloromethane	84.9	263e-10	0.104	510.0	62.2	0.0431	2.e-6
Toluene	92.1	669e-10	0.0849	591.8	40.5	0.002857	7.e-6
Trichloroethane	133.4	143e-10	0.0794	545.0	42.4	0.0402	1.e-5
Trichloroethylene	131.4	583e-10	0.0875	572.0	49.8	0.00640	6.e-5
Freon-13	187.4	38.6e-10	0	487.3	33.7	0.1973	1.e-5
p-xylene	106.2	811e-10	0.0670	616.7	34.8	0.00147	4.e-6
Acetone	58.1	150e-10	0	508.1	46.4	0.06667	8.e-6
Butanol	74.1	300e-10	0	563.1	43.6	0.02273	8.e-6
Chloroform	119.4	260e-10	0	536.4	53.0	0.04545	8.e-6
1,1-dichloroethene	96.9	110e-10	0	513.0	47.5	0.09091	8.e-6
Methyl ethyl ketone	72.1	165e-10	0	536.8	41.5	0.03704	8.e-6
Methyl isobutyl ketone	100.2	130e-10	0	571.0	32.3	0.01724	8.e-6
1,1,2,2-tetrachloroethane	167.9	2300e-10	0	661.2	57.6	0.003846	8.e-6
Tetrachloroethene	165.8	610e-10	0	620.2	47.0	0.009091	8.e-6
Benzene	78.1	280e-10	0	562.2	48.3	0.02941	8.e-6
Bromoform	252.7	4800e-10	0	658.7	69.2	0.00303	8.e-6
Chlorobenzene	112.6	600e-10	0	632.4	44.6	0.007692	8.e-6
1,1-dichloroethane	99.0	200e-10	0	523.0	50.0	0.05556	8.e-6
1,2-dichloroethane	99.0	445e-10	0	566.0	53.0	0.02381	8.e-6
Cis-1,2-dichloroethene	96.9	295e-10	0	537.0	55.3	0.04545	8.e-6
Ethylbenzene	106.2	260e-10	0	617.2	35.5	0.00833	8.e-6
Ethyl ether	74.1	40e-10	0	466.7	35.9	0.14706	8.e-6
1,3,5-trimethylbenzene	120.2	260e-10	0	637.3	30.9	0.004762	8.e-6
1,2,4-trimethylbenzene	120.2	320e-10	0	649.2	31.9	0.0040	8.e-6
o-xylene	106.2	360e-10	0	630.3	36.8	0.006667	8.e-6
m-xylene	106.2	260e-10	0	617.1	34.9	0.0083333	8.e-6

MW – molecular weight

P_{voc} – VOC permeability across polymer bags, cm³(STP) cm cm⁻² s⁻¹ (cm Hg)⁻¹

D_{voc} – VOC diffusivity in air, cm² s⁻¹

T_c – critical temperature, K

P_c – critical pressure, atm

H – VOC Henrys constant for drum liner, cm³ polymer atm cm⁻³ (STP)

k – VOC mass transfer coefficient at drum liner, s⁻¹

Three packaging configurations have been identified as bounding cases for waste stored in a pipe component. The three configurations and the other configurations bounded by them are listed below:

Packaging Configuration 1: 2 Inner Bags (IB)-Pipe component (PC)-Drum Liner (DL)-Vented Drum (DF)

Packaging Configuration Subset: 2 Filtered Inner Bags (FIB)-PC-DL-DF

Packaging Configuration 2: 2IB-Vented Can (FC)-PC-DL-DF

Packaging Configuration Subset: FC-2FIB-FC-Filtered Liner Bag (FLB)-DL-DF

FC-2FIB-FC-2FLB-DL-DF

2FIB-FC-PC-DL-DF

Packaging Configuration 3: 3IB-FC-2 Liner Bags (LB)-DL-DF

Packaging Configuration Subset: 2FIB-FC-FIB-FLB-DL-DF

2FIB-FC-FLB-DL-DF

FIB-FC-FLB-DL-DF

3FIB-FC-FIB-FLB-DL-DF

2IB-FC-IB-LB-DL-DF

3IB-FC-IB-LB-DL-DF

2IB-FC-LB-DL-DF

2FIB-FC-2FLB-DL-DF

Filtered bags offer considerably less resistance to VOC transport across polymer bags than unfiltered bags. That is why in Packaging Configuration 2 configurations containing up to four layers of vented bags are in the subset below the bounding case contain fewer unfiltered bags. Drum liners holding pipe components are assumed to have no lids. The physical dimensions assumed for these packaging configurations are tabulated in Table B-2.

The initial concentration profiles in all configurations is a constant VOC concentration inside the innermost layer of confinement and zero in all other layers indicative of a newly packaged container.

The filter vent on the metal can and pipe component as well as the filter vent on the drum lid are assumed to have a hydrogen diffusion characteristic of one of two values: 1.9×10^{-6} mol/s/mol fr and 3.7×10^{-6} mol/s/mol fr.

The VOC concentration multipliers are calculated in each packaging configuration after a specific period of time. Four time periods were selected: 75, 150, 300, and 600 days.

Table B-2. Physical dimensions used to calculate VOC concentration multipliers in Tables 6 through 9.

Packaging Configuration	Layer of confinement	A_p , cm ²	x_p , cm	V , cm ³	A_d , cm ²	x_d , cm
2IB-PC-DL-DF (Case 1)	Inner Bags	1,000	0.025	---	---	---
	Pipe component	---	---	45,000	---	---
	Drum Liner	12,800	0.279	105,000	150	1.4
	Drum Headspace	---	---	18,000	---	---
2IB-FC-PC-DL-DF (Case 2)	Inner Bags	500	0.025	---	---	---
	Vented Can	---	---	1,000	---	---
	Pipe component	---	---	46,000	---	---
	Drum Liner	12,800	0.279	105,000	150	1.4
3IB-FC-2LB-DL-DF (Case 3)	Drum Headspace	---	---	18,000	---	---
	Inner Bags	500	0.038	---	---	---
	Vented Can	---	---	1,000	---	---
	Liner Bags	4,000	0.075	37,000	---	---
	Drum Liner	15,500	0.279	134,000	2.85	1.2
	Drum Headspace	---	---	18,000	---	---
A_p – permeable/soluble surface area						
x_p – thickness of permeable/soluble polymer						
V – void volume inside later of confinement						
A_d – diffusion cross-sectional area						
x_d – diffusional length						

The methodology for calculating the drum age criterion in a drum being vented after remaining unvented for at least DAC_1 days is the same as for newly vented drums with liners at complete equilibrium. The only difference is in calculating DAC_2 values, the VOC in the drum liner headspace is assumed to be at 90% of the VOC concentration within the innermost layer of confinement instead of 100%. The VOC solubility in the liner is not considered since it is assumed that the liner is nearly saturated. This is reflected in the model input file by setting the mass-transfer coefficients (k) for each VOC to zero. All other VOC physical properties used to calculate DAC_2 values are listed in Table A-1. The physical parameters used to calculate DAC_2 values are listed in Table A-2. All drums are assumed to be at 25°C and ambient pressure of 76 cm Hg (1 atm). The other variables considered in calculating the DAC_2 values were the diameter of the circular opening in the drum liner lid and the hydrogen diffusion characteristic of the drum filter vent. The cross-sectional areas and diffusion lengths associated with each liner lid opening is shown in Table A-3. **The drum filter vent H_2 diffusion characteristic (mol/s/mol fr.) was evaluated at three values: 1.9×10^{-6} ; 3.7×10^{-6} ; 3.7×10^{-5} .**

Table A-3. Physical parameters associated with liner lid opening

Liner Lid Opening Diameter (in)	A_d (cm ²)	x_d (cm)
0.30	0.456	1.2
0.375	0.71	1.2
0.75	2.85	1.4
1.0	5.08	1.4

A_d – diffusion cross-sectional area

x_d - diffusional length

The initial concentration is defined by a constant VOC concentration within the innermost layer of confinement, with the same VOC concentration in all other layers of confinement except the drum liner headspace which is assumed to have achieved 90% of the constant source concentration. The drum headspace is assumed to be free of any VOCs until the liner is punctured. This is a conservative assumption.

DAC_3 Model Input Parameters

Three packaging configurations in waste drums were considered for each waste type (S3000/S4000 and S5000). The packaging configurations are distinguished by the number of bags and were selected to cover the range of packaging configurations. The physical parameters associated with each packaging configuration is summarized in Table A-4. The liner lid opening of five different sizes as well as the case of no liner present in the waste drum were considered. The physical properties associated with the liner in each case is listed in Table A-5. **The drum filter vent H_2 diffusion characteristic (mol/s/mol fr.) was evaluated at three values: 1.9×10^{-6} ; 3.7×10^{-6} ; 3.7×10^{-5} .** The VOCs and their physical properties used in calculating DAC_3 values are listed in Table A-1.

Table A-4. Physical parameters associated with waste type and packaging configuration.

Waste Type	Packaging Configuration	Inner bag		Liner Bag	
		A_p (cm ²)	x_p (cm)	A_p (cm ²)	x_p (cm)
S3000/S4000	1: No liner bags	---	---	3,000	0.0005*
S3000/S4000	2: One liner bag	---	---	3,000	0.028
S3000/S4000	3: Two liner bags	---	---	3,000	0.056
S5000	1: No inner or liner bags	---	---	14,000	0.0003*
S5000	2: Three inner, one liner bags	14,000	0.038	14,000	0.028
S5000	3: Four inner, two liner bags	14,000	0.050	14,000	0.056

*Model requires one bag so bag thickness is assumed to be negligible.

Table A-5. Physical parameters associated with liner and liner lid for DAC₃.

Liner lid opening diameter (in)/liner status	$A_{d,opening}$ (cm ²)	$x_{d,opening}$ (cm)	$A_{p,liner}$ (cm ²)	$x_{p,liner}$ (cm)
0.3	0.456	1.2	15,500	0.229
0.375	0.71	1.2	15,500	0.229
0.75	2.85	1.4	15,500	0.229
1.0	5.08	1.4	15,500	0.229
No lid	150^	1.4	12,800	0.229
No liner	150^	1.4	12,800	0.00005*

^Larger values cause instability in program and do not yield a lower DAC.

*Represent liner as having negligible thickness

In addition, two packaging configurations for standard waste boxes (SWBs) and a bounding case of bagged waste inside a vented metal can inside a vented pipe component were evaluated. The SWB packaging configuration 1 assumes waste wrapped inside 5 inner bags is placed in a single liner bag in a SWB. The SWB packaging configuration 2 assumes waste is directly placed inside a single liner bag in a SWB. For the two cases of SWBs, the DAC was defined by the physical properties of DCE (see Table A-1). The SWB has one or more filter vents with a total hydrogen diffusion characteristic of 7.4×10^{-6} mol/s/mol fr. The initial concentration profiles in all configurations is a constant VOC concentration inside the innermost layer of confinement and zero in all other layers indicative of a newly packaged container. The physical dimensions of each layer of confinement for the SWBs and pipe component used as model input are listed in Table A-6. The code VDRUM.FOR was used to calculate the DACs for the SWBs. The code VDRUM2.FOR was used to calculate the DAC for the limiting packaging configuration for a pipe component.

Table A-6. Model input parameters for calculating SWB and pipe component DACs.

Packaging Configuration	Layer of confinement	A_p (cm ²)	x_p (cm)	V (cm ³)	A_d (cm ²)	x_d (cm)	D^* , mol/s/mol
SWB	Inner bag (case 2 only)	14,000	0.063	---	---	---	---
	Liner Bag	14,000	0.036	190,000	---	---	---
	Liner (none)*	14,000	0.0001*	100,000	150*	1.4	---
	SWB Headspace	---	---	100,000	---	---	7.4e-6
Pipe component	Inner bags	500	---	---	0.025	---	---
	Metal can	---	---	1,000	---	---	1.9e-6
	Pipe component	---	---	46,000	---	---	1.9e-6

* - Liner wall thickness is assumed negligible to mimic configuration with no liner.

Appendix B

Model Input Parameters to Calculate VOC Concentration Multipliers

The physical properties of VOCs used in calculating VOC concentration multipliers are listed in Table B-1. The VOC diffusivity, in some cases, is estimated using the VOC critical properties.

Table B-1. VOC physical properties used to calculate VOC concentration multipliers.

VOC	MW	P _{voc}	D _{voc}	T _c	P _c	H	k
Carbon tetrachloride	153.82	193e-10	0.0828	556.4	45.0	0.0217	6.e-5
Cyclohexane	84.1	12.4e-10	0	553.2	40.2	0.8333	3.e-5
Methanol	32.0	135e-10	0.152	513.2	78.5	0.0272	2.4e-7
Dichloromethane	84.9	263e-10	0.104	510.0	62.2	0.0431	2.e-6
Toluene	92.1	669e-10	0.0849	591.8	40.5	0.002857	7.e-6
Trichloroethane	133.4	143e-10	0.0794	545.0	42.4	0.0402	1.e-5
Trichloroethylene	131.4	583e-10	0.0875	572.0	49.8	0.00640	6.e-5
Freon-13	187.4	38.6e-10	0	487.3	33.7	0.1973	1.e-5
p-xylene	106.2	811e-10	0.0670	616.7	34.8	0.00147	4.e-6
Acetone	58.1	150e-10	0	508.1	46.4	0.06667	8.e-6
Butanol	74.1	300e-10	0	563.1	43.6	0.02273	8.e-6
Chloroform	119.4	260e-10	0	536.4	53.0	0.04545	8.e-6
1,1-dichloroethene	96.9	110e-10	0	513.0	47.5	0.09091	8.e-6
Methyl ethyl ketone	72.1	165e-10	0	536.8	41.5	0.03704	8.e-6
Methyl isobutyl ketone	100.2	130e-10	0	571.0	32.3	0.01724	8.e-6
1,1,2,2-tetrachloroethane	167.9	2300e-10	0	661.2	57.6	0.003846	8.e-6
Tetrachloroethene	165.8	610e-10	0	620.2	47.0	0.009091	8.e-6
Benzene	78.1	280e-10	0	562.2	48.3	0.02941	8.e-6
Bromoform	252.7	4800e-10	0	658.7	69.2	0.00303	8.e-6
Chlorobenzene	112.6	600e-10	0	632.4	44.6	0.007692	8.e-6
1,1-dichloroethane	99.0	200e-10	0	523.0	50.0	0.05556	8.e-6
1,2-dichloroethane	99.0	445e-10	0	566.0	53.0	0.02381	8.e-6
Cis-1,2-dichloroethene	96.9	295e-10	0	537.0	55.3	0.04545	8.e-6
Ethylbenzene	106.2	260e-10	0	617.2	35.5	0.00833	8.e-6
Ethyl ether	74.1	40e-10	0	466.7	35.9	0.14706	8.e-6
1,3,5-trimethylbenzene	120.2	260e-10	0	637.3	30.9	0.004762	8.e-6
1,2,4-trimethylbenzene	120.2	320e-10	0	649.2	31.9	0.0040	8.e-6
o-xylene	106.2	360e-10	0	630.3	36.8	0.006667	8.e-6
m-xylene	106.2	260e-10	0	617.1	34.9	0.0083333	8.e-6

MW – molecular weight

P_{voc} – VOC permeability across polymer bags, cm³(STP) cm cm⁻² s⁻¹ (cm Hg)⁻¹

D_{voc} – VOC diffusivity in air, cm² s⁻¹

T_c – critical temperature, K

P_c – critical pressure, atm

H – VOC Henrys constant for drum liner, cm³ polymer atm cm⁻³ (STP)

k – VOC mass transfer coefficient at drum liner, s⁻¹

Three packaging configurations have been identified as bounding cases for waste stored in a pipe component. The three configurations and the other configurations bounded by them are listed below:

Packaging Configuration 1: 2 Inner Bags (IB)-Pipe component (PC)-Drum Liner (DL)-Vented Drum (DF)

Packaging Configuration Subset: 2 Filtered Inner Bags (FIB)-PC-DL-DF

Packaging Configuration 2: 2IB-Vented Can (FC)-PC-DL-DF

Packaging Configuration Subset: FC-2FIB-FC-Filtered Liner Bag (FLB)-DL-DF

FC-2FIB-FC-2FLB-DL-DF

2FIB-FC-PC-DL-DF

Packaging Configuration 3: 3IB-FC-2 Liner Bags (LB)-DL-DF

Packaging Configuration Subset: 2FIB-FC-FIB-FLB-DL-DF

2FIB-FC-FLB-DL-DF

FIB-FC-FLB-DL-DF

3FIB-FC-FIB-FLB-DL-DF

2IB-FC-IB-LB-DL-DF

3IB-FC-IB-LB-DL-DF

2IB-FC-LB-DL-DF

2FIB-FC-2FLB-DL-DF

Filtered bags offer considerably less resistance to VOC transport across polymer bags than unfiltered bags. That is why in Packaging Configuration 2 configurations containing up to four layers of vented bags are in the subset below the bounding case contain fewer unfiltered bags. Drum liners holding pipe components are assumed to have no lids. The physical dimensions assumed for these packaging configurations are tabulated in Table B-2.

The initial concentration profiles in all configurations is a constant VOC concentration inside the innermost layer of confinement and zero in all other layers indicative of a newly packaged container.

The filter vent on the metal can and pipe component as well as the filter vent on the drum lid are assumed to have a hydrogen diffusion characteristic of one of two values: 1.9×10^{-6} mol/s/mol fr and 3.7×10^{-6} mol/s/mol fr.

The VOC concentration multipliers are calculated in each packaging configuration after a specific period of time. Four time periods were selected: 75, 150, 300, and 600 days.

Table B-2. Physical dimensions used to calculate VOC concentration multipliers in Tables 6 through 9.

Packaging Configuration	Layer of confinement	A_p , cm ²	x_p , cm	V , cm ³	A_d , cm ²	x_d , cm
2IB-PC-DL-DF (Case 1)	Inner Bags	1,000	0.025	---	---	---
	Pipe component	---	---	45,000	---	---
	Drum Liner	12,800	0.279	105,000	150	1.4
	Drum Headspace	---	---	18,000	---	---
2IB-FC-PC-DL-DF (Case 2)	Inner Bags	500	0.025	---	---	---
	Vented Can	---	---	1,000	---	---
	Pipe component	---	---	46,000	---	---
	Drum Liner	12,800	0.279	105,000	150	1.4
3IB-FC-2LB-DL-DF (Case 3)	Drum Headspace	---	---	18,000	---	---
	Inner Bags	500	0.038	---	---	---
	Vented Can	---	---	1,000	---	---
	Liner Bags	4,000	0.075	37,000	---	---
	Drum Liner	15,500	0.279	134,000	2.85	1.2
	Drum Headspace	---	---	18,000	---	---
A_p – permeable/soluble surface area						
x_p – thickness of permeable/soluble polymer						
V – void volume inside later of confinement						
A_d – diffusion cross-sectional area						
x_d – diffusional length						

**Software Validation and Verification of Revised Computer Code (VDRUM) Used to
Calculate Drum Age Criteria INEEL/EXT-2000-01208**

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Software Validation and Verification of Revision of Computer Code (VDRUM) used to calculate Drum Age Criteria

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Software Validation and Verification of Revision of Computer Code (VDRUM) Used to Calculate Drum Age Criteria

1. BACKGROUND

In 1995, software written in the FORTRAN language was developed, validated, and used to estimate the time required for the volatile organic compound (VOC) concentration in a waste drum to reach near steady-state or equilibrium conditions. The name of the program was VDRUM.FOR, Revision 1 (referred to from now on as VDRUM1). The calculated time is referred to as the drum age criterion (DAC). The verification and the validation of the software to predict time-dependent concentrations in vented waste drums was conducted using experimental data and results from previously validated software.¹ The software was used to determine the DAC for two broad categories of waste packaging configurations under three different scenarios. The two waste packaging configurations considered were:

1. Waste drum, rigid drum liner, and polymer liner bags in which waste is placed;
2. Waste drum, rigid liner, polymer liner bags, and small polymer bags in which waste is placed.

The packaging scenarios considered included:

1. Previously packaged waste drums, newly vented;
2. Newly packaged, vented waste drums;
3. Newly packaged, unvented waste drums.

The waste packaging configurations and packaging scenarios selected were intended to serve as bounding, or limiting, cases representing the most conservative estimate for a DAC applicable to all similarly packaged waste drums.² However, given the wide variety of waste packaging variables (total layers of polymer bags, as well as the presence or absence of bag filters, drum liner, and vented metal cans), there is a need for calculating packaging-specific DACs that would reflect more accurate, and possibly less restrictive, minimum vent times.

2. CHANGE REQUEST DESCRIPTION AND JUSTIFICATION

The software is modified to allow calculations of DAC values for a wider range of waste drum packaging configurations. The modifications will enable the user to calculate DACs for waste drums with three to six layers of confinement, allow for the presence of vented layers of confinement, and enable the user to calculate the time to achieve a user-specified percentage of the steady-state drum headspace concentration or calculate the drum headspace concentration after a user-specified period of time.

The code no longer considers the possibility of gas generation in the waste drum. This feature was useful in modeling hydrogen generation in the drum. In addition, the capability of the code to model newly packaged, unvented drum and drum liner was removed. The code VDRUM1 was used to determine the DAC for three different packaging scenarios. The results demonstrated that the most conservative packaging scenario is newly packaged, vented waste drums. The DAC values for this scenario were

applied to all other packaging scenarios. It is assumed new DAC values calculated for other packaging configurations will be for newly packaged, vented waste drums.

3. SOFTWARE QUALITY ASSURANCE PLAN

The software quality assurance described in this document is designed to meet the intent of the specifications described in NQA-2 Part 2.7. Model equations, the original computer code, and the revision to the computer code were developed by Dr. Kevin Liekhus at the Idaho National Engineering and Environmental Laboratory (INEEL). Dr. Liekhus has a Ph.D in chemical engineering and extensive experience in modeling transport phenomena.³ This document and model verifications were reviewed by Andrea Chambers at the INEEL. Ms. Chambers has an undergraduate degree in chemical engineering.

4. SOFTWARE REQUIREMENTS

The functionality and design requirements of the VDRUM1 were defined in the validation documentation.¹ These requirements that are applicable to a revised VDRUM1 include (a) prompting the user to specify the input data file defining user-specified initial values and model parameters; (b) reading the input data file; (c) defining additional variables in terms of user-specified input; (d) solving a series of ordinary differential equations to define the change in gas concentration within each layer of confinement as a function of time; (e) calculating equilibrium or steady-state concentration; (f) calculating the time to reach the DAC (when the calculated concentration is within 10% of the steady-state or equilibrium concentration); and, (g) writing the calculated time to achieve the DAC, the DAC concentration, and equilibrium or steady-state concentration to an output data file.

In the revised version of VDRUM1, additional requirements were identified:

1. Program has capability to model VOC transport within a vented waste drum with or without a rigid drum liner and up to four additional layers of confinement;
2. Program has capability to model VOC transport within a vented waste drum that contains layers of confinement that may or may not be vented;
3. Program calculates steady-state concentration using computationally efficient algebraic equations instead of by solving a series of ordinary differential equations.
4. Program has the capability to calculate the time necessary to achieve a specified fraction of the steady-state concentration in the drum headspace or the fraction of the steady-state concentration achieved in the drum headspace for a specified period of time.

4.1 Design Constraints

The computer program for calculating the DAC or the relative VOC concentration in the drum headspace for a given period of time must be able to access the IMSL mathematical library. The IMSL mathematical library contains subroutines specifically designed to solve a series of ordinary differential equations. The computer program and the IMSL subroutines are written in FORTRAN computer language.

4.2 Software Design and Implementation

Major components of the computer code include:

1. All user-specified input data
2. Model parameter definition of gas-specific properties via internal subroutine
3. Model variable initialization
4. An algorithm to calculate steady-state gas concentration within waste drum
5. An algorithm to solve a series of ordinary differential equations of the gas transport model that define the gas concentration within each layer of confinement in the waste drum as a function of time
6. Model results written to an output data file

4.2.1 DAC Calculations

The drum age criterion is defined as the time in which the VOC concentration in the drum headspace achieves 90% of its steady-state concentration. In VDRUM1, the steady-state concentration was determined through the solution of a series of ordinary differential equations to be the concentration at the time it could be considered constant. The steady-state concentration was defined as the concentration when the relative change in concentration was less than 10^{-6} in order to avoid performing calculations out to a time approximating infinity. This approach was an arbitrary way of saying that this condition is close enough to steady-state conditions.

The equations that form the basis for describing transient VOC transport across polymer bags, filter vents, and openings in the drum liner lid as well as model assumptions have been described in earlier software validation documentation.¹ The equations were developed to describe the existence of potentially four layers of confinement – the drum, a liner, a large polymer liner bag, and small polymer bags. The program user was able to specify whether or not small bags were present inside the large liner bag. Only one mechanism for VOC transport across the confinement was assumed in each layer of confinement. There was no capability in the program for the user to specify more than one VOC transport mechanism in a given layer of confinement such as in the case of polymer bags with bag filter vents.

The steady-state concentrations in a waste drum can be efficiently determined algebraically knowing the parameters that affect VOC transport across each layer of confinement. In addition, this approach can account for multiple means of transport across a layer of confinement. In a vented drum, the steady-state rate of VOC transport from the drum can be defined knowing the drum headspace and drum filter vent VOC diffusion characteristic. Also during steady-state conditions, the rates of VOC transport across each layer of confinement are equal. The steady-state concentration in the drum headspace, y_{DH} , can be defined in terms of the VOC transport characteristic across the drum filter vent, D_N^* , the VOC concentration within the innermost layer of confinement, y_1 , and the VOC transport characteristics, K_i , across N layers of confinement in an algebraic equation:

$$y_{DH} = y_1 [D_N^* \sum_{i=1}^N (1/K_i)]^{-1} \quad (1)$$

If the VOC concentration within the innermost layer of confinement is assumed to remain constant as the result of the surrounding gas phase in equilibrium with the VOC-containing waste, the relative concentration in the drum headspace is defined by rearranging Eqn (1)

$$\frac{y_{DH}}{y_1} = [D_N^* \sum_{i=1}^N (1 / K_i)]^{-1} \quad (2)$$

The use of the relative concentration to define the VOC concentration in the drum headspace eliminates the need to know the exact initial concentration within the innermost layer of confinement.

The effective VOC transport characteristic, K_i , across a layer of confinement reflects the combined contributions of VOC diffusion and permeation, and is defined as

$$K_i = K_{p,i} + K_{d,i} + D_i^* \quad (3)$$

where $K_{p,i}$, $K_{d,i}$, and D_i^* are the VOC permeation, diffusion, and filter vent transport characteristics, respectively, across the i^{th} layer of confinement. In the case where one or more of these transport mechanisms does not occur (i.e., no filter vent present), the corresponding term is set to zero. The units of each term are mol s^{-1} . The units are sometimes alternatively expressed as $\text{mol s}^{-1} (\text{mol frac})^{-1}$ reflecting the fact that the product of these terms and the VOC mol fraction difference across a layer of confinement defines the molar rate of VOC transport across the layer of confinement.

The VOC permeation characteristic, $K_{p,i}$, is defined as

$$K_{p,i} = \frac{\Phi A_{p,i} P \rho}{x_{p,i}} \quad (4)$$

where

Φ = $4.46 \times 10^{-5} \text{ mol cm}^{-3}(\text{STP})$, gas concentration at standard conditions (STP)

$A_{p,i}$ = permeable surface area of layer of confinement, cm^2

P = gas pressure, cm Hg

ρ = VOC permeability coefficient, $\text{cm}^3(\text{STP}) \text{ cm cm}^{-2} \text{ s}^{-1} (\text{cm Hg})^{-1}$

$x_{p,i}$ = thickness of permeable surface area, cm

The VOC diffusion characteristic, $K_{d,i}$, is defined as

$$K_{d,i} = \frac{A_{d,i} D c}{x_{d,i}} \quad (5)$$

where

$A_{d,i}$ = opening surface area in confinement layer across which gas diffuses, cm^2

D = VOC diffusivity coefficient, $\text{cm}^2 \text{ s}^{-1}$

c = gas concentration, mol cm^{-3}

$x_{d,i}$ = thickness of permeable surface area, cm

The VOC diffusion characteristic across a filter vent was calculated knowing the VOC-to-hydrogen diffusivity ratio and the hydrogen diffusion characteristic of the filter vent

$$D_i^* = \frac{D}{D_{H_2}} D_{H_2}^* \quad (6)$$

The diffusivity ratio can be calculated using measured or estimated diffusivity values. In the case where the ratio is estimated using the molecular weight (MW), critical temperature (T_c), and critical pressure (P_c) of hydrogen and the VOC, the ratio is calculated with the following expression:

$$\frac{D}{D_{H_2}} = \frac{(T/298.15)^{1.823}}{P} \left(\frac{P_{c,voc}}{P_{c,H_2}} \right)^{1/3} \left(\frac{T_{c,H_2}}{T_{c,voc}} \right)^{1/2} \left(\frac{\frac{1}{MW_{air}} + \frac{1}{MW_{voc}}}{\frac{1}{MW_{air}} + \frac{1}{MW_{H_2}}} \right)^{1/2} \quad (7)$$

All temperatures are in units of K and pressure is in units of atm.

The DAC is the time required to achieve 90% of the steady-state concentration. The transient behavior of the VOC concentration within a waste drum given a set of initial conditions is modeled by solving a set of differential equations that define the rate of VOC transport across each layer of confinement. The rate of VOC transport across each layer of confinement equals

$$r_i = \frac{\partial(c_i)}{\partial t} = K_i \Delta y_i c \quad (8)$$

where

r_i = rate of VOC across i^{th} layer of confinement

Δy_i = VOC concentration difference across i^{th} layer of confinement, mol fraction

In addition to equations of the form in Eqn (6) for each layer of confinement, VOC solubility in the drum liner is accounted for by the following equation:

$$r_L = \frac{\partial(c_L)}{\partial t} = \eta \Phi V_p P [s_\infty - s] \quad (9)$$

where

r_L = rate of VOC accumulation in the drum liner, mol s^{-1}

c_L = VOC concentration in the drum liner, mol cm^{-3}

η = transfer coefficient, s^{-1}

V_p = volume of drum liner polymer, cm^3 polymer

$$s_{\infty} = \text{VOC equilibrium solubility in liner polymer,} \\ [\text{cm}^3(\text{STP VOC})(\text{cm}^{-3} \text{ polymer}) (\text{cm Hg})^{-1}]$$

$$s = \text{average VOC solubility in liner polymer,} \\ [\text{cm}^3(\text{STP VOC})(\text{cm}^{-3} \text{ polymer}) (\text{cm Hg})^{-1}]$$

The VOC equilibrium concentration is a function of the volume-average VOC mole fraction in the gas surrounding the liner, y_v

$$s_{\infty} = \frac{y_v}{H^*} \quad (10)$$

where H^* is the VOC Henrys constant in the drum liner. The transfer coefficient and Henrys constant for each VOC in the polyethylene drum liner was measured experimentally or estimated.⁴

The modified version of VDRUM1 will be referred to as VDRUM2. The VDRUM2 code is listed in Appendix A.

4.2.2 Modification to Data Input File

After specifying the name of the input and output file in the first line (each name in single quotes), the user now specifies the total number of VOCs being considered, the number of layers of confinement, and the number of rigid drum liners (zero or one) in the drum. This tells the code whether or not it needs to consider VOC solubility in the liner. The VOC solubility in all other layers of confinement is considered negligible. For example, the first two lines of an input file may look like

```
'zbase','zbase.out'
12,4,1
```

Two lines of data then follow this information for each VOC. The first line contains the name of each VOC as well as the initial concentration inside each layer of confinement. In the case of newly packaged waste drums, the concentration within the first, or innermost, layer of confinement is set to a nonzero value while the concentration in all other layers are set to zero. The next line specifies the VOC molecular weight, permeability in polyethylene ($\text{cm}^3(\text{STP}) \text{ cm cm}^{-2} \text{ s}^{-1} (\text{cm Hg})^{-1}$), VOC diffusivity in air at 25°C (if known) ($\text{cm}^2 \text{ s}^{-1}$), VOC critical temperature (K), VOC critical pressure (atm), VOC Henrys constant in the drum liner [$(\text{cm}^3 \text{ polymer}) \text{ atm cm}^{-3}(\text{STP}) \text{ VOC}$], and VOC mass transfer coefficient (s^{-1}) at the drum liner surface. The known, measured, or estimated values of these parameters for 29 VOCs have been collected.^{1,4} An example of VOC input data is listed for toluene

```
'toluene',1000.,0.,0.,0.
92.1,669.e-10,0.0849,594.,41.6,0.002857,7.e-6
```

In code validation and verification, the ratio of VOC-to-hydrogen diffusivity ratio across a filter vent was estimated using the molecular weight, critical temperature, and critical pressure of the VOC.

After all VOC-specific parameters have been specified, the parameters for each layer of confinement are entered beginning with the first layer of confinement. These parameters include (in order) the permeable surface area (cm^2), the diffusion cross-sectional area (cm^2), the total void volume within the layer of confinement (cm^3), the thickness of the permeable surface (cm), the diffusional length (cm), and the hydrogen filter vent diffusion characteristic (mol s^{-1}). If any of these terms are not

applicable for a given layer, they are to be set to zero. Typical data for a layer of confinement consisting of several layers of similar small polymer liner bags are listed below:

14000.,0.,0.,0.038,0.,0.

The parameter values used in the waste drum configurations considered in earlier DAC calculations have been summarized.^{1,4} The total permeable area of multiple small bags is estimated to be the total area of all small bags. Values of zero indicate that the parameter is not applicable. Knowledge of the void volume is not required for the first layer of confinement (VOC concentration assumed to be constant). If waste is typically wrapped in multiple layers of bags, the total bag thickness is assumed to be the sum of the bag thicknesses.

Finally, in the last line of the input file, the temperature (°C), pressure (cm Hg), fraction of the drum headspace steady-state concentration to achieve before terminating the code, and the total number of days to calculate the drum headspace concentration are specified. The calculations will stop when one of the two stop criteria are met. If the user wants to determine the DAC to achieve a specific relative concentration, the total number of days should be set to zero. If the user wants to determine the extent of VOC transport in a given time period, the fraction quantity in the last line of the data input file should be set to unity. Both values can be specified if the user wants the code to stop when either one of the criteria is met. In the case of calculating the DAC only at typical conditions, the input file would contain the following information:

25.,76.,0.9,0

If the user wished to determine the relative headspace concentration after 75 days, the input data would read as follows:

25.,76.,1.,75

4.2.3 Validation of DAC Calculations

The validity of the change in the program was determined by comparing the VDRUM2 results predicting the drum age criteria for newly packaged waste drums with results obtained using VDRUM1.¹ A comparison of input and output data files for VDRUM1 and VDRUM2 calculating DAC values for 12 indicator VOCs in identical packaging configurations and packaging scenarios are summarized in Appendix B. The DACs vary by a few days for VOCs that estimated the VOC-to-hydrogen diffusivity ratio using an estimated VOC diffusivity (input files to VDRUM2) instead of value specified by the user (input files to VDRUM1). In the case of toluene, the DAC values calculated using VDRUM1 were 142 and 225 days for the two configurations. The results of VDRUM2 for the same packaging configurations were 142 and 226 days, respectively.

The steady-state concentrations for VOCs that used critical properties to determine the VOC-to-hydrogen diffusivity ratio from VDRUM2 were consistently lower than values calculated in VDRUM1. This is attributed to the change in the calculated VOC diffusion characteristic across the filter vent. For those VOCs where the diffusivity ratio was calculated using the same information, the steady-state concentrations calculated in VDRUM2 were slightly greater than those calculated in VDRUM1. The exact steady-state concentration is calculated in VDRUM2 while an algorithm in VDRUM1 selects a concentration that is not significantly different than the last value calculated. This algorithm inherently will identify a steady-state concentration less than the actual value.

4.2.4 Model Verification

The steady-state concentration for a VOC is calculated using the input parameters specified in the input file and Eqns (2-7). Using input data in ZBASEII for toluene, the following values are calculated:

Layer 1: $K_1 = K_{p,1} = (\Phi A_{p,1} P \rho) / x_{p,1}$

$A_{p,1} = 14000 \text{ cm}^2$; $P = 76 \text{ cm Hg}$; $\rho = 669 \text{e-}10 \text{ cm}^3(\text{STP}) \text{ cm cm}^{-2} \text{ s}^{-1} (\text{cm Hg})^{-1}$; $x_{p,1} = 0.038 \text{ cm}$
 $K_{p,1} = 4.46\text{e-}5 (14000) (76) (669\text{e-}10)/(0.038) = 8.35\text{e-}5 \text{ mol/s}$

Layer 2: $K_2 = K_{p,2} = (\Phi A_{p,2} P \rho) / x_{p,2}$

$A_{p,2} = 14000 \text{ cm}^2$; $P = 76 \text{ cm Hg}$; $\rho = 669 \text{e-}10 \text{ cm}^3(\text{STP}) \text{ cm cm}^{-2} \text{ s}^{-1} (\text{cm Hg})^{-1}$; $x_{p,2} = 0.056 \text{ cm}$
 $K_{p,2} = 4.46\text{e-}5 (14000) (76) (669\text{e-}10)/(0.056) = 5.67\text{e-}5 \text{ mol/s}$

Layer 3: $K_3 = K_{d,3} = (A_{d,3} D_c) / x_{d,3}$

$A_{d,3} = 0.71 \text{ cm}^2$; $D = 0.0849 \text{ cm}^2 \text{ s}^{-1}$; $c = P/RT$; $P = 76 \text{ cm Hg}$; $T = 25^\circ\text{C} = 298 \text{ K}$;
 $R = 6236 \text{ cm}^3 (\text{cm Hg}) \text{ mol}^{-1} \text{ K}^{-1}$; $x_{d,3} = 1.2 \text{ cm}$
 $K_{d,3} = 0.71 (0.0849) (76/(298)(6236))/1.2 = 2.05\text{e-}6 \text{ mol/s}$

Layer 4: $K_4 = D_4^* = (D / D_{H_2}) D_{H_2}^*$

$$\frac{D}{D_{H_2}} = \frac{(T / 298.15)^{1.823}}{P} \left(\frac{P_{c,voc}}{P_{c,H_2}} \right)^{1/3} \left(\frac{T_{c,H_2}}{T_{c,voc}} \right)^{1/2} \left(\frac{\frac{1}{MW_{air}} + \frac{1}{MW_{voc}}}{\frac{1}{MW_{air}} + \frac{1}{MW_{H_2}}} \right)^{1/2}$$

$T = 298.15 \text{ K}$; $P = 1 \text{ atm}$; $P_{c,voc} = 41.6 \text{ atm}$; $P_{c,H_2} = 12.8 \text{ atm}$; $T_{c,H_2} = 33.3 \text{ K}$; $T_{c,voc} = 594 \text{ K}$; $MW_{air} = 29$;
 $MW_{voc} = 92.1$; $MW_{H_2} = 2.016$; $D_{H_2}^* = 42.\text{e-}7 \text{ mol/s}$

$$\frac{D}{D_{H_2}} = (1)(41.6/12.8)^{0.3333} (33.3/594)^{0.5} [(1/29+1/92.1)/(1/29+1/2.016)]^{0.5} = 0.1025$$

$K_4 = (0.1025)(42.\text{e-}7) = 4.30\text{e-}7 \text{ mol/s}$

$$\frac{y_{DH}}{y_1} = [4.3\text{e-}7(1.20\text{e}4 + 1.76\text{e}4 + 4.88\text{e}5 + 2.33\text{e}6)]^{-1} = 0.8180$$

Given $y_1 = 1000 \text{ ppmv}$, $y_{DH} = 818.0 \text{ ppmv}$.

From ZBASEII.OUT, the steady-state concentration for toluene = 818.0 ppmv

4.2.5 System Limitations

The primary system limitation is the requirement that the computer code has access to an IMSL mathematical library containing the called subroutine, written in FORTRAN, designed to solve a series of ordinary differential equations. Currently, a Visual FORTRAN compiler with an IMSL mathematical library is used to compile the computer code. In the past, as a result of hardware upgrades, previous FORTRAN compilers became obsolete. This required that a new FORTRAN compiler be acquired. There

is always a risk that the current FORTRAN compiler may become incompatible with future computer hardware. It is the responsibility of the user and maintenance support to insure that this situation is avoided.

4.2.6 Anticipated Errors

No computational errors are anticipated.

4.2.7 User and Maintenance Support

As of June 30, 2000, user and maintenance support of the computer code is provided by Andrea Chambers at the Idaho National Engineering and Environmental, Idaho Falls, Idaho. A copy of the computer codes as well as a record log will be maintained to record any code updates. If the software is significantly changed, baseline validation will be performed to determine if there is any significant or undesirable impact on software input.

5. REFERENCES

1. K.J. Liekhus, 1995, "Validation of gas transport modeling computer codes", INEL-95/121, Idaho National Engineering Laboratory, Idaho Falls, ID.
2. *Safety Analysis Report for the TRUPACT-II Shipping Package*, 1999, Rev. 18, Westinghouse Electric Corporation, Waste Isolation Division, Carlsbad, NM.
3. *Handbook of Chemistry and Physics*, 59th ed., 1979, CRC Press, Boca Raton, FL.
4. M.J. Connolly et al., 1998, *Position for Determining Gas Phase Volatile Organic Compound Concentrations in Transuranic Waste Containers*, INEEL-95/0109, Rev. 2, LMITCO, Idaho Falls, ID.

Appendix A

Appendix A

```
c*****
c***** VDRUM2.FOR = "VDRUM.FOR (Rev. 2)" *****
c
c Original program written by: Kevin J. Liekhus
c           Lockheed Idaho Technologies, Co.
c           Idaho National Engineering Laboratory
c Date: April 26, 1995
c*****
c*** Modified: 06/15/2000
c*** Modifications:
c 1) Program now calculates time to achieve percentage of steady-state
c    concentration in drum with or without drum liner, with up to
c    four (4) other layers of confinement through which VOCs may
c    permeate the surface (polymer bag), diffuse across an opening,
c    or diffuse across a filter vent.
c 2) Option to calculate percentage of steady-state concentration after
c    specified number of days.
c 3) Steady concentration is calculated directly based on the
c    waste drum configuration
c 4) Eliminate cases where gas generation is considered
c 5) Eliminate case of newly packaged, unvented drum/liner
c*****

c---- Model of gas transport in vented and unvented waste drums
c---- calculates time when gas concentration in drum headspace is within
c---- x% of the steady-state gas concentration. (Variable x defined by user)
c
c---- This program is written in FORTRAN and utilizes an IMSL FORTRAN
c---- subroutines for mathematical applications. The IMSL subroutine (IVPAG)
c---- solves a series of first-order ordinary differential equations.
c
c---- MODEL ASSUMPTIONS AND IMPORTANT FEATURES -----
c---- : Ideal gas behavior
c---- : Constant temperature in waste drum
c---- : Gas concentration throughout a void volume is uniform at all times
c---- : Drum configuration: waste drum, rigid drum liner (optional),
c----   and one to four additional layers of confinement
c---- : In case of multiple layers of bags (of same size), treat as one
c----   bag with thickness equal to sum individual bag thicknesses
c---- : In case of multiple layers of bags, each with a filter vent,
c----   define a single-bag filter vent diffusion characteristic =  $D^*/n$ 
c----   (filter vent diffusion char. divided by the number of bags)
c---- : In all layers of confinement (excluding drum liner and drum)
c----   Permeation of the gas, diffusion of gas across an opening,
c----   and diffusion of gas across filter vent are modeled.
c---- : In the case of multiple innermost layers of confinement
c----   (i.e., many small bags containing waste), the innermost layer
c----   of confinement is treated as a single volume with a surface area
```

c----- and filter diffusion characteristic equal to the sum of these
 c----- values from the individual packages.
 c----- : In drum liner, gas diffuses across opening or filter vent in
 c----- drum liner lid.
 c----- : Diffusion of gas across drum filter vent is primary means
 c----- of transport out of the drum
 c----- : All filter vents are characterized by hydrogen
 c----- diffusion characteristic (mol/s)
 c----- : Gas/vapor solubility in drum liner characterized by
 c----- Henry's constant
 c----- : Gas/vapor solubility in drum liner is assumed to be a linear
 c----- function of the volume-averaged VOC gas-phase concentration
 c----- between drum liner void volume and void volume outside the liner
 c----- : Dissolved gas concentration in drum liner is uniform
 c----- (not necessarily constant) at all times
 c----- : All model parameter inputs remain constant.
 c----- : Gear's backward difference method used to solve series of
 c----- ordinary differential equations
 c----- : Initial conditions
 c----- - Gas concentrations within each void volume (specified by user)
 c----- - Dissolved gas concentration in drum liner is initially defined
 c----- in terms of the initial gas concentration in drum liner headspace
 c----- : Boundary conditions
 c----- 1) VOC concentration, outside drum filter vent = 0
 c----- 2) VOC concentration, innermost layer of confinement = constant

```

c*****
c***** MAIN PROGRAM *****
c*****
  
```

```

    character*32 test,ifname,ofname,vocid(35)
    real aa(1,1),yy(35,7),yz(7),y(7),k
    real pm(35),df(35),amw(35),tc(35),pc(35),h(35),ak(35)
    real param(50),ap(7),ad(7),v(7),xp(7),xd(7),dfh(7)
    integer ivoc(35)
    common/qq/p,d,ap,ad,v,xp,xd,dfh,dfr,pHg,temp0,c0,s0,k,nlin
    external fcn,ivpag,sset
  
```

```

c*****
c***** USER-SUPPLIED INPUT *****
c*****
  
```

```

c-----
c specify input data file name
c-----
    write(*,9)
    9 format(1x,'Enter name of input data file ')
    read(*,*)ifname
    open(unit=3,file=ifname,status='unknown')
  
```

```

c-----
c reading of input data file
c-----
  
```

```

c----- User provided input
c----- test - text or title describing contents of input data file
c----- ofname - output file name
c----- ncom - number of compounds in gas phase of innermost layer
c----- nlay - total number of layers of confinement
c----- nlin - total number of drum liners in waste drum (0 or 1)
c----- vocid - name of gas or VOC
c----- yy(i,n) - i-th VOC concentration (ppmv) in n-th layer of confinement
c-----      n=1, headspace within innermost layer of confinement
c-----      subsequent layers of confinement are numbered 2, 3, etc.
c----- amw(i) - gas/VOC molecular weight
c----- pm(i) - gas/VOC permeability coefficient in polymer bag,
c-----      cm3(STP) cm/(cm2 s cm Hg)
c----- df(i) - gas/VOC diffusivity in air, cm2/s
c----- tc(i) - critical temperature of gas or VOC, K
c----- pc(i) - critical pressure of gas or VOC, atm
c----- h(i) - gas/VOC Henry's constant for drum liner,
c-----      cm3 polymer atm/cm3 (STP) gas
c----- ak(i) - gas/VOC mass transfer coefficient at drum liner surface, 1/s
c----- ap(n) - total permeable surface area (cm2) of n-th layer of confinement
c----- ad(n) - cross-sectional area of opening (cm2) across n-th layer
c----- v(n) - void volume within n-th layer of confinement (cm3)
c----- xp(n) - permeable surface thickness (cm) of n-th layer
c----- xd(n) - diffusional path length (cm) across n-th layer of confinement
c----- dfh(n) - vent hydrogen diffusion characteristic of n-layer, mol/s
c----- temp - drum temperature, C
c----- pHg - atmospheric pressure, cm Hg
c----- yssfrac - fraction of drum headspace steady-state concentration,
c-----      for which the time required to reach this fraction is calculated
c-----      if program ends after simulating (nday) days, set yssfrac=1.0
c----- nday - number of days over which to calculate model results,
c-----      if want to calculate to specific value of yssfrac, set nday=0
c
  read(3,*)test,ofname
  read(3,*)ncom,nlay,nlin
  do 8 i=1,ncom
    read(3,*)vocid(i),(yy(i,j),j=1,nlay)
    read(3,*)amw(i),pm(i),df(i),tc(i),pc(i),h(i),ak(i)
  8 continue
  read(3,*)(ap(j),ad(j),v(j),xp(j),xd(j),dfh(j),j=1,nlay)
  read(3,*)temp,pHg,yssfrac,nday
c*****
c***** INITIALIZATIONS AND CONVERSIONS *****
c*****
c----- r0 - gas constant (82.06 cm3 atm/mol K)
c----- patm - atmospheric pressure, atm
c----- temp0 - initial drum temperature, K
c----- c0 - initial ideal gas concentration in drum, mol/cm3
  r0=82.06
  patm=pHg/76.0
  temp0=temp+273.15

```

```

c0=patm/(r0*temp0)
c-----
c opening of output data file
c-----
    open(unit=2,file=ofname,status='unknown')
    write(2,15)test
15  format(1x,a32)
c-----
c write header to output file
c-----
    write(2,143)
143  format(27x,'N(days)',2x,'[]@N',4x,'[]@SS',3x,'0.9[]SS/[]N')
c-----
c calculate i-th compound concentrations throughout waste drum
c-----
    do 43 i=1,ncom
c calculate diffusion properties for VOC/gas
c *****
        CALL VPROP(amw(i),tc(i),pc(i),df(i),dfr,c0,h(i),s0,temp0,patm)
c *****
c----- calculate steady-state concentration for i-th compound
    sumi=0
    do 33 j=1,(nlay-nlin)-1
        a=0.
        b=0.
        if(ap(j).ne.0.)a=4.46e-5*pm(i)*ap(j)*pHg/xp(j)
        if(ad(j).ne.0.)b=(df(i)*ad(j)/xd(j))*c0
        sum=a+b+dfr*dfr(j)
        sumi=sumi+1./sum
33  continue
    if(nlin.eq.1)then
        blin=(df(i)*ad(nlay-1)/xd(nlay-1))*c0+dfr*dfr(nlay-1)
        sumi=sumi+1./blin
    end if
    dvent=dfr*dfr(nlay)
    sumi=sumi+1./dvent
    yss=yy(i,1)/(dvent*sumi)
c-----
c calculate drum headspace gas concentration as a function of time
c-----
c----- IMSL subroutines and parameters
c----- SSET - IMSL subroutine (sets a vector to a constant value)
c----- IVPAG - IMSL subroutine (initial-value ODE solver)
c----- ido - flag indicating state of computation
c----- a(1,1) - matrix used when ODE system is implicit
c----- tend - value of t at which solution is desired
c----- tol - tolerance for error control
c----- param - vector of length 50 containing optional parameters,
c-----         model parameters set to default values
c----- param(4) - maximum number of steps allowed
c----- param(10) - switch determining error norm

```

```

c----- param(12) - method indicator
c-----      1 = Adams' method;
c-----      2 = Gear's backward difference method
c initialize IMSL parameters, set param to default values
      mxparm=50
      CALL SSET(mxparm,0.0,param,1)
      param(4)=10000000
      param(10)=2
      param(12)=2
      ido=1
      tol=1.e-6
c----- initialization of other variables
c----- yz(n) - VOC concentration in n-th layer of confinement, mol/cm3
c----- yz(nlay+1) - VOC concentration in drum liner, cm3 VOC/cm3 polymer
c----- y(n) - VOC concentration in n-th layer of confinement, ppm
c----- t - time (sec)
c----- nc - number of days simulated in program
c----- ndac - time to achieve fixed percentage of steady-state conc.
c----- yss - steady-state gaseous compound conc. in outermost layer
c----- rr - DAC concentration, ppm
c----- zneq - VOC concentration in outermost layer on (nc-1)th day
c----- p - gas/VOC permeability coefficient in polymer bag,
c-----      cm3(STP) cm/(cm2 s cm Hg)
c----- d - gas/VOC diffusivity in air, cm2/s
c----- dvent - gas/VOC diffusion characteristic across drum filter vent,
c-----      mol/s/(fraction)
c----- k - gas/VOC mass transfer coefficient at drum liner surface, 1/s
c----- fcn - user-supplied subroutine to evaluate functions
c----- fcnj - user-supplied subroutine to compute the Jacobian
      t=0.
      nc=1
      nq=nlay+nlin
c convert gas concentration from ppmv to mol/cm3
      do 37 j=1,nlay
        yz(j)=yy(i,j)*c0*1.e-6
      37 continue
c
c----- VPROPS - subroutine calculate VOC properties not specified
c----- df - VOC diffusivity in air, cm2/s
c----- difr - ratio of VOC-to hydrogen diffusivity
c----- s0 - gas pressure/(total gas concentration*VOC Henry's constant),
c-----      [(cm3 VOC(STP)/(cm3 polymer))/(mol/cm3)]
c*****
      CALL VPROP(amw(i),tc(i),pc(i),df(i),dfr,c0,h(i),s0,temp0,patm)
c*****
      if(nlin.eq.1) yz(nlay+1)=yz(nlay-1)*s0
      p=pm(i)
      d=df(i)
      k=ak(i)

```

```

c*****
c***** MODEL CALCULATIONS *****
c*****
20  if(p.gt.50.e-10)then
c----- dt - time interval (sec)
        dt=120.*50.e-10/p
        if(dt.lt.12.)dt=12.
        else
        dt=120.*5.e-10/p
        end if
c----- tend - total time (sec)
        tend=t+dt
c
        CALL IVPAG(ido,nq,fcn,fcnj,aa,t,tend,tol,param,yz)
c
c***** MODEL OUTPUT *****
c*****
c-----
c output (every simulated 24 hrs)
c-----
        if(ifix((tend+0.1)/86400).eq.nc)then
            y(nlay)=(yz(nlay)/c0)*1.e6
c test if concentration or time quit criteria are met
            if((y(nlay).gt.yssfrac*yss).or.(nc.eq.nday))then
                ndac=nc
                rr=y(nlay)
            else
                nc=nc+1
                goto 20
            end if
        else
            goto 20
        end if
c-----
c write to output data file
c-----
        write(2,34)vocid(i),ndac,rr,yss,(0.9*yss)/rr
34  format(1x,a25,2x,i4,2x,f7.2,2x,f7.2,5x,f5.1)
c-----
c NOTE:
c Ratio [(0.9*yss)/rr] equals [VOC conc.@ndac/VOC conc.@90%ofSS]
c Thus, if DAC was determined at 90% of SS, ratio = 1.0
c-----
c final call to release workspace
c-----
        ido=3
        CALL IVPAG(ido,nq,fcn,fcnj,aa,t,tend,tol,param,yz)
43 continue
end

```

```

SUBROUTINE FCN(neq,t,y,yp)
real y(neq),yp(neq),p,d,ap(7),ad(7),v(7),xp(7),xd(7),dfh(7),k
common/qq/p,d,ap,ad,v,xp,xd,dfh,dfr,pHg,temp0,c0,s0,k,nlin

```

```

c-----
c----- MODEL EQUATION ASSUMPTIONS
c----- : VOC concentration within innermost layer of confinement remains
c----- constant; therefore yp(1)=0
c----- : VOC equilibrium concentration in drum liner is defined in terms
c----- of a volume-average VOC concentration in the void volumes
c----- (drum liner and drum headspaces) surrounding the drum liner
c-----
c----- neq - number of ordinary differential equations
c----- t - independent variable, time (s)
c----- y(i) - dependent variable: (i=1,neq-1) = gas VOC concentration (mol/cm3)
c----- (i = neq) VOC concentration in polymer (cm3 VOC/cm3 polymer)
c----- yp - first derivative of y with respect to t
c----- a = 4.46e-5*p*ap(i)*pHg/xp(i), mol/s
c----- b = c0*d*ad(i)/xd(i), mol/s
c----- dvent = dfr*dfh(i), mol/s
c----- q - rate of VOC transport from layer of confinement, mol/s
c----- g4 - fraction of VOC in drum liner headspace of all VOC in both
c----- drum liner and drum headspaces
c----- g5 = 1 - g4
c----- vp - volume of polymer in drum liner, cm3
c----- s - VOC equilibrium concentration in drum liner as defined in terms
c----- of volume-average VOC concentration surrounding drum liner, cm3 VOC/cm3
c----- s0 - VOC equilibrium concentration in drum liner as defined in terms
c----- of VOC vapor pressure in saturated vapor, cm3 VOC/cm3
c----- stp - gas concentration (mol/cm3) at standard temperature (273.15 K)
c----- and pressure (1 atm) = 1./(82.06*273.15) = 4.461e-5 mol/cm3
c----- dvent - VOC diffusion characteristic, mol/s
c----- k - VOC mass-transfer coefficient, 1/s
c-----
c----- i-th layer of confinement (excluding drum liner, drum)
c-----
q=0.
nj=neq-2*nlin-1
do 53 j=1,nj
a=0.
b=0.
if(ap(j).ne.0.)a=4.46e-5*p*ap(j)*pHg/xp(j)
if(ad(j).ne.0.)b=(d*ad(j)/xd(j))*c0
dvent=dfr*dfh(j)
sum=a+b+dvent
yp(j)=(-q+sum*(y(j+1)-y(j))/c0)/v(j)
yp(1)=0.
q=sum*(y(j+1)-y(j))/c0
53 continue
c-----
c drum liner headspace with punctured/vented liner lid (nlin=1)

```



```

c-----
      if(nlin.eq.1)then
c-----
c be sure liner headspace concentration > 0
c-----
      if(y(nj+1).gt.1.e-12)then
        g4=y(nj+1)*v(nj+1)/(y(nj+1)*v(nj+1)+y(nj+2)*v(nj+2))
        g5=1-g4
        vp=ap(nj+1)*xp(nj+1)
        s=s0*(y(nj+1)*v(nj+1)+y(nj+2)*v(nj+2))/(v(nj+1)+v(nj+2))
      else
        s=0.
        g4=0.
        g5=0.
      end if
      b=c0*d*ad(nj+1)/xd(nj+1)
      dvent=dfh(nj+1)*dfr
      sum=b+dvent
      stp=1./(82.06*273.)
      vs=g4*vp*stp
      yp(nj+1)=(-q+sum*(y(nj+2)-y(nj+1))/c0-vs*yp(nj+3))/v(nj+1)
      q=sum*(y(nj+2)-y(nj+1))/c0
c-----
c----- drum headspace
c-----
      dvent=dfr*dfh(nj+2)
      yp(nj+2)=(-q-dvent*y(nj+2)/c0-g5*yp(nj+3)*vp*stp)/v(nj+2)
c-----
c----- polyethylene drum liner
c-----
      yp(nj+3)=k*(s-y(nj+3))
    else
c-----
c----- drum headspace (no liner)
c-----
      dvent=dfr*dfh(nj+1)
      yp(nj+1)=(-q-dvent*y(nj+1)/c0)/v(nj+1)
    end if
c
    return
  end

SUBROUTINE FCNJ(neq,t,y,dypdy)
real y(neq),dypdy(*)
return
end

```

SUBROUTINE VPROP(amw,tc,pc,df,dfr,c0,h,s0,t,pr)

```

c-----
c----- amw - gas molecular weight
c----- tc - critical temperature (K) of gas
c----- pc - critical pressure (atm) of gas
c----- df - gas diffusivity in air (at 25 C if temperature not specified)
c----- dfr - ratio of gas/Hydrogen diffusion coefficients
c----- h - gas Henry's constant, cm3 gas (STP) cm3 polymer (atm)
c----- s0 - gas pressure/(gas Henry's constant * total gas concentration)
c-----          (cm3 gas/cm3 poly)(cm3 gas/mol gas)
c----- pch - critical pressure (atm) of hydrogen
c----- tch - critical temperature (K) of hydrogen
c----- pca - critical pressure (atm) of air
c----- tca - critical temperature (K) of air
c----- h2mw - molecular weight of hydrogen
c----- airmw - molecular weight of air
c----- smw = 1/airmw + 1/h2mw = 0.5305
c----- pt - P, T correction relative to 1 atm, 298.15K (25C)
c
    pch=12.8
    tch=33.3
    pca=36.4
    tca=132.
    h2mw=2.016
    airmw=29.
c-----
c
    if(df.eq.0)then
        if(tc.ne.0.)then
            smw=1./airmw+1/h2mw
            samw=sqrt(1./airmw+1/amw)
            sqmw=samw/sqrt(smw)
            df=2.745e-4*(t**1.823/pr)*(pc*pca)**(1./3.)*samw/sqrt(tca*tc)
        end if
    end if
c
    smw=1./airmw+1/h2mw
    samw=sqrt(1./airmw+1/amw)
    sqmw=samw/sqrt(smw)
    pt=(1./pr)*(t/298.15)**1.823
    dfr=pt*((pc/pch)**(1./3.)*(tc/tch)**(-0.5)*sqmw)
c
    if(h.ne.0.)then
        s0=pr/(c0*h)
    else
        s0=0.
    end if
c
    return
end

```

Appendix B

Appendix B

The output from VDRUM2 is compared to output from VDRUM1 identical waste packaging configurations and packaging scenarios. Two waste packaging configurations are evaluated. One configuration consists of a vented drum, drum liner, polymer liner bags, and small polymer bags surrounding the waste as seen in drums containing in Type II (inorganic solids) and Type III (organic solids) waste. The other configuration considered consists of a vented drum, drum liner, and polymer liner bags in which waste is placed as seen in drums containing Type I (inorganic solidified) and Type IV (organic solidified) waste. The input/output files for each case are summarized in Table B-1.

Table B-1. Summary of input/output files for each DAC-calculating program.

	VDRUM1	VDRUM2
Waste Type II/III	vbase/vbase.out	zbaseii/zbaseii.out
Waste Type I/IV	rbase/rbase.out	zbaseiv/zbaseiv.out

The content of the input and output files are listed on the following pages. In the case of VDRUM1 output, the first number listed after the name of the volatile organic compound (VOC) is the DAC value, or the number of days that are required for the drum headspace to achieve 90% of the steady-state concentration. The two numbers after the DAC value are the 90% of steady-state and steady-state VOC concentrations, respectively. Similar values are displayed in output files from VDRUM2 but are labeled more clearly. An additional number is displayed in VDRUM2 output. This number is the ratio of the 90% of steady-state VOC concentration to the VOC concentration achieved at the DAC value. In these cases, the ratio should equal unity.

INPUT FILE (VBASE) to VDRUM.FOR
 baseline for Waste Types II/III, 12 VOCs considered
 newly packaged, vented 55-gal waste drums
 all parameters defined in INEL-95/0109, Rev. 2

```
'vbase','vbase.out',12
'carbon tetrachloride',1000.,0.,0.,0.
153.82,193.e-10,0.0828,0.,0.,3.03e-7,0.0217,6.e-5,0.
'methanol',1000.,0.,0.,0.
32.0,135.e-10,0.152,0.,0.,6.05e-7,0.0272,2.4e-7,0.
'dichloromethane',1000.,0.,0.,0.
84.9,263.e-10,0.104,0.,0.,4.43e-7,0.0431,2.e-6,0.
'toluene',1000.,0.,0.,0.
92.1,669.e-10,0.0849,0.,0.,3.66e-7,0.002857,7.e-6,0.
'trichloroethylene',1000.,0.,0.,0.
131.4,583.e-10,0.0875,0.,0.,3.2e-7,0.00640,6.e-5,0.
'butanol',1000.,0.,0.,0.
74.1,300.e-10,0.,563.1,43.6,0.,0.02273,8.e-6,0.
'chloroform',1000.,0.,0.,0.
119.4,260.e-10,0.,536.4,53.0,0.,0.04545,8.e-6,0.
'1,1-dichloroethene',1000.,0.,0.,0.
96.9,110.e-10,0.,513.0,47.5,0.,0.09091,8.e-6,0.
'methyl ethyl ketone',1000.,0.,0.,0.
72.1,165.e-10,0.,536.8,41.5,0.,0.03704,8.e-6,0.
'methyl isobutyl ketone',1000.,0.,0.,0.
100.2,130.e-10,0.,571.0,32.3,0.,0.01724,8.e-6,0.
'1,1,2,2-tetrachloroethane',1000.,0.,0.,0.
167.9,2300.e-10,0.,661.2,57.6,0.,0.003846,8.e-6,0.
'chlorobenzene',1000.,0.,0.,0.
112.6,600.e-10,0.,632.4,44.6,0.,0.007692,8.e-6,0.
14000.,0.,0.,0.038,0.
14000.,0.,20000.,0.056,0.
15500.,0.71,40000.,0.229,1.2
0.,0.,28000.,0.,0.
25.,76.,42.e-7
```

c baseline for Waste Types II/III, 12 VOCs considered
 c newly packaged, vented 55-gal waste drums
 c all parameters defined in INEL-95/0109, Rev. 2

OUTPUT FILE (VBASE.OUT) FROM VDRUM.FOR (INPUT FILE = VBASE)

vbase		
carbon tetrachloride	51 762.5723	845.3864
methanol	64 718.2869	797.6616
dichloromethane	32 744.8869	826.5574
toluene	142 752.3510	835.4522
trichloroethylene	74 773.9573	858.1149
butanol	40 717.7332	793.4727
chloroform	29 714.6116	789.9650
1,1-dichloroethene	32 684.3615	759.8938
methyl ethyl ketone	39 701.5074	777.8983
methyl isobutyl ketone	76 699.6860	774.9249
1,1,2,2-tetrachloroethane	81 725.5580	803.9965
chlorobenzene	68 724.5751	803.2201

INPUT FILE (RBASE) to VDRUM.FOR
baseline for Waste Types I/IV, 12 VOCs considered
newly packaged, vented 55-gal waste drums
all parameters defined in INEL-95/0109, Rev. 2

```
'rbase','rbase.out',12
'carbon tetrachloride',0.,1000.,0.,0.
153.82,193.e-10,0.0828,0.,0.,3.03e-7,0.0217,6.e-5,0.
'methanol',0.,1000.,0.,0.
32.0,135.e-10,0.152,0.,0.,6.05e-7,0.0272,2.4e-7,0.
'dichloromethane',0.,1000.,0.,0.
84.9,263.e-10,0.104,0.,0.,4.43e-7,0.0431,2.e-6,0.
'toluene',0.,1000.,0.,0.
92.1,669.e-10,0.0849,0.,0.,3.66e-7,0.002857,7.e-6,0.
'trichloroethylene',0.,1000.,0.,0.
131.4,583.e-10,0.0875,0.,0.,3.2e-7,0.00640,6.e-5,0.
'butanol',0.,1000.,0.,0.
74.1,300.e-10,0.,563.1,43.6,0.,0.02273,8.e-6,0.
'chloroform',0.,1000.,0.,0.
119.4,260.e-10,0.,536.4,53.0,0.,0.04545,8.e-6,0.
'1,1-dichloroethene',0.,1000.,0.,0.
96.9,110.e-10,0.,513.0,47.5,0.,0.09091,8.e-6,0.
'methyl ethyl ketone',0.,1000.,0.,0.
72.1,165.e-10,0.,536.8,41.5,0.,0.03704,8.e-6,0.
'methyl isobutyl ketone',0.,1000.,0.,0.
100.2,130.e-10,0.,571.0,32.3,0.,0.01724,8.e-6,0.
'1,1,2,2-tetrachloroethane',0.,1000.,0.,0.
167.9,2300.e-10,0.,661.2,57.6,0.,0.003846,8.e-6,0.
'chlorobenzene',0.,1000.,0.,0.
112.6,600.e-10,0.,632.4,44.6,0.,0.007692,8.e-6,0.
0.,0.,0.,0.,0.
3000.,0.,20000.,0.056,0.
15500.,0.71,40000.,0.229,1.2
0.,0.,28000.,0.,0.
25.,76.,42.e-7
```

c baseline for Waste Types I/IV, 12 VOCs considered
c newly packaged, vented 55-gal waste drums
c all parameters defined in INEL-95/0109, Rev. 2

OUTPUT FILE (RBASE.OUT) FROM VDRUM.FOR (INPUT FILE = RBASE)

rbase			
carbon tetrachloride	92	726.7985	807.4005
methanol	115	638.3188	708.3283
dichloromethane	50	710.7165	787.7477
toluene	225	738.7659	820.7675
trichloroethylene	119	759.8959	843.3984
butanol	65	686.6910	760.4871
chloroform	46	677.4800	751.3829
1,1-dichloroethene	57	613.2073	680.0746
methyl ethyl ketone	68	649.6926	721.7274
methyl isobutyl ketone	140	644.1774	714.7215
1,1,2,2-tetrachloroethane	100	716.8054	795.3849
chlorobenzene	104	710.4477	787.3361

INPUT FILE (ZBASEII) to VDRUM2.FOR

This is an input file for the program vdrum2.for. Duplication of vbase (input file for vdrum.for)

```
'zbaseii','zbaseii.out'
12,4,1
'carbon tetrachloride',1000.,0.,0.,0.
153.82,193.e-10,0.0828,556.4,45.0,0.0217,6.e-5
'methanol',1000.,0.,0.,0.
32.0,135.e-10,0.152,513.2,78.5,0.0272,2.4e-7
'dichloromethane',1000.,0.,0.,0.
84.9,263.e-10,0.104,510.,62.2,0.0431,2.e-6
'toluene',1000.,0.,0.,0.
92.1,669.e-10,0.0849,594.0,41.6,0.002857,7.e-6
'trichloroethylene',1000.,0.,0.,0.
131.4,583.e-10,0.0875,572.0,49.8,0.00640,6.e-5
'butanol',1000.,0.,0.,0.
74.1,300.e-10,0.,563.1,43.6,0.02273,8.e-6
'chloroform',1000.,0.,0.,0.
119.4,260.e-10,0.,536.4,53.0,0.04545,8.e-6
'1,1-dichloroethene',1000.,0.,0.,0.
96.9,110.e-10,0.,513.0,47.5,0.09091,8.e-6
'methyl ethyl ketone',1000.,0.,0.,0.
72.1,165.e-10,0.,536.8,41.5,0.03704,8.e-6
'methyl isobutyl ketone',1000.,0.,0.,0.
100.2,130.e-10,0.,571.0,32.3,0.01724,8.e-6
'1,1,2,2-tetrachloroethane',1000.,0.,0.,0.
167.9,2300.e-10,0.,661.2,57.6,0.003846,8.e-6
'chlorobenzene',1000.,0.,0.,0.
112.6,600.e-10,0.,632.4,44.6,0.007692,8.e-6
14000.,0.,0.,0.038,0.,0.
14000.,0.,20000.,0.056,0.,0.
15500.,0.71,40000.,0.229,1.2,0.
0.,0.,28000.,0.,0.,42.e-7
25.,76.,0.9,990
```

OUTPUT FILE (ZBASEII.OUT) FROM VDRUM2.FOR (INPUT FILE = ZBASEII)

zbaseii	N(days)	[]@N	[]@SS	0.9[]SS/[]N
carbon tetrachloride	48	713.64	792.75	1.0
methanol	63	699.13	775.99	1.0
dichloromethane	32	723.17	797.54	1.0
toluene	142	737.40	818.00	1.0
trichloroethylene	71	735.64	814.71	1.0
butanol	40	717.73	793.89	1.0
chloroform	29	714.61	790.21	1.0
1,1-dichloroethene	32	684.36	760.00	1.0
methyl ethyl ketone	39	701.51	778.08	1.0
methyl isobutyl ketone	76	699.69	775.19	1.0
1,1,2,2-tetrachloroethane	83	730.44	811.16	1.0
chlorobenzene	68	724.58	804.58	1.0

INPUT FILE (ZBASEIV) to VDRUM2.FOR

This is an input file to vdrum2.for. Duplication of rbase (an input file for vdrum.for)

'zbaseIV','zbaseIV.out'

12,3,1

'carbon tetrachloride',1000.,0.,0.

153.82,193.e-10,0.0828,556.4,45.0,0.0217,6.e-5

'methanol',1000.,0.,0.

32.0,135.e-10,0.152,513.2,78.5,0.0272,2.4e-7

'dichloromethane',1000.,0.,0.

84.9,263.e-10,0.104,510.,62.2,0.0431,2.e-6

'toluene',1000.,0.,0.

92.1,669.e-10,0.0849,594.0,41.6,0.002857,7.e-6

'trichloroethylene',1000.,0.,0.

131.4,583.e-10,0.0875,572.0,49.8,0.00640,6.e-5

'butanol',1000.,0.,0.

74.1,300.e-10,0.,563.1,43.6,0.02273,8.e-6

'chloroform',1000.,0.,0.

119.4,260.e-10,0.,536.4,53.0,0.04545,8.e-6

'1,1-dichloroethene',1000.,0.,0.

96.9,110.e-10,0.,513.0,47.5,0.09091,8.e-6

'methyl ethyl ketone',1000.,0.,0.

72.1,165.e-10,0.,536.8,41.5,0.03704,8.e-6

'methyl isobutyl ketone',1000.,0.,0.

100.2,130.e-10,0.,571.0,32.3,0.01724,8.e-6

'1,1,2,2-tetrachloroethane',1000.,0.,0.

167.9,2300.e-10,0.,661.2,57.6,0.003846,8.e-6

'chlorobenzene',1000.,0.,0.

112.6,600.e-10,0.,632.4,44.6,0.007692,8.e-6

3000.,0.,20000.,0.056,0.,0.

15500.,0.71,40000.,0.229,1.2,0.

0.,0.,28000.,0.,0.,42.e-7

25.,76.,0.9,0

OUTPUT FILE (ZBASEIV.OUT) FROM VDRUM2.FOR (INPUT FILE = ZBASEIV)

zbaseIV

	N(days)	[]@N	[]@SS	0.9[]SS/[]N
carbon tetrachloride	87	672.01	745.84	1.0
methanol	112	613.43	680.86	1.0
dichloromethane	49	682.01	754.24	1.0
toluene	226	723.06	803.09	1.0
trichloroethylene	115	719.01	797.08	1.0
butanol	65	686.69	761.07	1.0
chloroform	46	677.48	751.73	1.0
1,1-dichloroethene	57	613.21	680.21	1.0
methyl ethyl ketone	69	652.31	721.97	1.0
methyl isobutyl ketone	140	644.18	715.08	1.0
1,1,2,2-tetrachloroethane	105	726.57	806.85	1.0
chlorobenzene	104	710.47	788.99	1.0

**Determination of Transuranic Waste Container Drum Age Criteria and Prediction Factors
Based on Packaging Configurations INEEL/EXT-99-01010
November 1999**

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Attachment A—Packaging Configurations in TRUCON Document

Attachment B—Preliminary Sensitivity Analysis on Packaging Variables Impacting Drum Age
Criteria

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DETERMINATION OF DRUM AGE CRITERIA AND PREDICTION FACTORS BASED ON PACKAGING CONFIGURATIONS

EXECUTIVE SUMMARY

Headspace sampling for volatile organic compounds (VOCs) is a characterization requirement for contact-handled (CH) transuranic (TRU) waste containers to be sent to the Waste Isolation Pilot Plant for disposal. Prior to performing headspace sampling, "drum age criteria" (DAC) need to be met for headspace samples to be valid. DACs are estimates of the time required for VOCs in a drum to reach 90 percent of the equilibrium steady-state concentration within the different layers of confinement. In addition, headspace sampling performed after the DAC has been met can be correlated to the VOC concentration in the innermost layer of confinement by the use of prediction factors (PFs), which are multipliers to be applied to the headspace concentration. A set of DACs and PFs for CH-TRU wastes were previously determined assuming conservative packaging configurations in terms of number of layers, presence of a rigid drum liner, and filter diffusivity. A major fraction of the CH-TRU waste is not packaged pursuant to these conservative configurations and would benefit from the application of packaging-specific DACs and PFs.

This report presents the results of a study to determine packaging-specific DACs and PFs, based upon current packaging practices and plans for future packaging configurations. DACs can be reduced up to an order of magnitude by the use of specific packaging options. For waste in a 55-gallon drum, the most dramatic improvement in DACs would result from the elimination of the rigid drum liner, from the removal of the rigid drum liner lid, or from an increase in the size of the hole in the rigid drum liner. For all payload containers, reducing the number of bag layers and improving the filter diffusivity result in lower DACs. The results from this study can be used to reduce the DAC requirement for existing, as well as, future waste forms and packaging configurations, thereby reducing the need for holding times and additional storage capacity at the sites.

The concept of DACs can also be applied to standard waste boxes (SWBs) to determine the "holding time" after waste packaging for headspace sampling. Because rigid drum liners are not used within SWBs, the DACs for the SWB packaging configurations currently in use at the U.S. Department of Energy sites are lower than those for drums.

1.0 INTRODUCTION

Drum age criteria (DAC) are estimates of the time required for volatile organic compounds (VOCs) in a container of contact-handled transuranic (CH-TRU) waste to reach 90 percent of the equilibrium steady-state concentration within the different layers of confinement. The DAC is the time period that must elapse after waste packaging in order for a headspace gas sample for VOCs to be valid. Once the DAC is satisfied and the headspace sampled for VOCs, prediction factors (PFs) can be used to correlate the headspace concentration with the VOC concentration in the innermost layer of confinement. DACs and PFs have been determined based on conservative packaging configurations as reported in Connolly et al. (1998). The current DAC and PF requirements are too restrictive for wastes that are not packaged as in the "bounding case." Waste packaging at several sites includes fewer bag layers; better filters in both bags, drums and other waste containers; more efficient filter sizes and materials; and the absence of the 90-mil rigid drum liner. The current DACs also impose a storage requirement on planned treatment facilities, as the requirement for headspace sampling of VOCs cannot be met until the DAC is satisfied.

2.0 PURPOSE AND SCOPE

The purpose of this study was to develop packaging-specific DACs and PFs that can be used at the U.S. Department of Energy (DOE) sites without the need to use bounding values for the entire CH-TRU waste inventory. A matrix of DACs and PFs has been developed that can be used to define packaging-specific parameters for the entire CH-TRU waste inventory. This report also clarifies the DAC and PF requirements for waste containers with different packaging and venting histories.

The scope of this report includes different packaging configurations used to package 55-gallon drums at the DOE sites. In addition, this report extends the concept of DACs to standard waste boxes (SWBs) and presents the "holding times" needed before headspace sampling of SWBs for VOCs.

3.0 SUMMARY OF PREVIOUS ANALYSIS FOR BASELINE DACS

The current limits for DACs (Connolly et al., 1998) are categorized based on the waste form and packaging as follows:

Waste Types I and IV, Solidified Inorganics and Solidified Organics. These wastes are assumed to be packaged in two drum liner bags, in a rigid drum liner with a 0.375-inch diameter hole, in a 55-gallon drum fitted with a filter with a hydrogen diffusivity of $4.2\text{E-}06$ moles/second/mole fraction.

Waste Types II and III, Solid Inorganics and Solid Organics. These wastes are assumed to be packaged in three inner bags and two drum liner bags, in a rigid drum liner with a 0.375-inch diameter hole, in a 55-gallon drum fitted with a filter with a hydrogen diffusivity of $4.2\text{E-}06$ moles/second/mole fraction.

These values were obtained from testing performed at the Idaho National Engineering and Environmental Laboratory (Connolly et al., 1998). The current DACs are also a function of the waste container packaging and venting history as follows:

- Category 1** Containers that have been packaged for a period of at least one year and are newly vented. For this configuration, the DACs are 22 days for Waste Types I and IV and 18 days for Waste Types II and III. The DACs apply from the date of venting.
- Category 2** Containers that are unvented and are sampled at the time of venting. For this configuration, the DACs are 127 days for Waste Types I and IV and 48 days for Waste Types II and III. The DACs apply from the time of waste packaging. In addition, if the sampling in this case is taken inside the rigid liner, the PF is 1 because the VOCs achieve equilibrium throughout the waste packaging within the rigid liner.
- Category 3** Containers that are newly generated in a vented condition. For this configuration, the DACs are 225 days for Waste Types I and IV and 142 days for Waste Types II and III. The DACs apply from the times of waste packaging and venting, which are the same. This is the most restrictive case that is being applied to the entire CH-TRU inventory at this time.

4.0 METHODOLOGY FOR DETERMINING PACKAGING-SPECIFIC DACS

This report addresses the derivation of DACs to expand available options for Category 3 based on specific packaging configurations. Compliance with the DACs under Category 1 is not an issue because most of the retrievably stored drums in the system have been in storage well over a one-year period prior to venting. Category 2 DACs also apply to retrievably stored wastes and are easily met.

Category 3 applies to newly generated wastes, including wastes to be generated from planned treatment facilities. The biggest impact of the current DACs is on waste containers belonging to this category. Because CH-TRU waste at the different DOE sites is packaged in a variety of ways, a matrix of representative packaging configurations (instead of a single bounding case) was developed for each of the two physical waste forms (solidified and solid) to adequately represent the DOE CH-TRU waste inventory belonging to Category 3. The selection of representative packaging configurations for the DAC analysis was based on the following criteria:

- A review of the TRUPACT-II Content Codes (TRUCON) document (DOE, 1999), which is a compilation of site-specific waste form information, including the different methods used to package the waste at each of the DOE sites. Based on the review of the TRUCON document, all TRUCON code packaging configurations have been summarized as 38 common configurations as listed in Attachment A. These 38 configurations were then divided into two groups: packaging configurations included in Waste Type I and Waste Type IV

TRUCON codes (14 configurations), and packaging configurations included in Waste Type II and Waste Type III TRUCON codes (38 configurations).

- An informal survey of some of the DOE sites expected to generate and package CH-TRU waste in the future.
- A preliminary sensitivity analysis performed to determine which factors most influence the DACs. The details of this sensitivity analysis are presented in Attachment B.

The 38 configurations listed in Attachment A and future packaging options to be used by the sites were consolidated for the DAC analysis based on the frequency of use for the packaging configuration and the sensitivity analysis. Packaging configurations for which the DACs were not expected to differ significantly were represented by a single configuration. Packaging configurations currently not allowed by the TRUPACT-II Safety Analysis Report (SAR) (DOE, 1999) (e.g., filtered bag configurations for Waste Types I and IV) or not used by the sites on a regular basis (e.g., the use of inner bags for Waste Types I and IV) were eliminated from further consideration. The final matrix of selected packaging configurations is shown in Table 1 for Waste Types I and IV and in Table 2 for Waste Types II and III. These selected packaging configurations address DAC dependence on the following parameters:

- Type and number of bag layers
- Presence of rigid drum liner
- Size of hole in the rigid drum liner
- Diffusivity of drum filter.

Table 1
Packaging Configurations for Waste Type I and IV Drums

Case	Packaging Configuration	Rigid Liner	Drum Filter Diffusivity
1	no plastic bags	0.3" diameter hole	3.7×10^{-6} m/s/mf
2	no plastic bags	1" diameter hole	3.7×10^{-5} m/s/mf
3	no plastic bags	no lid	3.7×10^{-6} m/s/mf
4	1 liner bag	0.3" diameter hole	3.7×10^{-6} m/s/mf
5	1 liner bag	1" diameter hole	3.7×10^{-5} m/s/mf
6	2 liner bags	no rigid liner	3.7×10^{-6} m/s/mf
7	2 liner bags	1" diameter hole	3.7×10^{-6} m/s/mf
8	2 liner bags	1" diameter hole	3.7×10^{-5} m/s/mf
9	2 liner bags	no lid	3.7×10^{-6} m/s/mf
10	2 liner bags	no lid	3.7×10^{-5} m/s/mf

Table 2
Packaging Configurations for Waste Type II and III Drums

Case	Packaging Configuration	Rigid Liner	Drum Filter Diffusivity
1	no plastic bags	0.3" diameter hole	3.7×10^{-6} m/s/mf
2	2 inner bags, 1 liner bag	0.3" diameter hole	3.7×10^{-5} m/s/mf
3	2 inner bags, 1 liner bag	1" diameter hole	3.7×10^{-6} m/s/mf
4	2 inner bags, 1 liner bag	1" diameter hole	3.7×10^{-5} m/s/mf
5	3 inner bags, 2 liner bags	no rigid liner	3.7×10^{-6} m/s/mf
6	3 inner bags, 2 liner bags	0.3" diameter hole	3.7×10^{-5} m/s/mf
7	3 filtered inner bags, 2 filtered liner bags	0.3" diameter hole	3.7×10^{-6} m/s/mf
8	5 inner bags, 1 liner bag	1" diameter hole	3.7×10^{-5} m/s/mf
9	5 inner bags, 1 liner bag	no lid	3.7×10^{-6} m/s/mf
10	2 inner bags, 1 liner bag	no lid	3.7×10^{-6} m/s/mf
11	2 inner bags, 1 liner bag	no liner	3.7×10^{-6} m/s/mf

m/s/mf = moles per second per mole fraction.

These are the key variables that impact the DACs and that are of interest to the sites in packaging CH-TRU wastes. The configurations listed in Tables 1 and 2 address Category 3 wastes (newly generated, vented containers) for which DACs are limiting. Some retrievably-stored wastes, which may have been packaged to meet the worst-case limits in the TRUPACT-II SAR (DOE, 1999), fall under Categories 1 or 2 for which the conservative DACs from Connolly et al. (1998) would easily be satisfied.

Application of DACs to SWBs

Attachment A also presents the packaging configurations used at the DOE sites for wastes loaded directly into SWBs. These packaging configurations range from no bag layers to five inner layers in one SWB liner bag. Because no rigid liners are used in SWBs, it was expected that the DACs for this spectrum of SWB packaging configurations would fall within a narrow range and could be encompassed by the following configurations:

- SWBs with one SWB liner bag
- SWBs with five inner bags and one SWB liner bag.

The inner bags are the same as those used in drums. The SWB liner bags are large bags lining the SWBs with a thickness of 14 mil and a surface area of $8.85\text{E}+04$ sq. cm (DOE, 1999). Conservative estimates indicate that the void volume inside the bag layers and in the SWB headspace is 10 percent of the total SWB volume (IT Corporation, 1999).

For the configurations presented in Tables 1 and 2, and the SWB configurations, the methodology for determining DACs was identical to that used in Connolly et al. (1998). The DACs are presented in Section 6.0.

5.0 METHODOLOGY FOR DETERMINING PACKAGING-SPECIFIC PFS

This section describes the methodology used for the determination of PFs for the configurations shown in Tables 1 and 2 and the SWB configurations. This methodology is based on the analysis presented in Connolly et al. (1998). The PF is a variable with a unique value for each VOC and packaging configuration that, when multiplied by the measured VOC concentration in the container headspace, predicts the concentration of the VOC in the innermost confinement layer.

At steady-state conditions, there is no accumulation of VOCs within any layer of confinement, the concentrations of VOCs are constant within each layer of confinement, and the VOC transport rate across each layer of confinement is equal to a constant rate. The primary mechanisms for gas transport across a confinement layer are permeation across a polymeric layer, diffusion through air across an opening in the layer, and diffusion through a filter vent in the case of a drum filter or filtered bag. One or all of these mechanisms of transport may be operating depending on the characteristics of the confinement layer.

Model Assumptions

The following assumptions were made in developing the PF methodology:

1. All gases exhibit ideal behavior.
2. Temperature and pressure are constant.
3. An equilibrium exists between the VOC-contaminated waste and the vapor phase in the innermost layer of confinement. Thus, the VOC concentration within the innermost confinement layer is constant.
4. A sufficient period of time has elapsed (i.e., the DAC has been satisfied) such that the VOC transport rates across all layers of confinement are equal and at steady-state. Thus, the VOC concentration within a void volume is constant and there is no accumulation of gas within any confinement layer.
5. The VOC concentration within a void volume is uniform at all times. Thus, there are no concentration variations within a single void volume.
6. Multiple layers of inner bags and liner bags are treated as a single inner bag or liner bag with a total thickness equal to the product of the number of such layers and the thickness of the individual layer.
7. The concentration of the VOC outside the container is zero. Thus, there is rapid transport by diffusion and convection of the VOC outside the container to maintain a zero concentration outside the drum.
8. All VOC properties and confinement layer properties are constant and uniform.

For each of the various layers of confinement that may be present in a container, the rate of VOC transport across each confinement layer, r , is defined as follows:

Inner Bag (Twist and Tape)

Equation 1

$$r = \frac{\phi c \rho A_{ib} P}{n_{ib} x_{ib}} \Delta y_{ib} = \frac{K_{ib}}{n_{ib}} \Delta y_{ib}$$

where,

- ϕ = 76 T / (273.15 P) (dimensionless)
- c = gas concentration at standard temperature (273.15 °K) and pressure (1 atmosphere) from ideal gas law, P/RT (4.46×10^{-5} mol cm⁻³)
- T = gas temperature (°K)
- ρ = VOC permeability [cm³ (STP) cm⁻¹ sec⁻¹ (cm Hg)⁻¹ = 10¹⁰ Ba]
- A_{ib} = surface area of inner bag (cm²)
- P = gas pressure (cm Hg)
- n_{ib} = number of inner bags in packaging configuration
- x_{ib} = thickness of inner bag (cm)
- Δy_{ib} = VOC mole fraction difference across inner bag (dimensionless)
- K_{ib} = inner bag VOC transport characteristic (mol sec⁻¹)
- R = gas constant (6236.6 cm Hg cm³ mol⁻¹ °K⁻¹)

Liner Bag (Twist and Tape)

Equation 2

$$r = \frac{\phi c \rho A_{lb} P}{n_{lb} x_{lb}} \Delta y_{lb} = \frac{K_{lb}}{n_{lb}} \Delta y_{lb}$$

where,

- A_{lb} = surface area of liner bag (cm²)
- n_{lb} = number of liner bags in packaging configuration

- x_{lb} = thickness of liner bag (cm)
 Δy_{lb} = VOC mole fraction difference across liner bag (dimensionless)
 K_{lb} = liner bag VOC transport characteristic (mol sec⁻¹).

Inner Bag (Filtered)

Equation 3

$$r = \left(\frac{\phi c \rho A_{lb} P}{n_{lb} x_{lb}} + \frac{D_{VOC-bf}^*}{n_{lb}} \right) \Delta y_{lb} = \frac{K_{lb}}{n_{lb}} \Delta y_{lb}$$

where,

- D_{VOC-bf}^* = VOC-bag filter diffusion characteristic (mol s⁻¹), which is calculated by the following equation:

Equation 4

$$D_{VOC-bf}^* = \frac{D_{VOC-air}}{D_{H_2-air}} D_{H_2-bf}^*$$

where,

- $D_{VOC-air}$ = VOC diffusivity in air (cm² sec⁻¹)
 D_{H_2-air} = hydrogen diffusivity in air (cm² sec⁻¹)
 $D_{H_2-bf}^*$ = hydrogen-bag filter diffusion characteristic (mol sec⁻¹).

Liner Bag (Filtered)

Equation 5

$$r = \left(\frac{\phi c \rho A_{lb} P}{n_{lb} x_{lb}} + \frac{D_{VOC-bf}^*}{n_{lb}} \right) \Delta y_{lb} = \frac{K_{lb}}{n_{lb}} \Delta y_{lb}$$

where all variables have been previously defined.

Rigid Drum Liner

Equation 6

$$r = \frac{P D_{VOC-air} A_{rl}}{R T x_{rl}} \Delta y_{rl} = K_{rl} \Delta y_{rl}$$

where,

- A_{rl} = cross-sectional area of the hole in the rigid drum liner lid (cm²)
- x_{rl} = diffusional path length across hole in the rigid drum liner lid (cm)
- Δy_{rl} = VOC mole fraction difference across the rigid liner (dimensionless)
- K_{rl} = rigid liner transport characteristic (mol sec⁻¹)

The VOC-diffusivity in air, $D_{VOC-air}$, can be estimated at low pressures using an equation developed from a combination of kinetic theory and corresponding-states arguments shown below (Liekhus, 1995):

Equation 7

$$D_{VOC-air} = 2.745 \times 10^{-4} \frac{T^{1.823}}{P} [p_{c-VOC} p_{c-air}]^{1/3} [T_{c-VOC} T_{c-air}]^{-1/2} \left[\frac{1}{M_{VOC}} + \frac{1}{M_{air}} \right]^{1/2}$$

where,

- M_{VOC} = molecular weight of VOC (g/mol)
- M_{air} = molecular weight of air (29 g/mol)
- p_{c-VOC} = critical pressure of VOC (atm)
- p_{c-air} = critical pressure of air (36.4 atm)
- T_{c-VOC} = critical temperature of VOC (°K)
- T_{c-air} = critical temperature of air (132°K).

Container Filter

Equation 8

$$r = n_{cf} D^*_{VOC-cf} \Delta y_{cf} = n_{cf} D^*_{VOC-cf} y_{hs}$$

where,

- Δy_{cf} = VOC mole fraction difference across the container filter (dimensionless)
- y_{hs} = VOC mole fraction measured in container headspace (dimensionless)
- n_{cf} = number of container filters in packaging configuration
- D^*_{VOC-cf} = VOC-container filter diffusion characteristic (mol sec^{-1}), which is calculated through the following equation:

Equation 9

$$D^*_{VOC-cf} = \frac{D_{VOC-air}}{D_{H_2-air}} D^*_{H_2-cf}$$

where,

- $D^*_{H_2-cf}$ = Hydrogen-container filter diffusion characteristic (mol sec^{-1}).

Sequential substitution and rearrangement of terms yields the following relationship for the innermost confinement layer VOC concentration as a function of the measured container headspace VOC concentration:

Equation 10

$$y_{icl} = y_{hs} [1 + n_{cf} D_{VOC-cf} (\sum_{i=1}^{nl} \frac{n_i}{K_i})]$$

where,

- y_{icl} = innermost confinement layer VOC mole fraction (dimensionless)
- n_i = number of type “i” confinement layers in packaging configuration
- K_i = transport characteristic of type “i” confinement layer (mol sec^{-1})
- nl = number of different confinement layer types.

Multiplying both sides of Equation 10 by a conversion factor (10^6 ppm/mole fraction) yields the following final equation for the prediction factor:

Equation 11

$$Y_{icl} = Y_{hs} [1 + n_{cf} D_{voc-cf} (\sum_{i=1}^{n_l} \frac{n_i}{K_i})]$$

where,

Y_{icl} = innermost confinement layer VOC concentration (ppm)

Y_{hs} = measured VOC concentration in container headspace (ppm).

Thus, the prediction factor, PF, is:

Equation 12

$$PF = [1 + n_{cf} D_{voc-cf} (\sum_{i=1}^{n_l} \frac{n_i}{K_i})]$$

Using this equation, the PFs for the representative configurations listed in Tables 1 and 2 and the two SWB configurations can be established.

6.0 RESULTS AND CONCLUSIONS

Tables 3 and 4 present a summary of the DACs and PFs for the packaging configurations listed in Tables 1 and 2. Table 5 lists the DACs and PFs for the two SWB configurations. Depending on the packaging configurations, the DACs can range from a few months to a few days. As shown in the tables, the use of packaging-specific information can reduce the DACs and PFs considerably. The following conclusions can be drawn from the results presented in Tables 3 and 4:

- The most significant reduction in DACs for drums is for packaging configurations that do not use a rigid drum liner or that do not use the lid on the drum liner. The rate-limiting step for the VOCs to reach equilibrium is the solubility and permeation through the liner. Absence of the liner or the liner lid eliminates this rate-limiting step. In addition, the larger the size of the hole in the liner lid, the smaller the DAC.
- Fewer bag layers result in smaller DACs and PFs, but the impact is less than removing the rigid liner or liner lid.
- Better filters in the drum result in smaller DACs. The use of filters in bags is less important, because the permeation of VOCs from the bags is significant compared to the diffusion through the filter.

- All SWB packaging configurations currently in use at the sites can be bound by the DACs shown in Table 5, with the maximum DAC being 56 days for SWBs. The SWB DACs are considerably lower than those for drums due to the absence of a rigid liner.

The matrices presented in Tables 3, 4 and 5 can be used with future TRUPACT-II SAR and Waste Isolation Pilot Plant Resource Conservation and Recovery Act Part B Permit amendments to specify lower DACs and PFs for different waste packaging configurations in drums and SWBs. The Revision 19 initiative of the TRUPACT-II SAR, expected to be submitted to the U.S. Nuclear Regulatory Commission in the near future, can use this study to classify the CH-TRU waste inventory for newly generated wastes pursuant to the matrices in Tables 3, 4 and 5. In addition, the DACs in Tables 3, 4 and 5 can be incorporated into the Automated TRUPACT-II Authorized Methods for Payload Control (e-TRAMPAC) and linked to the packaging description of the waste. Lower DACs can also be specified for retrievably stored wastes (Categories 1 and 2), for wastes with no confinement layers, and for treated waste forms for which the absence of VOCs can be established and documented.

Table 3
DACs and PFs for Waste Type I and IV Packaging Configurations for Drums

DAC (Days)	DAC/PF by VOC									
	Case 1	Case 2	Case 3	Case 4	Case 5	Case 6	Case 7	Case 8	Case 9	Case 10
	111	19	4	188	71	31	151	110	106	84
PF										
Flammable VOCs										
Acetone	1.3	1.3	1.0	1.4	2.1	1.2	1.2	2.8	1.2	2.5
Benzene	1.3	1.3	1.0	1.4	1.7	1.1	1.1	2.1	1.1	1.8
1-Butanol	1.3	1.3	1.0	1.3	1.7	1.1	1.1	2.0	1.1	1.7
Chlorobenzene	1.3	1.3	1.0	1.3	1.5	1.0	1.1	1.6	1.0	1.3
Cyclohexane	1.3	1.3	1.0	2.0	7.9	2.3	2.4	14.5	2.3	14.2
1,1-Dichloroethane	1.3	1.3	1.0	1.4	1.9	1.1	1.1	2.4	1.1	2.1
1,2-Dichloroethane	1.3	1.3	1.0	1.3	1.6	1.0	1.1	1.8	1.0	1.5
1,1-Dichloroethene	1.3	1.3	1.0	1.4	2.3	1.2	1.2	3.3	1.2	3.0
cis-1,2-Dichloroethene	1.3	1.3	1.0	1.4	1.7	1.1	1.1	2.1	1.1	1.8
Ethyl benzene	1.3	1.3	1.0	1.3	1.7	1.1	1.1	2.0	1.1	1.7
Ethyl ether	1.3	1.3	1.0	1.6	3.9	1.5	1.5	6.5	1.5	6.2
Methanol	1.3	1.3	1.0	1.4	2.5	1.2	1.3	3.6	1.2	3.3
Methyl ethyl ketone	1.3	1.3	1.0	1.4	2.0	1.1	1.2	2.6	1.1	2.3
Methyl isobutyl ketone	1.3	1.3	1.0	1.4	2.0	1.1	1.2	2.7	1.1	2.4
Toluene	1.3	1.3	1.0	1.3	1.5	1.0	1.1	1.6	1.0	1.3
1,2,4-Trimethylbenzene	1.3	1.3	1.0	1.3	1.6	1.1	1.1	1.8	1.1	1.5
1,3,5-Trimethylbenzene	1.3	1.3	1.0	1.3	1.6	1.1	1.1	2.0	1.1	1.6
o-Xylene	1.3	1.3	1.0	1.3	1.6	1.0	1.1	1.8	1.0	1.5
m-Xylene	1.3	1.3	1.0	1.3	1.7	1.1	1.1	2.0	1.1	1.7
p-Xylene	1.3	1.3	1.0	1.3	1.4	1.0	1.1	1.5	1.0	1.2
PF										
Nonflammable VOCs										
Bromoform (Tribromomethane)	1.3	1.3	1.0	1.3	1.3	1.0	1.0	1.4	1.0	1.1
Carbon tetrachloride	1.3	1.3	1.0	1.4	1.8	1.1	1.1	2.3	1.1	2.0
Chloroform	1.3	1.3	1.0	1.4	1.7	1.1	1.1	2.1	1.1	1.8
Methylene chloride (dichloromethane)	1.3	1.3	1.0	1.4	1.8	1.1	1.1	2.2	1.1	1.9
1,1,2,2-Tetrachloroethane	1.3	1.3	1.0	1.3	1.4	1.0	1.0	1.4	1.0	1.1
Tetrachloroethene	1.3	1.3	1.0	1.3	1.5	1.0	1.1	1.6	1.0	1.3
1,1,1-Trichloroethane	1.3	1.3	1.0	1.4	2.0	1.1	1.2	2.7	1.1	2.4
Trichloroethene	1.3	1.3	1.0	1.3	1.5	1.0	1.1	1.7	1.0	1.4
1,1,2-Trichloro-1,2,2-trifluoroethane	1.3	1.3	1.0	1.5	3.6	1.5	1.5	5.9	1.5	5.6

*Packaging configurations for each case are defined in Table 1.

Table 4
DACs and PFs for Waste Type II and III Packaging Configurations for Drums

DACs and PFs for Waste Type II and III Packaging Configurations for Drums												
DAC/PF by VOC		Packaging Configuration*										
		Case 1 113	Case 2 51	Case 3 52	Case 4 42	Case 5 14	Case 6 67	Case 7 134	Case 8 56	Case 9 40	Case 10 25	Case 11 9
DAC (Days)		PF										
Flammable VOCs		1.3	4.5	1.1	1.6	1.1	4.7	1.4	1.9	1.1	1.0	1.0
Acetone		1.3	4.3	1.0	1.5	1.0	4.4	1.3	1.6	1.0	1.0	1.0
Benzene		1.3	4.3	1.0	1.5	1.0	4.4	1.3	1.6	1.0	1.0	1.0
1-Butanol		1.3	4.2	1.0	1.4	1.0	4.3	1.3	1.4	1.0	1.0	1.0
Chlorobenzene		1.3	6.9	1.3	4.1	1.5	8.9	1.7	6.0	1.5	1.3	1.3
Cyclohexane		1.3	4.4	1.1	1.6	1.0	4.5	1.4	1.7	1.0	1.0	1.0
1,1-Dichloroethane		1.3	4.2	1.0	1.4	1.0	4.3	1.3	1.5	1.0	1.0	1.0
1,2-Dichloroethane		1.3	4.5	1.1	1.7	1.1	4.9	1.4	2.0	1.1	1.0	1.0
1,1-Dichloroethene		1.3	4.3	1.0	1.5	1.0	4.4	1.3	1.6	1.0	1.0	1.0
cis-1,2-Dichloroethene		1.3	4.3	1.0	1.5	1.0	4.4	1.3	1.6	1.0	1.0	1.0
Ethyl benzene		1.3	5.2	1.1	2.4	1.2	6.0	1.5	3.2	1.2	1.1	1.1
Ethyl ether		1.3	4.6	1.1	1.8	1.1	5.0	1.4	2.1	1.1	1.0	1.0
Methanol		1.3	4.4	1.1	1.6	1.0	4.6	1.4	1.8	1.0	1.0	1.0
Methyl ethyl ketone		1.3	4.4	1.1	1.6	1.1	4.6	1.4	1.8	1.1	1.0	1.0
Methyl isobutyl ketone		1.3	4.2	1.0	1.4	1.0	4.2	1.3	1.4	1.0	1.0	1.0
Toluene		1.3	4.2	1.0	1.4	1.0	4.3	1.3	1.5	1.0	1.0	1.0
1,2,4-Trimethylbenzene		1.3	4.3	1.0	1.5	1.0	4.4	1.3	1.5	1.0	1.0	1.0
1,3,5-Trimethylbenzene		1.3	4.2	1.0	1.4	1.0	4.3	1.3	1.5	1.0	1.0	1.0
o-Xylene		1.3	4.3	1.0	1.5	1.0	4.4	1.3	1.6	1.0	1.0	1.0
m-Xylene		1.3	4.2	1.0	1.4	1.0	4.3	1.3	1.5	1.0	1.0	1.0
p-Xylene		1.3	4.2	1.0	1.4	1.0	4.2	1.3	1.4	1.0	1.0	1.0
Nonflammable VOCs		PF										
Bromoform		1.3	4.1	1.0	1.3	1.0	4.2	1.3	1.3	1.0	1.0	1.0
(Tribromomethane)												
Carbon tetrachloride		1.3	4.4	1.1	1.5	1.0	4.5	1.4	1.7	1.0	1.0	1.0
Chloroform		1.3	4.3	1.0	1.5	1.0	4.4	1.3	1.6	1.0	1.0	1.0
Methylene chloride		1.3	4.3	1.1	1.5	1.0	4.5	1.3	1.7	1.0	1.0	1.0
(dichloromethane)												
1,1,2,2-Tetrachloroethane		1.3	4.2	1.0	1.3	1.0	4.2	1.3	1.4	1.0	1.0	1.0
Tetrachloroethene		1.3	4.2	1.0	1.4	1.0	4.3	1.3	1.4	1.0	1.0	1.0
1,1,1-Trichloroethane		1.3	4.4	1.1	1.6	1.1	4.6	1.4	1.8	1.1	1.0	1.0
Trichloroethene		1.3	4.2	1.0	1.4	1.0	4.3	1.3	1.5	1.0	1.0	1.0
1,1,2-Trichloro-1,2,2-trifluoroethane		1.3	5.1	1.1	2.3	1.2	5.8	1.5	3.0	1.2	1.1	1.1

*Packaging configurations for each case are defined in Table 2.

Table 5
DACs and PFs for SWB Packaging Configurations

DAC/ PF by VOC	Packaging Configuration	
	SWB Case 1 – One SWB Liner Bag	SWB Case 2 – Five Inner Bags & One SWB Liner Bag
DAC (Days)	15	56
Flammable VOCs		
Acetone	1.0	1.1
Benzene	1.0	1.0
1-Butanol	1.0	1.0
Chlorobenzene	1.0	1.0
Cyclohexane	1.1	1.7
1,1-Dichloroethane	1.0	1.1
1,2-Dichloroethane	1.0	1.0
1,1,1-Trichloroethane	1.0	1.1
cis-1,2-Dichloroethane	1.0	1.0
Ethyl benzene	1.0	1.0
Ethyl ether	1.0	1.0
Methanol	1.0	1.3
Methyl ethyl ketone	1.0	1.1
Methyl isobutyl ketone	1.0	1.1
Toluene	1.0	1.0
1,2,4-Trimethylbenzene	1.0	1.0
1,3,5-Trimethylbenzene	1.0	1.0
o-Xylene	1.0	1.0
m-Xylene	1.0	1.0
p-Xylene	1.0	1.0
Nonflammable VOCs		
Bromomethane (Tribromomethane)	1.0	1.0
Carbon tetrachloride	1.0	1.1
Chloroform	1.0	1.0
Methylene chloride (dichloromethane)	1.0	1.0
1,1,2,2-Tetrachloroethane	1.0	1.0
Tetrachloroethene	1.0	1.0
1,1,1-Trichloroethane	1.0	1.1
Trichloroethene	1.0	1.0
1,1,2-Trichloro-1,2,2-trifluoroethane	1.0	1.2

7.0 REFERENCES

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Attachment A

**Packaging Configurations in
TRUCON Document**

Packaging Configurations in the TRUCON Document

Configuration*	Number in TRUCON	Waste Type(s)	Payload Container(s)					
			Drum	SWB OP	SWB	Bin	TDOP	Pipe
No layers	31	I, II, III, IV	X	X	X		X	
No layers, filtered inner lid	1	III	X	X				
Metal Can (II.2)	24	II	X	X	X		X	X
1 inner	9	II, III, IV	X	X	X		X	
1 inner, filtered inner lid	1	III	X	X				
1 filtered inner	8	II, III	X	X	X		X	
1 liner	26	I, II, III	X	X	X		X	
1 liner, filtered inner lid	1	III	X	X				
1 filtered liner	15	II, III	X	X	X		X	
1 inner, 1 liner	14	I, II, III	X	X	X		X	
1 filtered inner, 1 filtered liner	2	II, III	X		X			
1 inner, 1 liner, 1 filtered can	3	III	X	X				
1 filtered inner, 1 filtered liner, 1 filtered can	4	III	X	X	X			
2 inner	18	II, III, IV	X	X	X		X	X
2 inner, 1 filtered can	3	III	X	X				X
2 filtered inner	21	I, II, III, IV	X	X				X
2 filtered inner, 1 filtered can	16	I, II, III, IV						X
2 liner	29	I, II, III, IV	X	X	X	X	X	
2 filtered liner	9	II, III	X					
1 inner, 2 liner	3	II, III			X		X	
2 inner, 1 liner	29	I, II, III, IV	X	X	X		X	
2 filtered inner, 1 filtered liner	4	I, III	X	X	X			
2 inner, 1 liner, 1 filtered can	2	III	X	X				
2 filtered inner, 1 filtered liner, 1 filtered can	10	II, III, IV	X	X	X			
2 filtered inner, 1 filtered liner, 2 filtered cans	3	I, III	X	X				
2 inner, 2 liner	28	I, II, III	X	X	X			
2 filtered inner, 2 filtered liner	2	III	X	X				
2 filtered inner, 2 filtered liner, 1 filtered can	1	II	X	X				
3 inner, filtered inner lid	1	III	X	X				
3 inner, 1 liner	6	II, III	X	X	X		X	
3 inner, 1 liner, 1 filtered can	2	III	X	X				
3 filtered inner, 1 filtered liner, 1 filtered can	5	I, III	X	X				
4 inner	1	II			X			
4 inner, 1 liner	6	II, III	X	X	X		X	
4 filtered inner, 1 filtered liner, 1 filtered can	4	III	X					
3 inner, 2 liner	11	II, III	X	X	X			
4 inner, 2 liner	1	II	X	X	X			
5 inner, 1 liner	3	II, III	X	X	X		X	

*"Inner" and "liner" refer to plastic bag layers.

Attachment B

**Preliminary Sensitivity Analysis on
Packaging Variables Impacting
Drum Age Criteria**

B-1

B-1

Preliminary Sensitivity Analysis on Packaging Variables Impacting Drum Age Criteria

Background

A computer code incorporating model equations describing unsteady-state or transient gas transport in a waste drum has been developed and used to estimate the time required for the concentration of a volatile organic compound (VOC) to reach near steady-state or equilibrium concentrations in the drum.¹ The time required to reach these concentrations is defined as a drum age criterion (DAC) and is a function of the VOC and waste drum configuration.

The DAC was calculated for 30 VOCs in two different waste drum configurations under three different sampling scenarios.² Common features to these drum configurations was the presence of a rigid polyethylene drum liner and polymers bags, in which the waste was packaged, inside a 55-gallon waste drum. Variables in the packaging configuration include the number of polymer bags, bag thickness, and available permeable surface area surrounding the waste. One configuration is typical for solidified waste (Waste Type I and IV). Another packaging configuration is typically used for solid waste (Waste Types II and III). In addition, three different sampling scenarios were considered:

- 1) Newly vented existing waste drums that had achieved equilibrium conditions before venting.
- 2) Newly packaged vented waste drum
- 3) Newly packaged unvented waste drum

In the first two scenarios, the DAC represent the time required to approach steady-state conditions. In the case of the unvented waste drum, the DAC is the time required to approach equilibrium conditions.

The DAC is also a function of the chemical and physical properties of the VOC. The VOCs were screened to identify indicator VOCs that are most significant with regards to flammability issues and human health risks. The highest DAC value among the indicator VOCs in the different drum configurations and scenarios is currently used to define the minimum storage or vent time required before sampling the drum headspace. These values are summarized in Table I.

Table I
Current DACs (in days) for Different Packaging Configurations
(by Waste Type) and Sampling Scenarios

	Waste Type I/IV	Waste Type II/III
Newly vented, existing	22	18
Newly packaged, vented	225	142
Newly packaged, unvented	127	48

The DACs associated with newly packaged waste drums have been identified as potentially impacting waste drum packaging and characterization processes because of the significant holding period required. As part of a study to identify ways to decrease the total holding time or DAC, a series of model calculations were performed to identify how changes in waste packaging configuration may result in smaller DACs.

Model Parameters

The following parameters were evaluated:

- Number of layers of polymer bags
- VOC permeability across polymer bags (reflecting influence of bag material)
- Presence or absence of rigid polyethylene drum liner
- Cross-sectional area of opening in drum liner lid
- Bag filter and drum filter vent diffusion characteristics.

In order to demonstrate the relative effect of changing these variables, DAC values are calculated for a baseline case as well as other cases in which one baseline parameter is changed.

Baseline Case

The packaging configuration associated with solid waste (Waste Types II/III) serves as the baseline case to demonstrate the effect of changing parameter values. The model parameters for this case are listed in Table II. Waste is packaged inside three consecutive small bags (bag thickness = 0.0125 cm). All small bags are contained within two large bags (bag thickness = 0.028 cm). All waste and polymer bags are contained inside a rigid 90-mil polyethylene liner with a 0.375-diameter opening in the liner lid. The drum vent has a hydrogen diffusion characteristic of 42×10^{-7} mol/s. The DAC for this waste packaging configuration is based on the DAC for toluene and is 142 days.

Layers of Polymer Bags

Three waste packaging configurations with different numbers of layers of polymer bags were considered:

- 1) Four small bags, two large bags

- 2) One large bag only
- 3) No polymer bags.

The computer code is written assuming the presence of at least one bag in the system. In order to simulate the case of no bags, a large bag with a larger surface area and almost no thickness (0.0001 cm) is assumed to approximate the final case. The results are summarized in Table III.

VOC Permeability and Polymer Bag Material

Different bag materials have been used or are proposed for use. Polyethylene and polyvinyl chloride bags have been used in waste packaging. Limited data showed that VOC permeability across these bags are similar.³ Nylon bags are being considered for packaging but permeability of all indicator VOCs in this polymer is not well characterized. In order to demonstrate the effect of different polymer bag material on the DAC, the VOC permeability is varied. Low VOC permeability will increase the DAC and higher permeability will decrease. Parameter variability and results are listed in Table II.

Drum Liner and Opening in Drum Liner Lid

When a drum liner is present, an opening in the drum liner lid is required to allow gas transport from the inner polymer bags to the drum headspace below the vented drum lid. The effect of varying the cross-sectional area of the opening in the drum liner lid is listed in Table III. The DAC for a waste drum with no drum liner present is calculated and listed in Table III. It is estimated in the computer model by assuming a drum liner is present but has minimal thickness (0.0001 cm) and no lid.

Table II
Drum Age Criterion as a Function of Polymer Bag Layers and VOC Permeability

Case	Input File ^a	Indicator VOC	Waste Type II/III DAC (days)	Waste Type I/IV DAC (days)
Baseline (3 small bags, 2 large bags)	vbase	toluene	142	---
Baseline (2 large bags)	rbase0	toluene	---	225
4 small bags, 2 large bags	vbase2a	toluene	149	---
0 small bags, 1 large bags	vbase2b	toluene	103	---
	rbase1	---	---	162
0 small bags, 0 large bags (estimate)	vbase2d	toluene	84	---
	rbase1b	---	---	90
Baseline ($p_{\text{voc}} = 670.\text{e-}10$) ^b	See above	toluene	142	225
$p_{\text{voc}} = 67.\text{e-}10$	vbase3a	NA	517	---
	rbase2a	---	---	1051
$p_{\text{voc}} = 6700.\text{e-}10$	vbase3c	NA	77	---
	rbase2b	---	---	87

a. Output file name is "inputfile.out"

b. Units of $\text{cm}^3(\text{STP}) \text{ cm cm}^{-2} (\text{cm Hg})^{-1} \text{ s}^{-1}$

Bag Filters and Drum Filter Vents Properties

The addition of a bag filter to polymer bags is intended to facilitate the diffusion of hydrogen between layers of confinement. The presence of a bag filter inherently increases the ability of VOCs to move between layers of confinement. While bag filters can be designed to significantly reduce resistance to gas diffusion, VOC diffusivity is generally an order of magnitude less than that of hydrogen.

In the same manner, the drum filter vent can be designed to have a higher hydrogen diffusion characteristic but the VOC diffusion characteristic will always be an order of magnitude lower. The results of using different filters and vents on the DAC are listed in Table IV.

Table III
Drum Age Criterion as a Function of Drum Liner and Opening in Liner Lid

Case	Input File ^a	Indicator VOC	Waste Type II/III DAC (days)	Waste Type I/IV DAC (days)
Baseline ($A_{DL}=0.71 \text{ cm}^2$, $x_d=1.2 \text{ cm}$) ^b	vbase rbase0	toluene	142 ---	--- 225
1-in diameter opening in liner lid $A_{DL}=5.07 \text{ cm}^2$, $x_d=1.4 \text{ cm}^c$	vbase5b rbase3a	toluene	73 ---	--- 151
2-in diameter opening in liner lid $A_{DL}=20.27 \text{ cm}^2$, $x_d=1.4 \text{ cm}$	vbase5c rbase3b	toluene	55 ---	--- 133
No lid on top of liner $A_{DL}=150 \text{ cm}^2$, $x_d=1.4 \text{ cm}$	vbase5e rbase3c	toluene	41 ---	--- 126
No liner (estimate) ^d $A_{DL}=150 \text{ cm}^2$, $x_d=1.4 \text{ cm}$, $x_p=0.0001 \text{ cm}$ $V_{DL} = V_{DH} = 20,000 \text{ cm}^3$	vbase5i	toluene	2	---
		1,1-DCE ^e	9	---
		methanol	< 9 ^f	---
		MIBK ^e	8	---
		MEK ^e	6	---
		CCl_4 ^e	6	---
		CH_2Cl_2 ^e	4	---
		CHCl_3 ^e	4	---
		butanol	4	---
		TCE ^e	2	---
		chlorobenzene	2	---
No liner (estimate) ^d $A_{DL}=150 \text{ cm}^2$, $x_d=1.4 \text{ cm}$, $x_p=0.0001 \text{ cm}$ $V_{DL} = V_{DH} = 20,000 \text{ cm}^3$	rbase3f	1,1,2,2- CH_2Cl_4 ^e	1	---
		toluene	---	4
		1,1-DCE ^e	---	18
		methanol	---	< 18 ^f
		MIBK ^e	---	16
		MEK ^e	---	13
		CCl_4 ^e	---	12
		CH_2Cl_2 ^e	---	9
		CHCl_3 ^e	---	9
		butanol	---	8
		TCE ^e	---	5
		chlorobenzene	---	4
		1,1,2,2- CH_2Cl_4 ^e	---	2

a. Output file name is "inputfile.out".

b. A_{DL} = cross-sectional area of opening in drum liner lid; x_d = diffusional path length across opening.

c. Increased diffusion path length used for larger openings

d. Lid area $\approx 2,700 \text{ cm}^2$, but model results converge for areas equal to or greater than 150 cm^2 . The case of no liner is approximated by letting liner thickness (x_p) approach zero. Total void volume assumed to be approximately 20% of drum volume (40 L) and equally divided between liner headspace and drum headspace.

e. DCE: dichloroethene; MIBK: methyl isobutyl ketone; MEK: methyl ethyl ketone; CCl_4 : carbon tetrachloride; CH_2Cl_2 : dichloromethane; CHCl_3 : chloroform; TCE: trichloroethylene; CH_2Cl_4 : tetrachloride

f. Methanol diffusivity is greater than that of 1,1-DCE and therefore will have a smaller DAC in this case.

Table IV
Drum Age Criterion as a Function of Polymer Bag Filters and Drum Filter Vents

Case	Input File ^a	Indicator VOC	Waste Type II/III DAC (days)	Waste Type I/IV DAC (days)
Baseline ($D_{H_2}^* = 42.e-7 \text{ mol/s}$) ^b	vbase rfbase0	toluene	142 ---	--- 225
$D_{H_2}^* = 420.e-7 \text{ mol/s}$	vbase7b rfbase7a	toluene	68 ---	--- 122
Baseline (no bag filters)	vbase rfbase0	toluene	142 ---	--- 225
Bag filters ($D_{H_2}^* = 1000.e-7 \text{ mol/s}$) $D_{VOC}^* = 0.1 D_{H_2}^*$	vbase6b rfbase6b	toluene	137 ---	--- 164
Bag filters ($D_{H_2}^* = 10000.e-7 \text{ mol/s}$) $D_{VOC}^* = 0.1 D_{H_2}^*$	vbase6a rfbase6a	toluene	110 ---	--- 88

a. Output file name is "inputfile.out"

b. D^* = gas diffusion characteristic of filter or filter vent

Model Parameters for Smaller DAC

The following parameters resulted in a smaller DAC compared to a baseline case:

- Decreased layers of polymer bags or thinner polymer bags
- Increased VOC permeability across polymer bags
- Larger opening in drum liner lid
- Elimination of the drum liner
- Use of bag filters
- Drum filter vents with greater hydrogen diffusion characteristic

The greatest benefit in achieving a smaller DAC value came from the elimination of the drum liner or at least the removal of the liner lid. The reduction of the available mass of drum liner for absorbing VOC vapors decreases the time to achieve near steady-state conditions.

The effect of increased bag surface area was not specifically examined. As the permeable surface area of polymer bags increases, the DAC decreases. However, since the surface area in model calculations is based on an assumption of the amount of waste in the drum and not easily manipulated in an actual waste drum, model calculations using different values for surface area were not performed.

The VOC permeability in a given polymer cannot be readily varied. Great benefit was demonstrated for highly porous drum filter vents but it is not clear that such vents are currently available. Bag filters were shown to be more beneficial for the drum containing waste sludge where the permeable area of the bags was assumed to be small. Possible fouling of the bag filter on the innermost bag may prevent credit being taken for the presence of a bag filter. Just as much benefit can be achieved by eliminating a bag layer all together.

References

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